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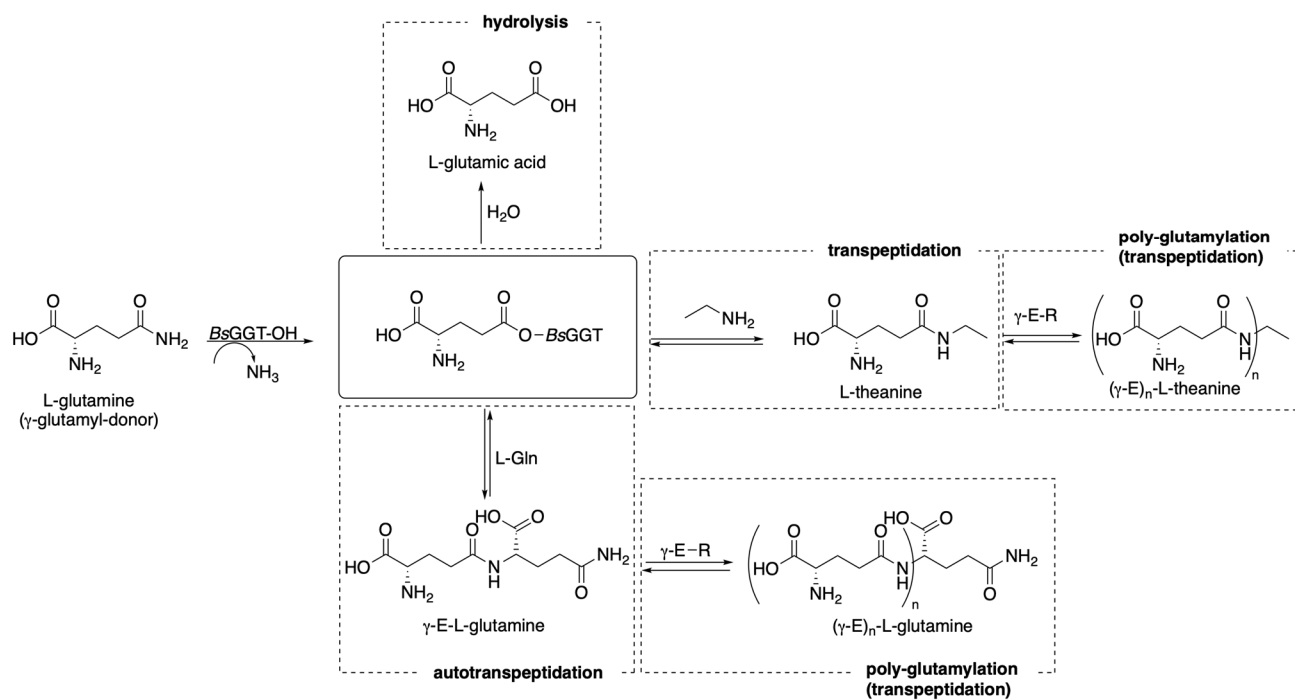
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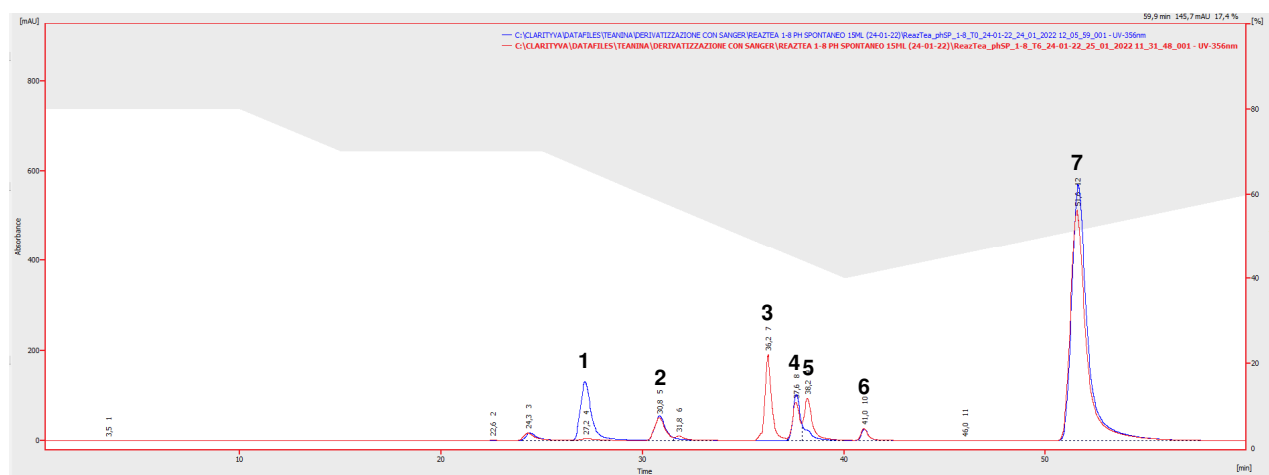
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### Green metrics calculations

