

1 Efficient Enzymatic Preparation of Flavor Esters in Water

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7 **ABSTRACT:** A straightforward biocatalytic method for the enzymatic preparation of different flavor esters starting from
 8 primary alcohols (e.g., isoamyl, *n*-hexyl, geranyl, cinnamyl, 2-phenethyl, and benzyl alcohols) and naturally available ethyl esters
 9 (e.g., formate, acetate, propionate, and butyrate) was developed. The biotransformations are catalyzed by an acyltransferase
 10 from *Mycobacterium smegmatis* (MsAcT) and proceeded with excellent yields (80–97%) and short reaction times (30–120
 11 min), even when high substrate concentrations (up to 0.5 M) were used. This enzymatic strategy represents an efficient
 12 alternative to the application of lipases in organic solvents and a significant improvement compared with already known
 13 methods in terms of reduced use of organic solvents, paving the way to sustainable and efficient preparation of natural flavoring
 14 agents.

15 **KEYWORDS:** *flavor esters, enzymatic acylation, biocatalysis, acyltransferase, Mycobacterium smegmatis (MsAcT)*

16 ■ INTRODUCTION

17 Many esters are components of natural flavors and are used as
 18 flavor and fragrance in food, drinks, and cosmetics.¹ Their
 19 preparation starting from natural substrates and using
 20 bioprocesses (e.g., fermentation or enzymatic reactions) is
 21 appealing, because the final product can be labeled and
 22 commercialized in the European Union and the United States
 23 as natural.^{2,3} Therefore, new biotechnological approaches for
 24 obtaining flavors are highly demanded as long as they are
 25 efficient and sustainable.^{4,5} Many flavor and fragrance esters
 26 can be enzymatically obtained using lipases that catalyze
 27 esterification, transesterification, or interesterification reactions
 28 in media (e.g., organic solvents) characterized by low water
 29 activity.^{6–8} The presence of water is critical for the equilibrium
 30 of lipase-catalyzed reactions in organic media, strongly limiting
 31 the overall yields. In fact, water may compete as a nucleophile
 32 with the alcohol in the attack of the acyl–enzyme intermediate,
 33 thus favoring hydrolysis over transesterification,^{9–11} and for
 34 this reason, water must be avoided or removed during the
 35 reaction to achieve high yields.^{12,13} Flavor-ester biosynthesis in
 36 an aqueous system composed of coconut cream and fusel oil
 37 was achieved with limited conversion (14.25 mg/g, based on
 38 cream weight), after optimization of the process catalyzed by
 39 the lipase Palatase.¹⁴ The potential of lipases for flavor-ester
 40 production has also been exploited using immobilized
 41 enzymes¹⁵ and whole microbial cells;^{16–18} these systems
 42 have been especially employed for setting up robust processes
 43 and facilitating product recovery. Acetate esters are among the
 44 most valuable flavor esters, and few of them have been
 45 produced in hydrophobic solvents (e.g., *n*-pentane, *n*-hexane,
 46 or *n*-heptane) using different immobilized lipases;¹⁹ in a large
 47 scale production of flavor esters, Novozym 435 (35 g/L) was
 48 able to give yields ranging between 91 and 95% after 24 h,
 49 starting from an alcohol concentration of 1.0 M and an excess
 50 of acetic acid.¹² Alternatively, the use of *Candida rugosa* lipase,

immobilized in calcium alginate gel, allowed for a productivity
 of 1600–2200 $\mu\text{mol/h}$ per gram of biocatalyst for the
 preparation of isoamyl and butyryl acetate.²⁰

An interesting enzymatic alternative for preparing esters is
 the use of the acyltransferase from *Mycobacterium smegmatis*
 (MsAcT).²¹ MsAcT is characterized by a hydrophobic tunnel
 leading to the active site, where water access is disfavored;^{21,22}
 moreover, MsAcT is functionally active as a closely aggregated
 octamer in aqueous solution.²¹ This overall architecture means
 that MsAcT is able to favor transesterification reactions with
 respect to hydrolysis even in water, unlike lipases that catalyze
 transesterification only under conditions of low water
 activity.²² For these structural reasons, MsAcT has been used
 for catalyzing transesterification reactions of primary and
 secondary alcohols with ethyl acetate in aqueous buffers, often
 with good enantioselectivity.^{22–24} The ratio between the
 catalytic rate constants of the hydrolysis and synthesis of
 benzyl acetate were compared, showing that MsAcT is indeed
 an effective acetyltransferase rather than a hydrolytic enzyme.²⁴
 At reasonably high concentrations of the ester, the reaction
 mixtures of these biotransformations are actually two-liquid-
 phase systems composed of the hydrophobic ester and water,
 and the reaction occurs in the aqueous phase. The peculiar
 features of this enzyme make it also suitable for catalyzing
 amide synthesis in aqueous media.^{25,26}

