

26 Transportation of the whey was one of the main hotspots in the life cycle assessment
27 performed (28–70%); electricity use accounted for 18–20% of the impact. The
28 alternative scenario, that involves the pre-concentration of whey, obtained a reduction
29 of the impacts from 0.9% to 14.3%. The pre-concentration of whey in a pretreatment
30 plant closer to the cheese factory reduces the environmental burden of the whole
31 process. This occurs even if the energy consumption for pre-concentration increases
32 due to the use of smaller and less efficient devices.

33

34 **Keywords:** cheese-making, coproducts, dairy production processes, environmental
35 assessment, protein, reverse osmosis

36 **1 Introduction**

37 Whey is a coproduct of cheese-making and casein manufacture in the dairy industry
38 (Smithers, 2008) and is considered a waste stream. Whey is rich in lactose (0.18–60 kg
39 m³), proteins (1.4–33.5 kg/m³) and fats (0.08–10.58 kg/m³), and this organic matter is
40 around 99% biodegradable (Madureira et al., 2010; Prazeres et al., 2012). The volume of
41 effluents produced in the cheese manufacturing industry has increased with the
42 increase in cheese production (Prazeres et al., 2012), and its proper disposal has
43 become a compelling issue.

44 Recently, the introduction in many countries of restrictive legislation regarding food
45 waste treatment and the possibility of taking advantage of the interesting properties of
46 whey components have contributed to the consideration of whey as a valuable and
47 prized raw material instead of a waste (Smithers, 2008). Beneficial new uses for whey
48 are possible from new technologies such as microfiltration, ultrafiltration and reverse
49 osmosis that make separation and concentration of the whey protein component
50 highly efficient. In particular, ultrafiltration is a pressure-driven membrane separation
51 process, largely utilized in the dairy industry (Luján-Facundo et al., 2017), which is
52 successfully used to recover whey proteins (whey protein concentrate, WPC) and
53 separate smaller compounds in the permeate stream such as lactose, vitamins and
54 minerals (Rebouillat and Ortega-Requena, 2015), while ion exchange and reverse
55 osmosis are principally used to purify and concentrate lactose (Prazeres et al., 2012).

56 Whey proteins account for only about 20% (weight/weight) of the whole milk protein
57 inventory, whereas caseins account for most of it. The major components among whey
58 proteins are β -lactoglobulin, α -lactalbumin, bovine serum albumin and immunoglobulin,
59 representing 50%, 20%, 10% and 10% of the whey fraction, respectively. Besides these,
60 whey also contains numerous minor proteins such as lactoferrin, lactoperoxidase,
61 proteose peptone, osteopontin and lysozyme (Mollea et al., 2013).

62 Whey proteins are characterized by interesting functional properties due to their
63 physical, chemical and structural features. The most important property is the ability to

64 form gels capable of holding water, lipids and other components that act as emulsifiers
65 providing textural properties. For this property, whey proteins are included in processed
66 meat and dairy and bakery products. Another aspect is its foaming property, which
67 mainly depends on the degree of protein denaturation (Rebouillat and Ortega-
68 Requena, 2015).

69 These abilities are also influenced by the grade of protein concentration in the WPC.
70 For example, WPC containing 34–35% protein (WPC35) has good emulsification
71 properties, is highly soluble and has a mild dairy flavor. This product is used in the
72 manufacture of yogurt, processed cheese and infant formulae; in various bakery
73 applications and in stews and sauces. WPC with about 80% protein (WPC80) has lower
74 carbohydrate content, as compared to WPC35, and is characterized by good
75 gelation, emulsification and foaming properties. WPC80 is an excellent ingredient for
76 sports nutrition and weight management products as well as for meat products, thanks
77 to its high gel strength and good water-binding properties (Rebouillat and Ortega-
78 Requena, 2015).

79 Ultrafiltration represents an excellent separation process compared to other
80 techniques: it allows simultaneous cost reduction and improvement of
81 nutritional/functional protein properties (Luján-Facundo et al., 2017). However, from an
82 environmental point of view, ultrafiltration (and also reverse osmosis) presents two
83 important constraints: the use of high energy inputs for the pressure against membranes
84 and the utilization of large amounts of cleaning agents for removing fouling and
85 maintaining the membranes. The use of cleaning agents can cause the degradation of
86 the membrane material and generate effluents possibly damaging to the environment.
87 Moreover, the reverse osmosis could have limitations from an economic point of view
88 due to the need for high pressures and the high cost of membrane.

89 Another problem regarding whey treatment is related to the spatial collocation of the
90 industrial process and as a consequence the distance between the cheese factory
91 where the whey is produced and the concentration plant. The best solution is to
92 produce WPC directly in the cheese factory to avoid the transport of great volumes of

93 diluted whey, but as previously explained, whey concentration is a complex operation
94 that can only be performed in specialized companies able to cushion the high
95 production costs. A possible alternative is to pre-concentrate the whey directly in the
96 cheese factory, then transport the pre-concentrated whey to an ultrafiltration plant.
97 Considering that in Italy there are only a few ultrafiltration plants, this last solution is
98 adopted by many dairy factories in Italy.

99 Starting from this consideration, it is important to evaluate the environmental benefits
100 arising from the valorization of liquid whey. This is particularly important in Italy where the
101 production of liquid whey from cheese-making was 9,467,004 tons in 2014 (Clal, 2017).