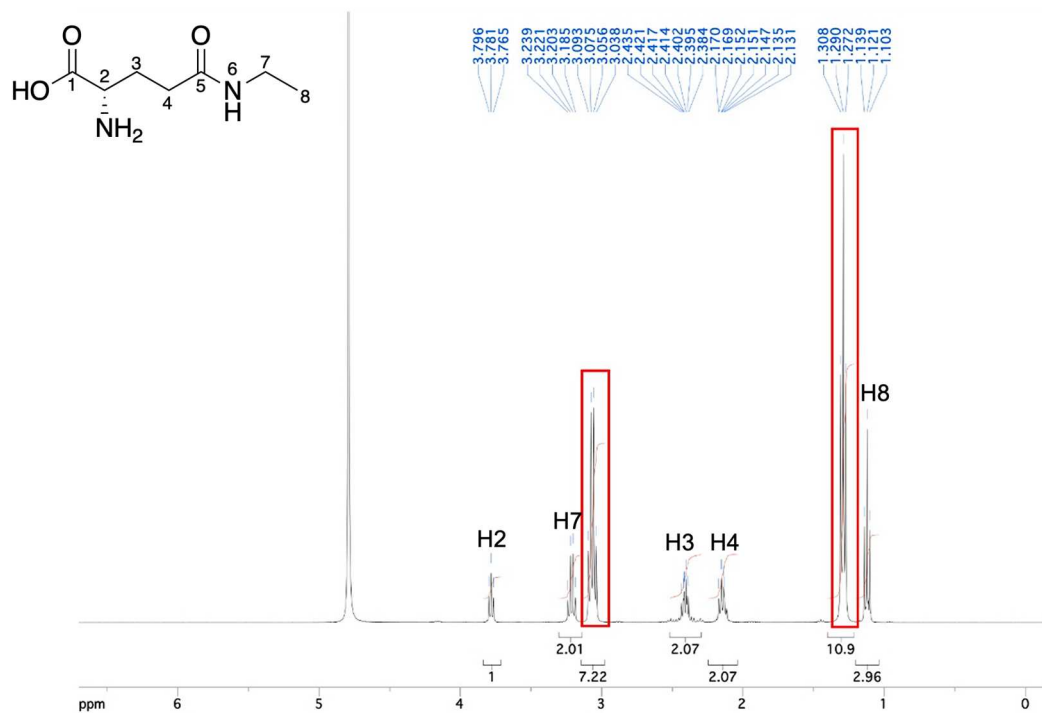
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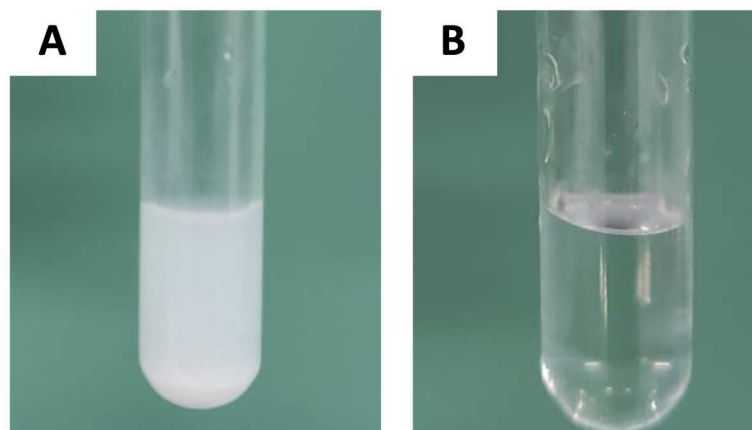
**Figure S1.** Reactions catalyzed by  $\gamma$ -glutamyl transferase from *Bacillus subtilis* (BsGGT).  $\gamma\text{-E-R}$  =  $\gamma$ -glutamyl-compounds formed during the reaction.



**Figure S2.** HPLC chromatogram of the enzymatic synthesis of L-Th at pH 11.6: t0 (blue line) and 6 h endpoint (red line). 1= L-Gln; 2 =L-Ser (internal standard); 3= L-Th; 4= Sanger's reagent; 5= ammonia; 6= derivatization artifact; 7= ethylamine.