In this work, we have explored the potential of MsAcT for
 flavor-ester preparation; the enzyme was able to work in two-
 liquid-phase systems composed of sparingly water-soluble
 esters and water, accomplishing the reaction in the aqueous
 phase. Several (24) different flavor esters derived from 80

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Table 1. Acetylation of Geraniol at Different Initial Concentrations Using MsAcT (1.0 mg/mL, 110 U/mL) in the Presence of EtOAc (10%, v/v) in Phosphate Buffer (0.1 M, pH 8.0) at 25 °C

geraniol (mM)	initial rate ($\mu\text{mol}/\text{mg}/\text{min}$)	maximum conversion (%) ^a	maximum product yield (mg/mL)	time (h) ^b
100	2.25	>98	19.6	2
200	4.56	>98	39.2	24
250	6.36	98	48.1	24
300	6.57	95	55.9	24
400	7.68	79	62.0	48
500	7.65	68	66.7	48

^aAs determined by gas chromatography. ^bTime refers to the maximum conversion observed.

81 transesterification of primary alcohols (e.g., isoamyl, *n*-hexyl,
82 geranyl, benzyl, 2-phenylethyl, and cinnamyl) with ethyl esters
83 bearing short-chain acyl groups (e.g., formyl, acetyl, propionyl,
84 and butyryl) were prepared in excellent yields with short
85 reaction times when high concentrations of substrates (up to
86 500 mM) were loaded, making the process interesting at
87 industrial level.

88 ■ MATERIALS AND METHODS

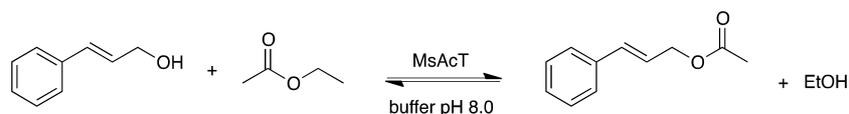
89 **Chemicals.** All reagents and solvents were obtained from
90 commercial suppliers and were used without further purification.

91 **Preparation of the Acetyltransferase from *Mycobacterium***
92 ***smegmatis* (MsAcT).** *Escherichia coli* BL21 star (DE3) was used as
93 the host for the production of the recombinant protein; cloning was
94 carried out as described before, starting from a synthetic gene
95 encoding for MsAcT (GenBank accession: ABK70783) from *M.*
96 *smegmatis* strain MC2 155.²⁶ Recombinant *E. coli* was first grown at
97 37 °C in Luria–Bertani (LB) liquid medium in the presence of 25 $\mu\text{g}/$
98 mL kanamycin for 16 h; this starting culture was used to inoculate the
99 cultivation medium (Terrific Broth: 12 g/L bacto-tryptone, 24 g/L
100 yeast extract, 4 g/L glycerol, 17 mM KH_2PO_4 , 72 mM K_2HPO_4 , 25
101 $\mu\text{g}/\text{mL}$ kanamycin), which was brought to an initial $\text{OD}_{600\text{nm}}$ of 0.1.
102 Cultivation was carried out at 37 °C in orbital shakers with an
103 agitation speed 110 rpm; cells were grown until an $\text{OD}_{600\text{nm}}$ of 0.5–
104 0.6. The expression of MsAcT was induced by adding isopropyl- β -D-
105 thiogalactopyranoside (IPTG) to a final concentration of 0.1 mM.
106 The culture was further incubated for 16 h at 25 °C. Wet cells (2.0 g)
107 were then harvested by centrifugation (20 min, 9000 rcf at 4 °C),
108 washed with 20 mM phosphate buffer (pH 8.0), resuspended in 10
109 mL of buffer (100 mM phosphate buffer, pH 8.0; 6 mM imidazole;
110 100 mM NaCl), and sonicated (5 cycles of 1 min on and 1 min off at
111 4 °C). Cell debris were recovered by centrifugation (45 min, 36 000
112 rcf at 4 °C). The enzyme was purified by affinity chromatography with
113 HIS-Select Nickel Affinity Gel. The fractions showing activity were
114 pooled and dialyzed against phosphate buffer (100 mM, pH 8.0) and
115 stored at 4 °C; 96 mg of pure protein was obtained. Activity was
116 spectrophotometrically evaluated at 400 nm by determining the
117 release of *p*-nitrophenol after hydrolysis of *p*-nitrophenylacetate at 25
118 °C in a half-microcuvette (volume of 1 mL) for 2 min. One unit (U)
119 of activity is defined as the amount of enzyme that catalyzes the
120 consumption of 1 μmol of *p*-nitrophenylacetate per minute. Reference
121 conditions were 0.1 mg/mL *p*-nitrophenylacetate, 0.1% (v/v) EtOH,
122 and different amounts of MsAcT in 100 mM phosphate buffer (pH
123 8.0). The specific activity of the purified enzyme was 110 U/mg.