102 A significant and widely appreciated approach to evaluate the environmental impact
103 of a process or product is the Life Cycle Assessment (LCA), which considers the impact
104 throughout the entire life cycle. LCA is largely used in the dairy sector, in particular for
105 the primary phase (Roy et al., 2008; Biswas and Naude, 2016), while few studies have
106 considered cheese production. In studies such as van Middelaar et al. (2011) for a semi
107 hard cheese in the Netherlands, Kristensen et al. (2014) in Denmark and Gonzalez-
108 Garcia et al. (2013a, 2013b) in Spain, the liquid whey obtained from the cheese-making
109 process was not considered ("surplus approach" in which all the environmental load is
110 associated with the main product—the cheese), or it was considered a by-product
111 whose impact was assessed by allocation. In other studies (Kristensen et al., 2014;
112 Palmieri et al., 2017), liquid whey was regarded as feed and included in an alternative
113 scenario at the dairy farm level. Only the study of Kim et al. (2013) took into account
114 the environmental impact of drying whey obtained from mozzarella and cheddar
115 production. Omont et al. (2012), using the LCA approach, underlined the differences in
116 terms of the environmental impacts of two industrial processes to separate purified
117 whey protein from whey (one method based on chromatography separation and one
118 based on microfiltration).

119 In the literature, many studies describe different and innovative methods to
120 concentrate liquid whey (Makardij et al., 1999; Rinaldoni et al., 2009; Walmsley et al.,
121 2013; Méthot-Hains et al., 2016), but there is a lack of information about the generated

122 environmental impact. The aim of this study is to evaluate, using a life cycle approach,
123 the environmental impact of the production of WPC with an ultrafiltration process. In
124 order to understand the mitigation effect of the pre-concentration process of whey in a
125 pretreatment plant, an alternative scenario was also considered. Finally, two sensitivity
126 analyses were performed: the first changing the transport distance of whey, the second
127 using a different allocation method.

128

129 **2 Materials and methods**

130 **2.1 System description and alternative scenarios**

131 The production systems of WPC can be divided into two subsystems.

- 132 - Subsystem 1 (SS1): This subsystem involves the transport of whey (characterized
133 by a dry matter [DM] content of 6%) to the factory and its pretreatment. More in
134 detail, the whey is treated (bactofugation, skimming and pasteurization) and
135 pre-concentrated (by means of reverse osmosis) until it reaches a DM content
136 of 20%.
- 137 - Subsystem 2 (SS2): The pre-concentrated whey is further treated (bactofugation,
138 skimming and pasteurization) and ultrafiltrated to produce WPC with a DM
139 content of 30%. Although all with the same dry matter content, three different
140 WPCs are produced: WPC35 (35% protein content on DM basis), WPC60 (60%
141 protein content on DM basis) and WPC 80 (80% protein content on DM basis).

142

143 Two scenarios were considered (**Figure 1**).

- 144 - Baseline scenario (BS): Whey with a dry matter content of 6% is transported from
145 the cheese factories to the WPC production factory. In this scenario, all
146 operations needed to produce the WPCs are carried out at the WPC factory.
- 147 - Alternative scenario (AS): The pre-concentration of whey is carried out close to
148 the cheese factory in a pre-treatment plant; therefore, only whey with a dry
149 matter content of 20% is transported to the WPC factory.

150

151 **Figure 1 – Around here**

152

153 **2.2 Functional unit and system boundary**

154 The functional unit (FU) provides a reference unit for which the inventory data are
155 normalized (ISO 14040, 2006). In this study, 1 ton of protein in the different WPCs was
156 selected as the FU.

157 In this study, a “cradle-to-industry-gate” perspective was applied. The core system is the
158 process of concentrating whey into WPC; the upstream system involves the whey
159 production while the downstream system includes the delivery of the produced WPC to
160 the factory in which it is completely dried. The distribution as well as the final drying of
161 the WPC were excluded from the system boundaries as they are equal in the two
162 scenarios (BS and AS).

163 The system boundary considers the life cycle of the following processes: raw material
164 extraction (e.g., fossil fuels and minerals), consumption of whey (6% of dry matter), heat,
165 electricity, diesel fuel, water and cleaning agents, transport of whey to the WPC factory
166 as well as the emissions into water and air. The impact of capital goods (e.g.
167 infrastructures of the cheese-factory and to the whey concentration plant) was not
168 considered according to their minor contribution proved by previous LCA studies
169 related to food products (Fusi et al., 2014; Siracusa et al., 2014; Notarnicola et al., 2015;
170 Bacenetti et al., 2015; Garofalo et al., 2017; De Marco and Iannone, 2017).

171

172 **2.3 Inventory analysis**

173 For the BS, all the activities performed in SS1 and SS2 were identified by means of
174 interviews and surveys carried out at the WPC factory as well as in the cheese-making
175 industries.

176 More in detail, all the information regarding the annual volume of processed whey,
177 produced WPC and coproducts as well as all the consumption of electricity, natural

178 gas and cleaning agents was collected by means of questionnaire and a survey at the
179 factory. [Table 1](#) summarizes the main inventory data for SS1 and SS2 while in [Table 2](#) the
180 specific energy consumption for the different WPC is reported. Over the considered
181 year, the WPC factory produced 10,532, 6,629 and 3,923 t of WPC35, WPC60 and
182 WPC80, respectively, corresponding to a whey protein content of 1,080, 1,193 and 942
183 t, respectively.