**Figure S3.** <sup>1</sup>H NMR spectrum of L-Th (D<sub>2</sub>O) synthesized at pH 10.0. Ethyl signals from ethyl ammonium chloride are highlighted in red.



**Figure S4.** Silver nitrate precipitation test on L-Th synthesized at pH 10 (**A**) and at pH 11.6 (**B**).

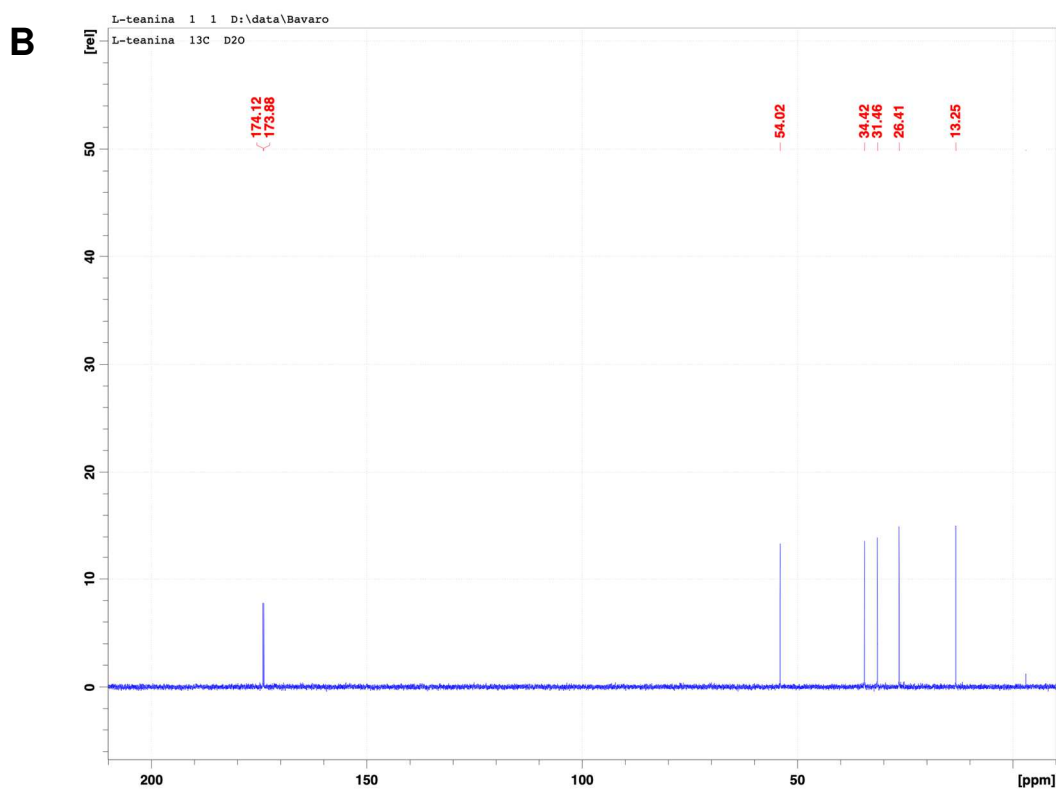
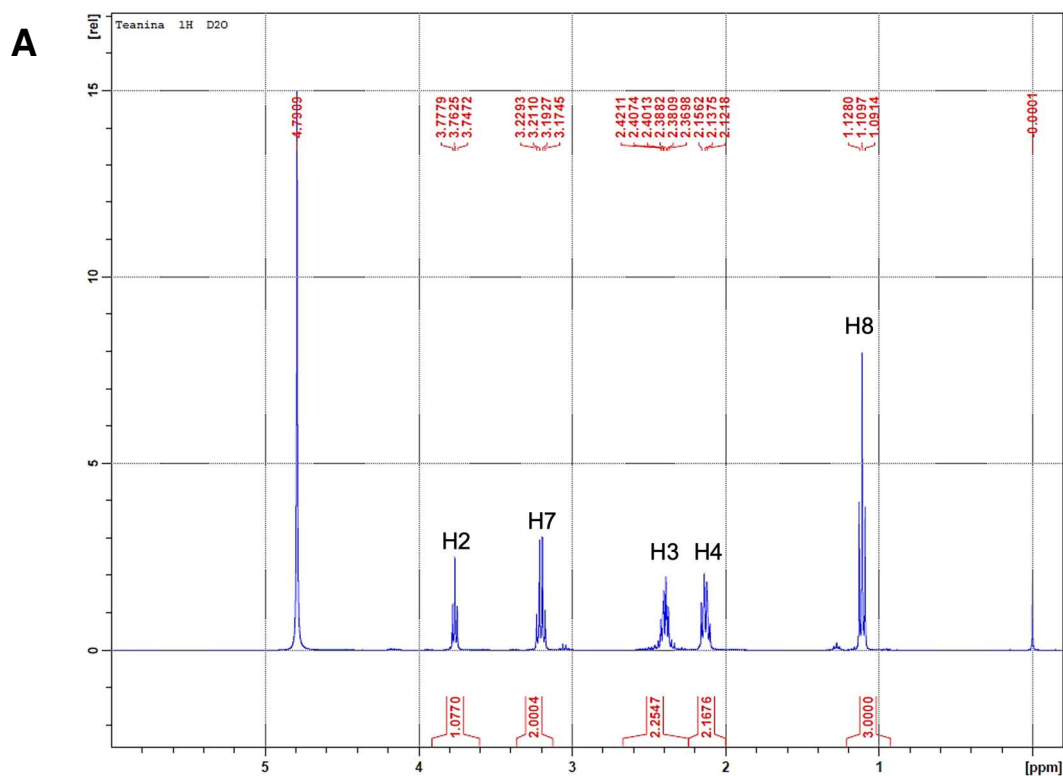
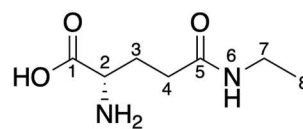
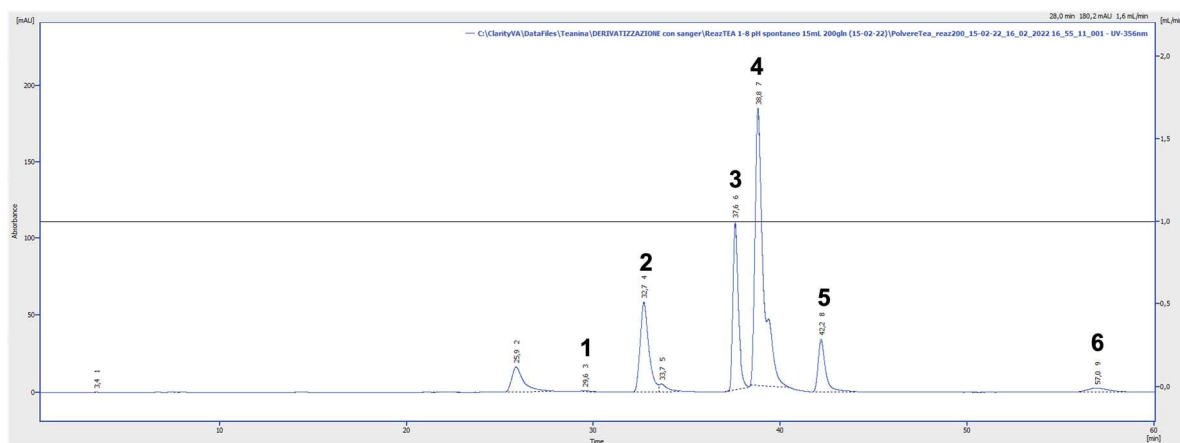
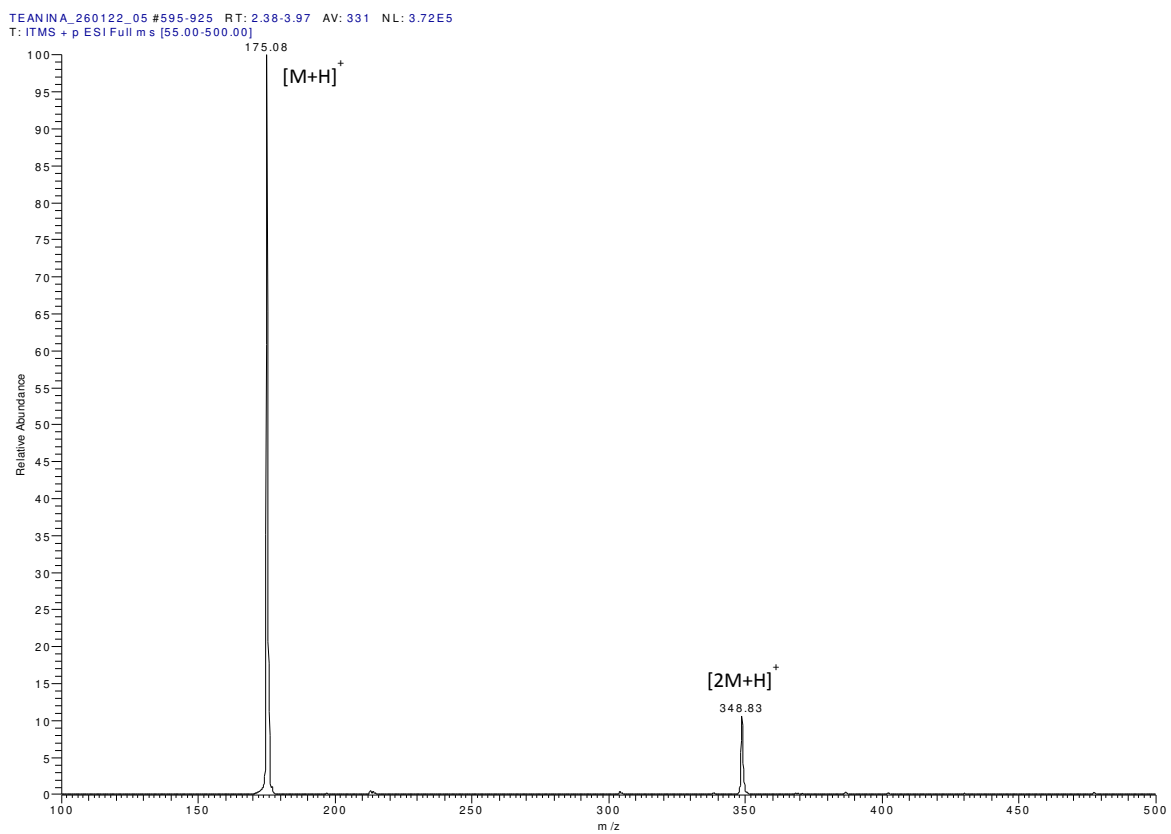