124 **Preparation of Flavor Esters.** Standard transesterification
125 reactions were carried out in 10 mL screw cap tubes: alcohols (250
126 mM) and ethyl esters (10%, v/v) were added to 2.5 mL of phosphate
127 buffer (100 mM, in the range of pH 8.0) containing MsAcT as
128 purified enzyme (0.1–1.5 mg/mL); the reaction was left under
129 magnetic stirring at 25 °C. The reactions were stopped after 24 h and
130 extracted with EtOAc (2 \times 8 mL); the organic phases were collected,
131 dried over Na_2SO_4 and evaporated. Products were purified by flash

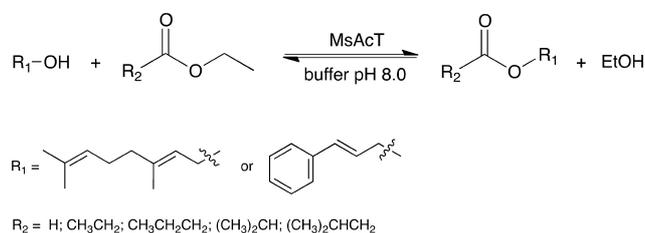
132 chromatography (eluent: *n*-hexane/EtOAc), and their structures and
133 purities were determined via ¹H NMR analysis by comparison with
134 commercially available samples. Optimization of geranyl and cinnamyl
135 acetate synthesis was carried out using a 1 mL reaction mixture in
136 phosphate buffer (100 mM, in the range of pH between 5.0 and 8.0)
137 containing geraniol or cinnamyl alcohol (25–500 mM), MsAcT
138 (0.1–1.5 mg/mL) and a fixed amount of ethyl acetate (10%, v/v); the
139 solution was left under magnetic stirring at different temperatures
140 (20–40 °C). Aliquots (50 μL) were withdrawn at different reaction
141 times and extracted twice with EtOAc (2 \times 100 μL), and the collected
142 organic phase was dried over Na_2SO_4 . Preparative biotransformations
143 at the multimilligram scale aimed at synthesizing geranyl acetate and
144 cinnamyl acetate were carried out using geraniol (250 mM) and
145 cinnamyl alcohol (250 mM) dissolved in 9 mL of phosphate buffer
146 (0.1 M, pH 8.0) in the presence of 10 mg of MsAcT and 1 mL of
147 EtOAc at 25 °C. The reactions were stopped after 24 h and extracted
148 with EtOAc (2 \times 8 mL); the organic phases were collected, dried over
149 Na_2SO_4 , and evaporated. Products were purified by flash chromatog-
150 raphy; 442 mg (90% yield) of geranyl acetate (eluent: *n*-hexane/
151 EtOAc, 98:2; chemical purity >98%) and 410 mg (93% yield) of pure
152 cinnamyl acetate (eluent: *n*-hexane/EtOAc, 95:5; chemical purity
153 >98%) were obtained. Purity of the product was confirmed by ¹H
154 NMR and gas-chromatography analysis.