184

185 [Table 1](#) around here

186 [Table 2](#) around here

187

188 Concerning the SS2 and, in particular, ultrafiltration, the rejection coefficient, the whey
189 protein recovery efficiency as well as the main inputs and outputs for the different
190 WPCs are reported in [Table 3](#).

191 The rejection coefficient was calculated as

192

193
$$RC = 1 - \left(\frac{C_P}{C_R} \right)$$

194 where:

195 RC = rejection coefficient, which varies from 0 (the membrane is completely
196 permeable) to 1 (the membrane is completely impermeable) and indicates the share
197 of protein retained by the membrane;

198 C_P = concentration of the protein in permeate;

199 C_R = concentration of the protein in WPC.

200

201 Whey protein recovery efficiency was calculated as

202

203
$$WPRR = \left(\frac{Q_P \times C_P}{Q_F \times C_F} \right)$$

204 where:

205 WPRR = whey protein recovery efficiency indicates the share of protein retained by the
206 membrane;

207 Q_P = protein in the WPC flow in output from the ultrafiltration (kg/h);

208 Q_F = protein in whey at 20% dry matter flow in input to ultrafiltration (kg/h);

209 C_F = concentration of the protein in whey at 20% of dry matter (kg/h).

210

211 **Table 3** around here

212 The whey (6% DM content and 12.5 % protein on DM) was collected in a cheese factory
213 producing Grana Padano PDO cheese, a long-ripened cheese from skim milk. This
214 cheese represents the most important PDO cheese in northern Italy (183,000 t in 2015),
215 and from its production process comes the main proportion of the processed whey at
216 the WPC factory. The products of the cheese factory were cheese, whey, cream,
217 butter and buttermilk. The whey was considered a coproduct of cheese-making; the
218 impact related to its production was assessed based on the data reported by Bava et
219 al. (2016); according to the PCR for dairy products (EPD, 2016) dry matter content
220 allocation was considered.

221 Considering the location of the whey processing plant and the area of Grana Padano
222 PDO production, for the BS, an average transport distance of 150 km was considered
223 for the whey at 6% DM.

224 Inventory data characterizing the SS1, in the AS, were collected by means of surveys
225 and interviews in a plant that processes yearly about 40,000–60,000 t of whey coming
226 from Grana Padano PDO cheese plants. The transport distance between the cheese
227 factory and the pre-concentration plant and between this last and the WPC factory
228 were assumed to be equal to 20 and 130 km, respectively. Regarding the energy
229 consumption for pretreatment, no reliable information was collected during the surveys
230 due to the impossibility of separating the electricity and heat consumption among the
231 different processes. According to Ramirez et al. (2006), Giaccone and Mancò (2012),
232 Augustin et al. (2014) and Méthot-Hains et al. (2016), being bactofugation, skimming
233 and pasteurization were performed using smaller devices than in BS, an increase of

234 energy consumption ranging from 5 to 20% is expectable. Due to the lack of primary
235 data, in this scenario, a 20% increase in energy consumption for the treatment of 6% DM
236 whey was considered.

237 Concerning the transport of whey, empty return (from the WPC factory to the cheese-
238 making factory in BS and to the pre-processing plant in AS) was taken into account.

239 Background data for the production of electricity, natural gas and cleaning agents as
240 well as for the transport and wastewater treatment were retrieved from the Ecoinvent
241 database v.3 (Weidema et al., 2013).

242

243 **2.4 Allocation**

244 During whey processing at the WPC factory, besides the three WPCs, a permeated
245 stream is produced. The multifunctionality issue was solved by allocation. According to
246 the ISO 14040 (ISO, 2006a), allocation is the "partitioning of the input and output flows
247 of a product system between its main product and co-products" and allows one to
248 calculate how much of the process impacts should be assigned to each product.

249 In this study, physical allocation based on the DM content of the different products and
250 coproducts was applied. More in detail, allocation was performed taking into account
251 the DM content of

- 252 - cheese, whey and other cheese coproducts such as buttermilk and butter at
253 the cheese factory;
- 254 - the different WPCs and the permeate at the WPC factory.

255 Therefore, at the cheese factory, 46.3% of the impact is attributed to the cheese, 37.9%
256 to the whey, 13.0% to the cream, 1.7% to the butter and 1.0% to the buttercream, while
257 at the WPC factory, the allocation factor is 68.5% for WPC35, 69.4% for WPC60 and
258 67.3% for WPC80.

259

260 **2.5 Impact assessment**

261 Among the steps defined within the life cycle impact assessment phase of the
262 standardized LCA methodology, only classification and characterization stages were
263 undertaken (ISO 14040, 2006). The characterization factors reported by the ILCD
264 method were used (Wolf et al., 2012). The following nine impact potentials were
265 evaluated according to the selected method: climate change (CC); ozone depletion
266 (OD); particulate matter (PM); photochemical oxidant formation (POF); acidification
267 (TA); freshwater eutrophication (FE); terrestrial eutrophication (TE); marine
268 eutrophication (ME) and mineral, fossil and renewable resource depletion (MFRD).

269

270 **2.5.1 Sensitivity analysis**

271 A sensitivity analysis was carried out in order to test the robustness of the results. To this
272 purpose, a set of parameters was changed, and the influence of the change on the
273 environmental results was evaluated. The aspects that were taken into account to run
274 the sensitivity analysis were as follows.