Figure S5. <sup>1</sup>H NMR (A) and <sup>13</sup>C NMR (B) spectra of L-Th (D<sub>2</sub>O) synthesized at pH 11.6.

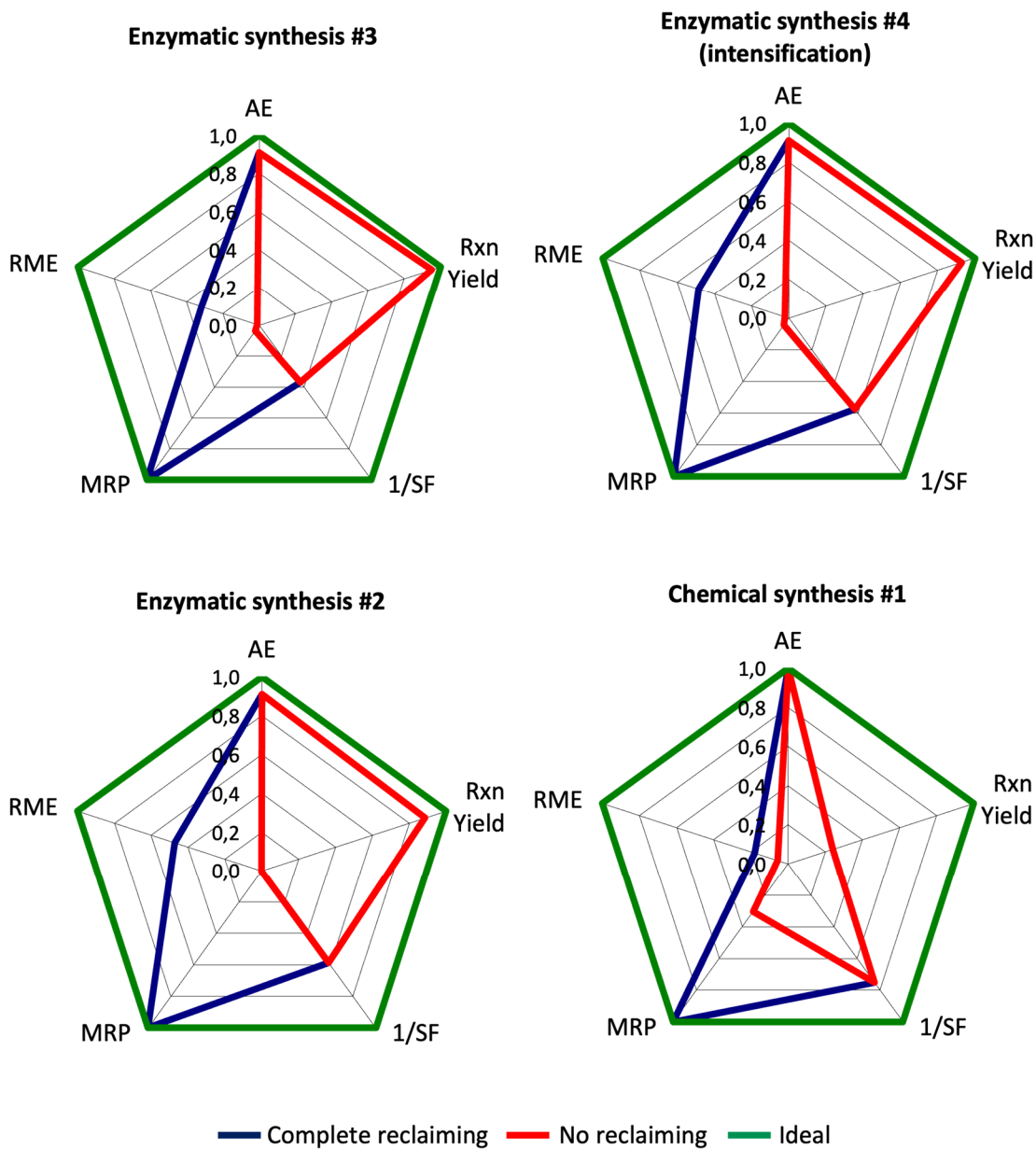


**Figure S6.** HPLC purity (%) determination of L-Th synthesized at pH 11.6. 1= L-Gln; 2 =L-Ser (internal standard); 3= L-Th; 4= Sanger's reagent; 5= derivatization artifact; 6= ethylamine.