Analysis of the Biotransformations. Aliquots of the bio-
155 transformation medium (100 μL) were withdrawn at different
156 reaction times, quenched with 5 μL of 0.5 M sulfuric acid and
157 extracted with 100 μL of ethyl acetate. The amounts of produced
158 flavor esters and the residual quantity of alcohol substrates were
159 determined by gas-chromatographic (GC) analysis. Geraniol,
160 cinnamyl alcohol, *n*-hexanol, benzyl alcohol, 2-phenylethanol, and
161 their esters were analyzed by gas-GC analysis on a Carlo Erba
162 Fractovap GC equipped with a fused-silica capillary column MEGA-
163 SE30 (100% methyl polysiloxane; 25 m \times 0.25 mm i.d.), with the
164 injector temperature at 200 °C. Oven temperatures ranged from 45 to
165 180 °C. The retention times for geraniol and its esters (temperature
166 gradient: from 80 to 180 °C at 5 °C/min) were as follows: geraniol,
167 7.3 min; geranyl formate, 10.2 min; geranyl acetate, 10.2 min; geranyl
168 propionate, 12.5; and geranyl butyrate, 14.5 min. The retention times
169 for cinnamyl alcohol and its esters (temperature gradient: 80 °C for 2
170 min then from 80 to 180 °C with a 5 °C/min gradient) were as
171 follows: cinnamyl alcohol, 9.9 min; cinnamyl formate, 10.7 min;
172 cinnamyl acetate, 13.2 min; cinnamyl propionate, 15.5 min; and
173 cinnamyl butyrate 17.8 min. The retention times for *n*-hexanol and its
174 esters (temperature gradient: 50 °C for 10 min then from 50 to 150
175 °C with a 10 °C/min gradient) were as follows: *n*-hexanol, 5.3 min; *n*-
176 hexyl formate, 7.7 min; *n*-hexyl acetate, 8.8 min; *n*-hexyl propionate,
177 15.2 min; and *n*-hexyl butyrate, 16.8 min. The retention times for
178 benzyl alcohol, 2-phenylethanol, and their esters (temperature
179 gradient: from 80 to 180 °C with a 10 °C/min gradient) were as
180 follows: benzyl alcohol, 3.0 min; benzyl formate, 3.4 min; benzyl
181 acetate, 4.2 min; benzyl propionate, 5.0 min; benzyl butyrate, 6.5 min;
182 2-phenylethanol, 3.7 min; 2-phenylethyl formate, 4.3 min; 2-
183 phenylethyl acetate, 5.4 min; 2-phenylethyl propionate, 6.6 min; 184

Table 2. Acetylation of Cinnamyl Alcohol at Different Initial Concentrations Using MsAcT (1.0 mg/mL, 110 U/mL) in the Presence of EtOAc (10%, v/v) in Phosphate Buffer (0.1 M, pH 8.0) at 25 °C

cinnamyl alcohol (mM)	initial rate ($\mu\text{mol}/\text{mg}/\text{min}$)	maximum conversion (%) ^a	maximum product yield (mg/mL)	time (h) ^b
100	2.54	>98	17.6	1
200	5.07	>98	35.2	3
250	6.32	>98	44.0	6
300	6.82	92	48.6	24
400	8.53	84	59.2	24
500	8.65	79	69.6	24

^aAs determined by gas chromatography. ^bTime refers to the maximum conversion observed.

Table 3. Acylation of Geraniol (250 mM) and Cinnamyl Alcohol (250 mM) Using MsAcT (1.0 mg/mL, 110 U/mL) in the Presence of Different Ethyl Esters (10%, v/v) in Phosphate Buffer (0.1 M, pH 8.0) at 25 °C

alcohol	ester	ester main flavor property ¹	initial rate ($\mu\text{mol}/\text{mg}/\text{min}$)	conversion (%) ^a	time (h) ^b
geraniol	ethyl formate	rose	7.69	>98	3
geraniol	ethyl propionate	fruity	1.51	86	48
geraniol	ethyl butyrate	fruity, apricot	1.15	62	48
geraniol	ethyl isobutyrate	rose, apricot	1.42	74	48
geraniol	ethyl isovalerate	rose, sweet apple	0.88	38	48
cinnamyl alcohol	ethyl formate	fruity, apple	7.72	>98	1
cinnamyl alcohol	ethyl propionate	fruity, woody	2.13	>98	3
cinnamyl alcohol	ethyl butyrate	fruity, honey	1.87	90	24
cinnamyl alcohol	ethyl isobutyrate	fruity, apple–banana	1.92	87	24
cinnamyl alcohol	ethyl isovalerate	rose, apple	0.91	44	48

^aAs determined by gas chromatography. ^bTime refers to the maximum conversion observed.