275 i) Transport distance of the whey: More in detail, in both scenarios a halving
276 and a doubling of the distance to the WPC factory was considered. In AS,
277 the whey transport distance between cheese plant and preprocessing plant
278 was not varied.

279 ii) Allocation method: In this regard an economic allocation was considered
280 rather than a physical one based on DM content. The economic allocation
281 is widely included in LCA studies about cheese production (Berlin, 2002;
282 González-García et al., 2013a, 2013b). Therefore, the environmental burden
283 among cheese, cream, butter, buttermilk and whey at the cheese factory
284 and between WPC and permeate at the WPC factory was divided
285 considering the products' economic values. More in detail, at the cheese

286 factory, the allocation factor¹ is equal to 76.2%, 4.8%, 17.3%, 1.3% and 0.4%
287 for the produced cheese, whey, cream, butter and buttermilk, respectively.
288 Concerning WPC and permeate, considering the selling prices of the
289 different WPCs (1,445, 2,670 and 3,835 €/t for WPC35, WPC60 and WPC80,
290 respectively) and permeate (130 €/t), the allocation factor is equal to
291 78.25% for WPC35, 80.83% for WPC60 and 81.80% for WPC80.

292

293 **3 Results and discussion**

294 **3.1 Baseline scenario**

295 The hotspots analysis for the three WPCs highlights that the impact due to whey
296 consumption is by far the main factor for environmental impact, ranging from 61% to
297 97% of the total score. The impact categories in which whey consumption has a higher
298 incidence are TA and ME (>95%) while MFRD is at about 60% (**Table 4**). For the latter, the
299 impact of whey is reduced because it is higher the impact related to the energy
300 consumption at the WPC factory during pretreatment and ultrafiltration.

301

302 **Table 4**– around here

303

304

305 **Figures 2 and 3** show the hotspots for WPC production, excluding the impact related to
306 the whey.

307

308 **Figures 2, 3, 4** – Around here

309

310 Excluding whey production, the transport of the whey from cheese factory to WPC
311 factory is the main factor for most of the evaluated impact categories. More in detail,

¹ The allocation factor indicates the proportion of the environmental impact that is allocated to the different products of the evaluated production system.

312 its role ranges from 28% to 30% in ME (mainly due to the emissions of ammonia in the air
313 and nitrates in the water) to 69–71% in POF (mainly due to the emissions of nitrogen
314 oxides, NMVOC and sulfur dioxide). Compared to heat, electricity consumption is
315 responsible for a higher impact: >20% for CC, OD, PM, TA and FE and about 15% for
316 POF, TE and ME. Among the different processes in which electricity is consumed, reverse
317 osmosis has the most impact. On the contrary, the impact of heat consumption is
318 negligible for all the evaluated impact categories except CC (10–11%). Cleaning
319 agents, above all the ones consumed during SS2, are responsible for about half of OD
320 (mainly due to sodium hydroxide production and the consumption of fossil fuels for their
321 production) and 40% of FE (mainly due to electricity consumption during the production
322 process).

323 With regard to the environmental hotspots, only small differences can be highlighted
324 among the three WPCs; this should not be surprising. In fact, although different amounts
325 of whey are needed for the production of the three WPCs (from 5.07 t of whey/t of
326 WPC35 to 12.35 t of whey/t of WPC80), the specific energy consumption is also higher
327 for the WPCs with higher proportions of protein content on a DM basis. [Table 5](#) reports
328 the comparison of the different WPCs considering also the impact of whey. As
329 expected, the impact goes up (from 2 to 7%) with the increase in protein
330 concentration.

331

332 [Table 5](#)– around here

333

334 **3.2 Alternative scenario**

335 For the AS, which involves the pre-concentration of whey at the cheese-making plant,
336 [Table 6](#) reports the environmental hotspots of the three different WPCs. For all the WPCs,
337 the reduction of the amount of whey transported, achieved thanks to pre-
338 concentrating, involves an impact reduction for all the evaluated impact categories.
339 This reduction ranges from 0.9% to 14.3% and is higher for the impact categories such as

340 MFRD (about 14%) and POF (about 8%) that are more affected by transport and, in
341 particular, by diesel consumption and exhaust gases emission. Even if the treatment
342 carried out at the pre-concentration plant in smaller devices involves higher energy
343 consumption for skimming, bactofugation and pasteurization, the reduction of the
344 transport completely offsets the higher energy consumption and results in an impact
345 reduction ranging from 8% to 20%.

346

347 [Table 6– around here](#)

3.3 Sensitivity analysis results

The results of the sensitivity analysis carried out considering the variation (halving and doubling) of the transport distance to the WPC factory are shown in [Table 7](#) while the impact variation related to the use of a different allocation method is reported in [Table 8](#).

[Table 7 – around here](#)

The variation of the whey transport distance has a different impact on the environmental results in the two scenarios. In BS, the variation of the distance involves higher consequences, with respect to AS. The impact variation related to the halving of the distance ranges from -0.8% for TA and -11.8% for MFRD in BS and from -0.2% for TA and -3.6% for MFRD in AS. When the distance is doubled, the impact increases from +1.5% (TE) to +23.7% (MFRD) in BS and from +0.4% (TE) to +7.2% (MFRD) in AS. For both scenarios, for 7 of the 9 evaluated impact categories (CC, OD, PM, TA, TE, FE, ME), impact variations are small, while not negligible for POF and MFRD (the most affected by the consumption of fuel and the engine exhaust gas emissions that occur during transport).