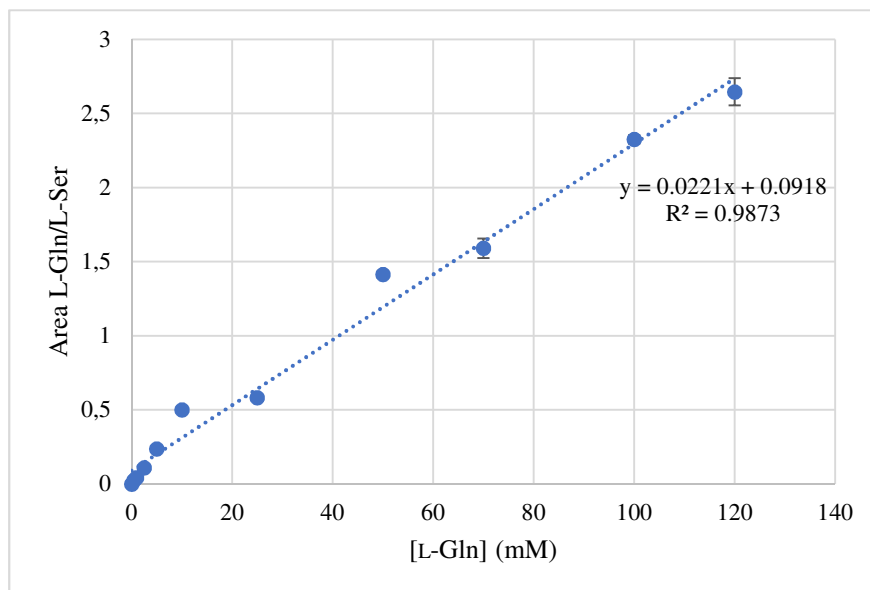


**Figure S7.** ESI-MS of L-Th synthesized at pH 11.6.

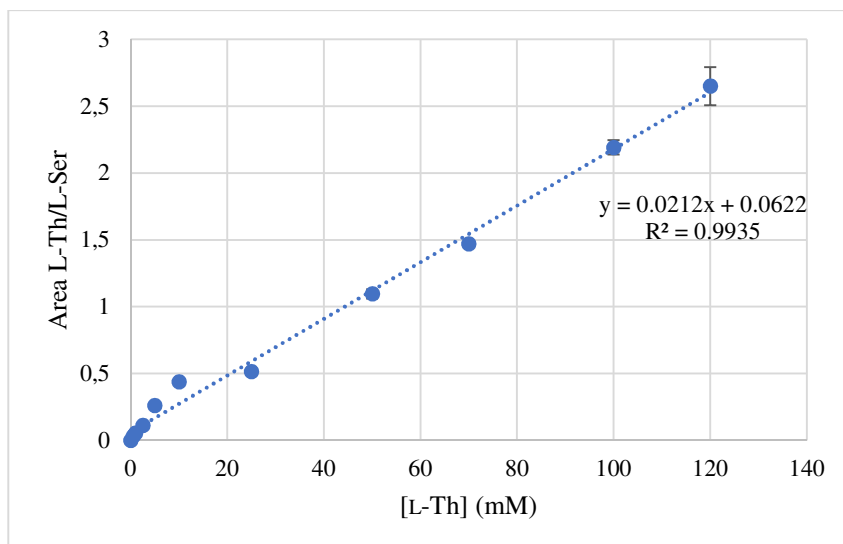




**Figure S8.** Radial pentagon representation for the syntheses of L-Th discussed in the text (#1-4).



**Figure S9.** HPLC calibration curve of L-Gln.



**Figure S10.** HPLC calibration curve of L-Th.

**Table S1.** Chemometric parameters for the preparative synthesis of L-Th reported in this work (Synth. #3).

Parameter	Complete Reclaiming	Partial Reclaiming	No Reclaiming	Ideal
AE	0.911	0.911	0.911	1
Rxn Yield	0.950	0.950	0.950	1
1/SF	0.368	0.368	0.368	1
MRP	1	0.036	0.036	1
RME	0.319	0.012	0.012	1

**Table S2.** Chemometric parameters for the intensified synthesis of L-Th reported in this work (Synth. #4).

Parameter	Complete Reclaiming	Partial Reclaiming	No Reclaiming	Ideal
AE	0.911	0.911	0.911	1
Rxn Yield	0.929	0.929	0.929	1
1/SF	0.575	0.575	0.575	1
MRP	1	0.045	0.045	1
RME	0.487	0.022	0.022	1

**Table S3.** Chemometric parameters for the enzymatic synthesis by Xu et al.<sup>[26]</sup> (Synth. #2).

Parameter	Complete Reclaiming	Partial Reclaiming	No Reclaiming	Ideal
AE	0.911	0.11	0.911	1
Rxn Yield	0.885	0.885	0.885	1
1/SF	0.586	0.586	0.586	1
MRP	1	0.003	0.003	1
RME	0.472	0.001	0.001	1

**Table S4.** Chemometric parameters for the chemical synthesis by Zhang et al.<sup>[16]</sup> before recrystallization (Synth. #1).

Parameter	Complete Reclaiming	Partial Reclaiming	No Reclaiming	Ideal
AE	1.000	1.000	1.000	1
Rxn Yield	0.784	0.784	0.784	1
1/SF	0.752	0.752	0.752	1
MRP	1	0.305	0.305	1
RME	0.589	0.180	0.180	1