185 and 2-phenylethyl butyrate, 7.8 min. Conversions of isoamyl alcohol
186 into its esters were determined by GC analysis on a Carlo Erba
187 Fractovap GC equipped with a fused-silica capillary column MEGA-
188 DEX DMP-Beta (dimethyl pentyl- β -cyclodextrin, 25 m \times 0.25 mm
189 i.d.), with the injector temperature at 200 °C. The retention times
190 (temperature gradient: from 40 to 180 °C at 5 °C/min) were as
191 follows: isoamyl alcohol, 6.7 min; isoamyl formate, 5.8 min; isoamyl
192 acetate, 7.1 min; isoamyl propionate, 9.4 min; and isoamyl butyrate,
193 11.5 min. Initial rates were defined as the amount (μmol) of ester
194 produced after 30 min per amount of enzyme.

195 ■ RESULTS AND DISCUSSION

196 The reaction between geraniol and ethyl acetate (EtOAc)
197 using the acyltransferase from *M. smegmatis* (MsAcT) as
198 biocatalyst was studied in a two-liquid-phase system composed
199 of water and EtOAc; the product (geranyl acetate) presents a
200 green-type flavor and a floral-type odor.¹ Different parameters
201 (pH, temperature, and enzyme concentration) were optimized,
202 while the amount of geraniol (0.065 mM) and the phase ratio
203 between water and EtOAc (9:1) were kept fixed; a Multi-
204 simplex optimization design was employed²⁷ using initial rate
205 and molar conversions after 30 min as response variables. The
206 best results (corresponding to conversions >98% after 30 min)
207 were obtained using 1.0 mg/mL MsAcT at pH 8.0 and 25 °C;

under these conditions, the production of the ester was studied 208
using different initial geraniol concentrations (Table 1). 209 t1

The highest rates of geranyl acetate synthesis were achieved 210
at geraniol concentrations between 400 and 500 mM, whereas 211
almost quantitative yields were obtained only at alcohol 212
concentrations lower than 300 mM. Possible product 213
inhibition was evaluated by assessing the activity of MsAcT 214
in the presence of increasing concentrations of EtOH and 215
geranyl acetate (0–500 M); the activity of the enzyme was 216
assayed (with *p*-nitrophenyl acetate) in the presence of 217
concentrations of EtOH between 250 and 500 mM and 218
showed that the enzyme was 40–50% inhibited, whereas no 219
significant effects were observed with geranyl acetate. 220

The best compromise between rates and conversion was 221
observed starting from 250 mM geraniol, allowing for 98% 222
conversion (48.1 mg/mL analytical yield) after 24 h. Notably, 223
good conversion (68%) after 48 h was achieved even when the 224
biotransformation was carried out starting from 500 mM 225
geraniol, allowing for the accumulation of 66.7 mg/mL geranyl 226
acetate. 227

A similar evaluation of the effect of substrate concentration 228
was carried out in the case of the acetylation of cinnamyl 229

Table 4. Acylation of Different Primary Alcohols (100–500 mM Starting Concentrations) with Short-Chain Ethyl Esters Using MsAcT (1.0 mg/mL, 110 U/mL) in the Presence of Different Ethyl Esters (10%, v/v) in Phosphate Buffer (100 mM, pH 8.0) at 25 °C

$$R_1-CH_2-OH + R_2-COOEt \xrightarrow[\text{buffer pH 8.0}]{\text{MsAcT}} R_1-CH_2-O-C(=O)-R_2 + EtOH$$