[Table 8 – around here](#)

As expected, the use of economic allocation instead of DM deeply affects the environmental results for the different WPCs; more in detail, it involves an impact variation ranging from -59% to -88%. This variation is related to the different allocation factors between the WPCs and the permeate at the WPC factory but, above all, to the higher impact attributed to the cheese during cheese-making instead of the whey. Unlike the allocation based on dry matter content (that allocates about 40% of the impact related to cheese production to the whey), the economic allocation attributes only 4.8% of cheese-making impact to the whey. Consequently, whey consumption is the main hotspot for WPC production when economic allocation is performed; also, the WPC impact decreases.

In conclusion, the outcomes of the sensitivity analysis show how the environmental results are only slightly affected by the transport distance of whey. On the contrary, the choice of the allocation method plays a relevant role in the environmental profile of the different WPCs; in fact, if economic allocation is used, the environmental impact is reduced up to 88%.

4 Conclusions

Cheese-making involves the production of a considerable amount of whey. Due to its low DM content, whey management can be challenging above all for big cheese-making plants where the produced volume is remarkable. Considering that the use of whey as feed or as a feedstock for biogas production is not profitable, the whey concentration to produce a product with a higher value is an attractive solution. In this study, the environmental impacts related to whey concentration were assessed using the LCA approach and considering real data collected in the biggest Italian cheese-making plant. The achieved results show how whey consumption is the main factor responsible for the WPC impact, followed by whey transport and energy consumption. The pre-concentration of whey in pretreatment plants closer to the cheese factory reduces the amount of whey transported for long distances and, consequently, reduces the environmental burdens of the whole process. This occurs even if the energy consumption for pre-concentration increases due to the use of smaller and less efficient devices.

Up to now, no studies quantified the environmental impacts related to WPC production as well as the impact reduction related to a different logistical organization of the supply chain of the WPC factories. The outcomes of this study are the starting point for further studies on the WPCs used as food components (e.g., production of baby food, substitution of fat during the production of dietetic cheese).

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TABLES

Table 1 – Main inventory data for baseline scenario (BS)

Input	Subsystem	Amount
Whey (6%)	1	409,610 t
Electricity	1	2,553 MWh for whey treatment and reverse osmosis
Natural gas	1	502,000 m ³ for whey treatment and reverse osmosis
Electricity	2	981,517 MWh for whey treatment 1,370 MWh for ultrafiltration
Natural gas	2	370,000 m ³ for whey treatment 52,000 m ³ for ultrafiltration
Whey (20%)	2	226,882 t (from subsystem 1)
Cleaning agent	2	
Electricity	1 & 2	1,320 MWh for refrigeration 1,231 MWh for general consumption 298,000 kWh water well
WPC35	2	10,532 t of dry matter
WPC60	2	6,629 t of dry matter
WPC80	2	3,923 t of dry matter
Permeated	2	23,860 t of dry matter

Table 2 – Specific energy consumption for the different WPCs in BS

Energy source	Unit	WPC35	WPC60	WPC80
Electricity SS1	MWh/t of protein	0.70	0.87	0.82
Natural Gas SS1	m ³ / t of protein	152.36	171.36	161.95
Electricity pre-treatment SS2	MWh/ t of protein	0.298	0.303	0.317
Natural Gas pre-treatment SS2	m ³ / t of protein	112.30	114.27	119.37
Electricity ultrafiltration SS2	MWh/ t of protein	0.416	0.423	0.442
Natural gas ultrafiltration SS2	m ³ / t of protein	15.78	16.06	16.78

Table 3 – Input and output of the ultrafiltration carried out in SS2

WPC	Whey (20%) consumption	Water consumption	Permeated t/t _{WPC}	Rejection Coefficient	Whey Protein Recovery Efficiency

	t/t _{WPC}	t/t _{WPC}	t/t _{WPC}	%	%
WPC35	5.07	0	4.08	99.49	97.9
WPC60	8.86	1.25	9.12	99.65	96.5
WPC80	12.35	3.12	14.46	99.60	94.6

Table 4 – Relative contribution of whey and the other production factors and processes.

Impact Category	Whey consumption			Energy, Cleaning agents & whey transport		
	WPC35	WPC60	WPC80	WPC35	WPC60	WPC80
CC	88.7%	88.7%	88.7%	11.3%	11.3%	11.3%
OD	86.1%	86.0%	86.3%	13.9%	14.0%	13.7%
PM	91.7%	91.6%	91.7%	8.3%	8.4%	8.3%
POF	80.6%	80.5%	80.6%	19.4%	19.5%	19.4%
TA	96.5%	96.5%	96.6%	3.5%	3.5%	3.4%
TE	97.7%	97.7%	97.7%	2.3%	2.3%	2.3%
FE	80.0%	79.8%	80.1%	20.0%	20.2%	19.9%
ME	97.3%	97.3%	97.3%	2.7%	2.7%	2.7%
FEx	84.0%	84.0%	84.2%	16.0%	16.0%	15.8%
MFRD	61.2%	61.2%	61.5%	38.8%	38.8%	38.5%

Table 5 – Environmental impact of the different WPCs in BS (FU = 1 t of protein in the WPC)