**Table S5.** Chemometric parameters for the chemical synthesis by Zhang et al.<sup>[16]</sup> after recrystallization (Synth. #1).

Parameter	Complete Reclaiming	Partial Reclaiming	No Reclaiming	Ideal
AE	1.000	1.000	1.000	1
Rxn Yield	0.240	0.240	0.240	1
1/SF	0.752	0.752	0.752	1
MRP	1	0.305	0.305	1
RME	0.181	0.055	0.055	1

RME= reaction AE= atom economy; Rxn yield= reaction yield (between 0 and 1); 1/SF= 1/stoichiometric factor (SF= 1 for stoichiometric reactions; SF >1 when excess of reagents is used); MRP= material recovery parameter; mass efficiency.

$$E^+ = E + \frac{W \times CI}{\text{mass of desired product (kg)}}$$

$W = \text{electrical power used (kWh)}$   
 $CI = \text{carbon intensity } \frac{\text{kg (CO}_2\text{)}}{\text{kWh}}$

$$\text{(C)limate Factor} = \frac{\text{total mass of CO}_2 \text{ emitted}}{\text{mass of product formed}} \quad (\text{kg CO}_2 / \text{kg product})$$

**Case 1. This paper (Synth. #3)**

Reaction is carried out by stirring at **25 °C** (which can be considered room temperature) for **6 h**

The estimated consumption for stirring at r.t. is 10 W (from different commercial stirrers)

Then:

$$10 \text{ W} \times 6 \text{ h} = 60 \text{ W}\cdot\text{h} = 0.060 \text{ KW}\cdot\text{h}$$

According to OECD average (2015) the equivalency is 404 g CO<sub>2</sub>/KW·h.<sup>[60]</sup>

$$\text{Therefore } 0.060 \text{ KW}\cdot\text{h} \times 404 \text{ g CO}_2/\text{KW}\cdot\text{h} = \mathbf{24.24 \text{ g CO}_2}$$

$$\mathbf{C-Factor} = 24.24 \text{ g CO}_2 / (0.248 \text{ g}) = 97.742 \approx \mathbf{98}$$

**Case 2. This paper (Synth. #4)**

Reaction is carried out by stirring at **25 °C** (which can be considered room temperature) for **6 h**