R ₁	initial alcohol (mM)	R ₂	ester main flavor property ¹	conversion (%) ^a	time (h) ^b
(CH ₃) ₂ CHCH ₂ -	100	H-	black currant, currant	93	0.5
(CH ₃) ₂ CHCH ₂ -	250	H-		93	0.5
(CH ₃) ₂ CHCH ₂ -	500	H-		86	1
(CH ₃) ₂ CHCH ₂ -	100	CH ₃ -	banana, pear	94	0.5
(CH ₃) ₂ CHCH ₂ -	250	CH ₃ -		95	0.5
(CH ₃) ₂ CHCH ₂ -	500	CH ₃ -		88	0.5
(CH ₃) ₂ CHCH ₂ -	100	CH ₂ CH ₃ -	pineapple-apricot, apricot	97	0.5
(CH ₃) ₂ CHCH ₂ -	250	CH ₂ CH ₃ -		97	1
(CH ₃) ₂ CHCH ₂ -	500	CH ₂ CH ₃ -		95	1
(CH ₃) ₂ CHCH ₂ -	100	CH ₂ CH ₂ CH ₃ -	fruity	94	24
(CH ₃) ₂ CHCH ₂ -	250	CH ₂ CH ₂ CH ₃ -		93	24
(CH ₃) ₂ CHCH ₂ -	500	CH ₂ CH ₂ CH ₃ -		92	24
CH ₃ (CH ₂) ₄ -	100	H-	apple	97	0.5
CH ₃ (CH ₂) ₄ -	250	H-		97	1
CH ₃ (CH ₂) ₄ -	500	H-		88	3
CH ₃ (CH ₂) ₄ -	100	CH ₃ -	fruity, pear	97	0.5
CH ₃ (CH ₂) ₄ -	250	CH ₃ -		95	1
CH ₃ (CH ₂) ₄ -	500	CH ₃ -		90	3
CH ₃ (CH ₂) ₄ -	100	CH ₂ CH ₃ -	earthy, metallic-fruity	72	1
CH ₃ (CH ₂) ₄ -	250	CH ₂ CH ₃ -		50	1
CH ₃ (CH ₂) ₄ -	250	CH ₂ CH ₃ -		35	2
CH ₃ (CH ₂) ₄ -	500	CH ₂ CH ₃ -		30	1
CH ₃ (CH ₂) ₄ -	500	CH ₂ CH ₃ -		24	2
CH ₃ (CH ₂) ₄ -	100	CH ₂ CH ₂ CH ₃ -	apricot, pineapple	94	2
CH ₃ (CH ₂) ₄ -	250	CH ₂ CH ₂ CH ₃ -		96	6
CH ₃ (CH ₂) ₄ -	500	CH ₂ CH ₂ CH ₃ -		95	24
Ph-	100	H-	floral-fruity, apricot	92	0.5
Ph-	250	H-		84	1
Ph-	500	H-		86	3
Ph-	100	CH ₃ -	jasmine	92	0.5
Ph-	250	CH ₃ -		90	1
Ph-	500	CH ₃ -		87	3
Ph-	100	CH ₂ CH ₃ -	floral-fruity, peach	96	0.5
Ph-	250	CH ₂ CH ₃ -		95	1
Ph-	500	CH ₂ CH ₃ -		89	3
Ph-	100	CH ₂ CH ₂ CH ₃ -	plum, pear	95	8
Ph-	250	CH ₂ CH ₂ CH ₃ -		92	8
Ph-	500	CH ₂ CH ₂ CH ₃ -		95	24
PhCH ₂ -	100	H-	hyacinth	95	0.5
PhCH ₂ -	250	H-		88	2
PhCH ₂ -	500	H-		86	3
PhCH ₂ -	100	CH ₃ -	rose, raspberry	96	0.5
PhCH ₂ -	250	CH ₃ -		91	0.5
PhCH ₂ -	500	CH ₃ -		82	0.5
PhCH ₂ -	100	CH ₂ CH ₃ -	red rose, strawberry	97	0.5
PhCH ₂ -	250	CH ₂ CH ₃ -		97	0.5
PhCH ₂ -	500	CH ₂ CH ₃ -		96	0.5
PhCH ₂ -	100	CH ₂ CH ₂ CH ₃ -	rose, honey	97	4
PhCH ₂ -	250	CH ₂ CH ₂ CH ₃ -		97	8
PhCH ₂ -	500	CH ₂ CH ₂ CH ₃ -		90	24
PhCH=CHCH ₂ -	100	H-	fruity, apple	>98	0.5
PhCH=CHCH ₂ -	250	H-		>98	4
PhCH=CHCH ₂ -	500	H-		82	24
PhCH=CHCH ₂ -	100	CH ₃ -	floral, pineapple	>98	1
PhCH=CHCH ₂ -	100	CH ₃ -		>98	4
PhCH=CHCH ₂ -	250	CH ₃ -		96	24