Impact category	Unit	WPC35	WPC60	WPC80
CC	kg CO ₂ eq	38,053	39,167	40,652
OD	g CFC-11 eq	3.579	3.684	3.815
PM	kg PM _{2.5} eq	20.39	20.98	21.77
POF	kg NMVOC eq	91.99	94.67	98.23
TA	molc H ⁺ eq	649.61	668.15	693.86
TE	molc N eq	2,784.8	2,863.8	2,974.7
FE	kg P eq	3.331	3.432	3.552
ME	kg N eq	214.69	220.78	229.33
FEx	CTUe	114,420	117,736	122,037
MFRD	kg Sb eq	0.349	0.359	0.371

Table 6 – Environmental impact for the different WPCs in AS (FU = 1 t of protein in the WPC)

Impact category	AS - WPC35		AS - WPC60		AS - WPC80	
	Value	Δ % respect to BS	Value	Δ % respect to BS	Value	Δ % respect to BS
CC	36,966 kg CO ₂ eq	-2.85%	38,053 kg CO ₂ eq	-2.84%	3,9494 kg CO ₂ eq	-2.85%
OD	3.502 g CFC-11 eq	-2.15%	3.605 g CFC-11 eq	-2.14%	3.733 g CFC-11 eq	-2.15%
PM	19.982 kg PM2.5 eq	-2.00%	20.559 kg PM2.5 eq	-1.99%	21.331 kg PM2.5 eq	-2.00%
POF	84.630 kg NMVOC eq	-8.00%	87.108 kg NMVOC eq	-7.99%	90.378 kg NMVOC eq	-8.00%
TA	643.6 molc H ⁺ eq	-0.92%	662.0 molc H ⁺ eq	-0.92%	687.5 molc H ⁺ eq	-0.92%
TE	2,759.6 molc N eq	-0.90%	2,837.9 molc N eq	-0.90%	2,947.8 molc N eq	-0.90%
FE	3.250 kg P eq	-2.45%	3.348 kg P eq	-2.43%	3.465 kg P eq	-2.44%
ME	212.4 kg N eq	-1.07%	218.4 kg N eq	-1.07%	226.9 kg N eq	-1.07%
MFRD	0.299 kg Sb eq	-14.26%	0.308 kg Sb eq	-14.25%	0.318 kg Sb eq	-14.33%

Table 7 – Impact variation (%) considering the doubling or the halving of the transport distance to the WPC factory in BS e AS

Impact category	BS						AS					
	WPC35		WPC60		WPC80		WPC35		WPC60		WPC80	
	Halving	Doubling	Halving	Doubling	Halving	Doubling	Halving	Doubling	Halving	Doubling	Halving	Doubling
CC	-2.62%	5.24%	-2.62%	5.24%	-2.62%	5.24%	-0.70%	1.40%	-0.70%	1.40%	-0.70%	1.40%
OD	-1.93%	3.87%	-1.93%	3.87%	-1.94%	3.88%	-0.51%	1.03%	-0.51%	1.03%	-0.52%	1.03%
PM	-1.76%	3.53%	-1.76%	3.52%	-1.76%	3.53%	-0.47%	0.94%	-0.47%	0.93%	-0.47%	0.94%
POF	-6.79%	13.59%	-6.79%	13.57%	-6.80%	13.59%	-1.92%	3.84%	-1.92%	3.84%	-1.92%	3.84%
TA	-0.82%	1.63%	-0.82%	1.63%	-0.82%	1.63%	-0.21%	0.43%	-0.21%	0.43%	-0.21%	0.43%
TE	-0.77%	1.54%	-0.77%	1.54%	-0.77%	1.54%	-0.20%	0.40%	-0.20%	0.40%	-0.20%	0.40%
FE	-2.43%	4.87%	-2.43%	4.86%	-2.44%	4.88%	-0.65%	1.30%	-0.65%	1.29%	-0.65%	1.30%
ME	-0.91%	1.82%	-0.91%	1.82%	-0.91%	1.82%	-0.24%	0.48%	-0.24%	0.48%	-0.24%	0.48%
MFRD	-11.85%	23.70%	-11.84%	23.68%	-11.91%	23.82%	-3.59%	7.19%	-3.59%	7.18%	-3.62%	7.23%

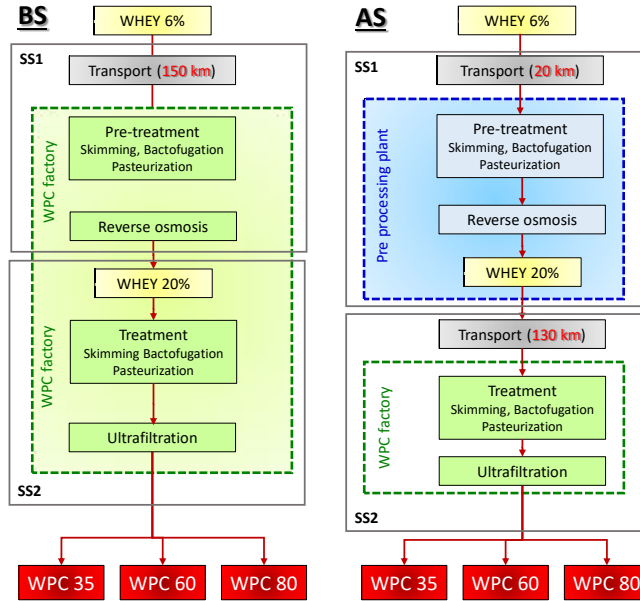
1 **Table 8** – Impact variation for the different WPC in the two scenarios considering
 2 Economic Allocation instead of the Dry matter allocation in AS e BS
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Impact category	Economic allocation					
	BS			AS		
	WPC35	WPC60	WPC80	WPC35	WPC60	WPC80
CC	-80.2%	-80.5%	-81.1%	-80.2%	-82.7%	-83.3%
OD	-78.2%	-78.6%	-79.3%	-78.2%	-80.1%	-80.9%
PM	-82.5%	-82.8%	-83.3%	-82.5%	-84.3%	-84.8%
POF	-74.0%	-74.4%	-75.2%	-74.0%	-79.9%	-80.5%
TA	-86.2%	-86.4%	-86.8%	-86.2%	-87.2%	-87.5%
TE	-87.1%	-87.3%	-87.7%	-87.1%	-88.0%	-88.3%
FE	-73.7%	-74.1%	-75.0%	-73.7%	-75.9%	-76.8%
ME	-86.8%	-87.1%	-87.5%	-86.8%	-87.9%	-88.2%
MFRD	-59.2%	-60.0%	-61.3%	-59.2%	-67.7%	-68.9%