The estimated consumption for stirring at r.t. is 10 W (from different commercial stirrers)

Then:

$$10 \text{ W} \times 6 \text{ h} = 60 \text{ W}\cdot\text{h} = 0.060 \text{ KW}\cdot\text{h}$$

According to OECD average (2015) the equivalency is 404 g CO<sub>2</sub>/KW·h.<sup>[60]</sup>

$$\text{Therefore } 0.060 \text{ KW}\cdot\text{h} \times 404 \text{ g CO}_2/\text{KW}\cdot\text{h} = \mathbf{24.24 \text{ g CO}_2}$$

$$\mathbf{C-Factor} = 24.24 \text{ g CO}_2 / (0.485 \text{ g}) = 49.979 \approx \mathbf{50}$$

**Case 3. Enzymatic synthesis (Synth. #2)<sup>[26]</sup>**

Reaction is carried out by ultrasound power **100 Wat** for **16 h**

Then:

$$100 \text{ W} \times 16 \text{ h} = 1600 \text{ W}\cdot\text{h} = 1.6 \text{ KW}\cdot\text{h}$$

According to OECD average (2015) the equivalency is 404 g CO<sub>2</sub>/KW·h.<sup>[60]</sup>

$$\text{Therefore } 1.6 \text{ KW}\cdot\text{h} \times 404 \text{ g CO}_2/\text{KW}\cdot\text{h} = \mathbf{646.4 \text{ g CO}_2}$$

$$\mathbf{C-Factor} = 646.4 \text{ g CO}_2 / (18.61 \text{ g}) = 34.734 \approx \mathbf{35}$$

**Case 4. Chemical synthesis (Synth. #1)<sup>[16]</sup>**

**a) Before recrystallization**

Reaction is carried out by heating at **35 °C** for **10 days**

The estimated consumption for heaters is 300 W (from different commercial stirrers)

Then:

$$300 \text{ W} \times 240 \text{ h} = 72000 \text{ W}\cdot\text{h} = 72 \text{ KW}\cdot\text{h}$$

According to OECD average (2015) the equivalency is 404 g CO<sub>2</sub>/KW·h.<sup>[60]</sup>

$$\text{Therefore } 72 \text{ KW}\cdot\text{h} \times 404 \text{ g CO}_2/\text{KW}\cdot\text{h} = 29088 \text{ g CO}_2 \approx \mathbf{29 \text{ kg CO}_2}$$

$$\mathbf{C-Factor} = 29088 \text{ g CO}_2 / (37.01 \text{ g}) = 785.94 \approx \mathbf{786}$$

### b) After recrystallization

For recrystallization: the residual mixture was dissolved in warm (**45 °C**) water and allowed to crystallize in 84% ethanol at **4 °C** for **5-7 days**

- No indication of warming time. Assumption: 1 h
- The estimated consumption for heaters is 300 W (from different commercial stirrers)
- Then:
- $300 \text{ W} \times 1 \text{ h} = 300 \text{ W}\cdot\text{h} = 0.3 \text{ KW}\cdot\text{h}$
- According to OECD average (2015) the equivalency is  $404 \text{ g CO}_2/\text{KW}\cdot\text{h}$ .<sup>[60]</sup>
- Therefore  $0.3 \text{ KW}\cdot\text{h} \times 404 \text{ g CO}_2/\text{KW}\cdot\text{h} = \mathbf{121.2 \text{ g CO}_2}$
  
- Cooling at 4 °C, time 6 days (between 5 and 7) = 144 h
- The estimated consumption for heaters/coolers is 300 W (from different commercial stirrers)
- Then:
- $300 \text{ W} \times 144 \text{ h} = 43200 \text{ W}\cdot\text{h} = 43.2 \text{ KW}\cdot\text{h}$
- According to OECD average (2015) the equivalency is  $404 \text{ g CO}_2/\text{KW}\cdot\text{h}$ .<sup>[60]</sup>
- Therefore  $43.2 \text{ KW}\cdot\text{h} \times 404 \text{ g CO}_2/\text{KW}\cdot\text{h} = 17452.8 \text{ g CO}_2 = \mathbf{17.45 \text{ kg CO}_2}$

OVERALL upon RECRYSTALLIZATION: 17.57 kg CO<sub>2</sub> (0.121 kg +17.45 kg)

**TOTAL PROCESS** (Reaction plus recrystallization) = 29 kg + 17.57 kg ≈ **46.6 kg CO<sub>2</sub>**

**C-Factor** =  $46600 \text{ g CO}_2 / (37.01 \text{ g}) = 1256.1 \approx \mathbf{1256}$