Table 4. continued

R ₁	initial alcohol (mM)	R ₂	ester main flavor property ¹	conversion (%) ^a	time (h) ^b
PhCH=CHCH ₂ -	100	CH ₃ CH ₂ -	fruity, woody	>98	1
PhCH=CHCH ₂ -	250	CH ₃ CH ₂ -		>98	5
PhCH=CHCH ₂ -	500	CH ₃ CH ₂ -		97	24
PhCH=CHCH ₂ -	100	CH ₃ CH ₂ CH ₂ -	fruity, honey	>98	16
PhCH=CHCH ₂ -	250	CH ₃ CH ₂ CH ₂ -		92	24
PhCH=CHCH ₂ -	500	CH ₃ CH ₂ CH ₂ -		80	48

^aAs determined by gas chromatography. ^bTime refers to the maximum conversion observed.

alcohol (Table 2). Cinnamyl acetate has a balsamic–floral odor and a pineapple flavor.¹

Enzymatic acetylation of cinnamyl alcohol occurred with generally better rates and yields than those observed with geraniol, allowing for almost complete conversion of the alcohol up to 250 mM initial concentration after 6 h. In the case of the reaction carried out with the highest initial concentration of alcohol (500 mM), 79% molar conversion was obtained after 48 h.

Acetylation of geraniol and cinnamyl alcohol was performed on semipreparative scale (10 mL) starting from 250 mM alcohol concentration; the reactions were stopped and worked up when conversions reached the maximum yield, allowing for the recovery of 442 mg of geranyl acetate (90% recovered yield) and 410 mg of cinnamyl acetate (93% yield), respectively.

Acylation of geraniol and cinnamyl alcohol was then studied with other acyl donors that varied in acyl-chain length; the results of the biotransformations carried out under optimized conditions (alcohol, 250 mM; acyl donor, 10%, v/v; enzyme, 1.0 mg/mL; buffer, pH 8.0; 25 °C) are summarized in Table 3.

The ability to act as an acyl donor decreased as the acyl-chain length increased; geranyl formate was obtained in quantitative yield after 1–3 h, whereas with geranyl propionate and butyrate, the maximum yields (ranging between 65 and 98%) were reached only after 1–2 days.

Enzymatic acylation was then studied with different primary alcohols and different acyl donors; all the reactions studied were aimed at preparing esters used as flavor or fragrance components (Table 4). Biotransformations were carried out starting from 100, 250, and 500 mM alcohol concentrations.

Formylation and acetylation of all the tested primary alcohols allowed for quantitative or almost quantitative conversions with high rates (≥90% within 30–60 min) when the initial concentration of alcohols was kept between 100 and 250 mM. When the biotransformation was carried out with higher alcohol concentration (500 mM), still high molar conversions of the flavor-esters were observed (from 80 up to >98%), albeit with longer reaction times. Slower reactions were generally found with acyl donors of increased chain length (propionyl- and butyryl-). The only biotransformation occurring with relatively low yields (30–70%, depending on the initial concentration) was the propionylation of *n*-hexanol to give *n*-hexyl propionate; interestingly, in this case, hydrolysis of the formed ester was predominant after reaching its maximum accumulation, as noticeable from an increase in the alcohol concentration (data not shown).

In conclusion, a highly efficient preparation of different flavor-esters was achieved using the acyltransferase from *M. smegmatis* (MsAcT), which catalyzes the acylation of different primary alcohols in aqueous systems. The results collected so far indicate that the biotransformation can not only be applied

to the production of acetate esters but can also be expanded to a range of other acyl donors (e.g., ethyl formate, propionate, butyrate) useful for the formation of different flavor and fragrance esters, making this process strongly versatile. Notably, all the primary alcohols tested were accepted as substrates, even at higher concentrations (up to 500 mM); preparation of geranyl acetate and cinnamyl acetate was carried out on a semipreparative scale (10 mL) starting from 250 mM alcohol concentration, allowing for the recovery of 44.2 mg/mL (geranyl acetate) and 41.0 mg/mL (cinnamyl acetate) products. Biocatalysis is sometimes perceived to be inefficient compared with conventional chemical processes because of the low productivity, mostly because of substrate or product inhibition of the enzymatic activity, which often occurs at somewhat low concentrations. To become an industrially attractive technology, a biocatalytic process must be engineered to improve space–time yields.²⁸ In this work, we have described that the use of relatively low amounts of MsAcT allowed the conversion of remarkably high substrate concentrations with good yields. The proposed enzymatic method may pave the way for an efficient and environmentally sustainable preparation of natural esters; the biotransformation may be further intensified by immobilizing the enzyme and carrying out continuous processes in suited reactors,²⁹ thus making it appealing at an industrial level.

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Notes

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