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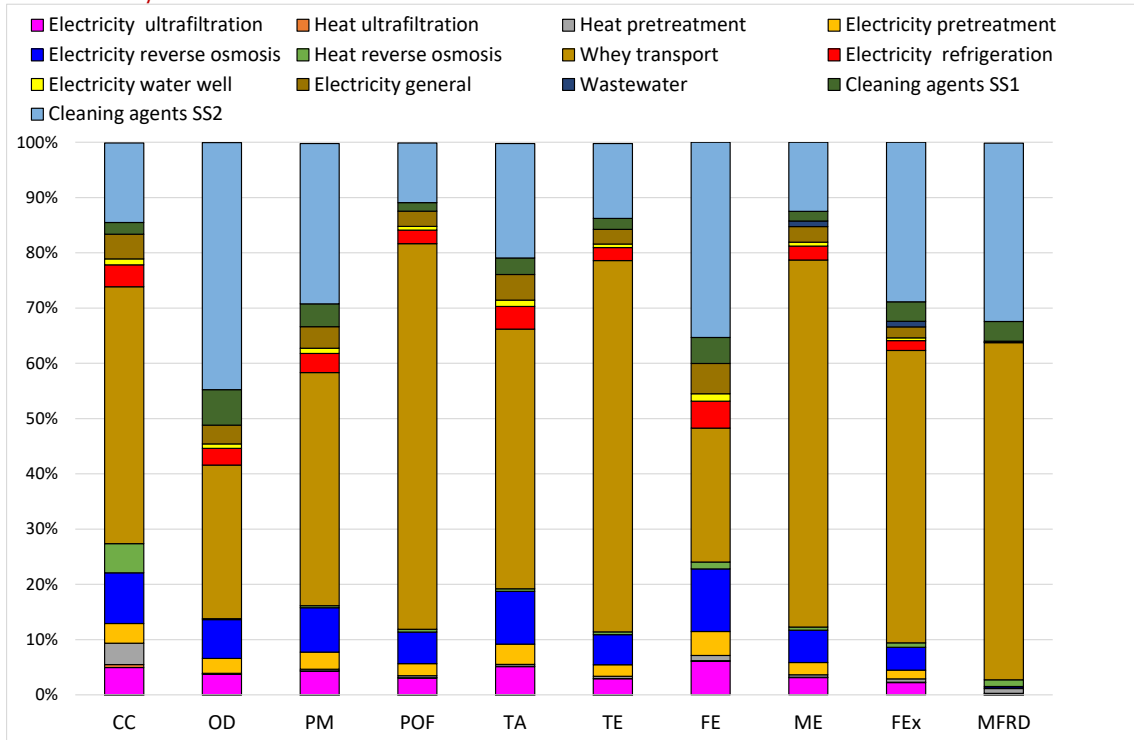
FIGURE CAPTIONS



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Figure 1 –Schematisation of the two considered scenarios (BS = baseline, AS = alternative).

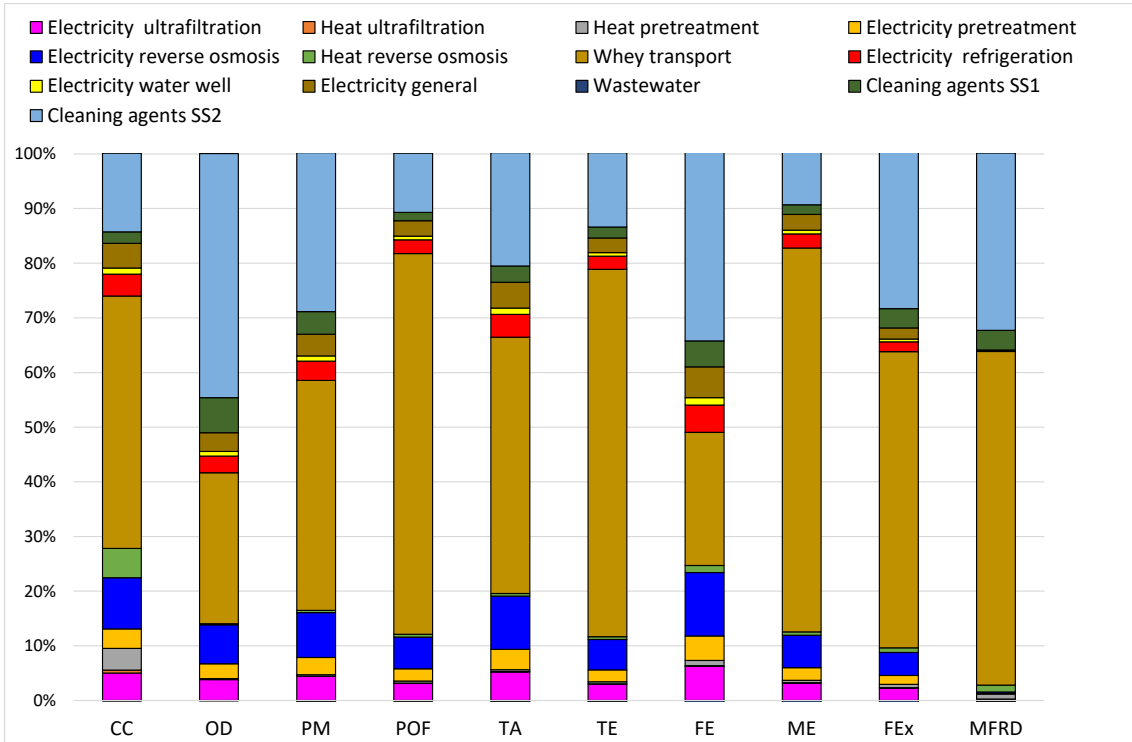
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Figure 2 – Hotspots identification for the WPC35 in BS excluding whey production; climate change (CC), ozone depletion (OD), particulate matter (PM); photochemical oxidant formation (POF); acidification (TA), freshwater eutrophication (FE), terrestrial eutrophication (TE) marine eutrophication (ME), and mineral, fossil and renewable resource Depletion (MFRD).

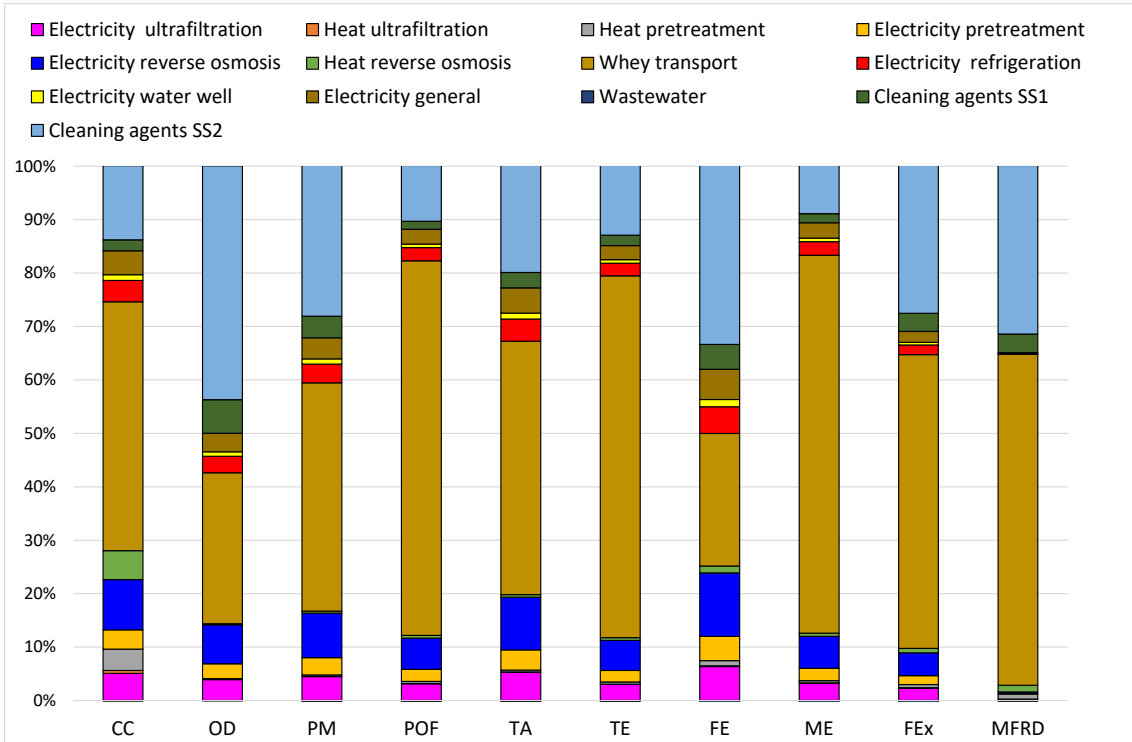
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19 **Figure 3** – Hotspots identification for the WPC60 in BS excluding whey production;
 20 climate change (CC), ozone depletion (OD), particulate matter (PM); photochemical
 21 oxidant formation (POF); acidification (TA), freshwater eutrophication (FE), terrestrial
 22 eutrophication (TE) marine eutrophication (ME), and mineral, fossil and renewable
 23 resource Depletion (MFRD).

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49 **Figure 4** – Hotspots identification for the WPC80 in BS excluding whey production;
 50 climate change (CC), ozone depletion (OD), particulate matter (PM); photochemical
 51 oxidant formation (POF); acidification (TA), freshwater eutrophication (FE), terrestrial
 52 eutrophication (TE) marine eutrophication (ME), and mineral, fossil and renewable
 53 resource Depletion (MFRD).

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