

**Role of amylose content and milling fractions on physico-chemical features of co-extruded snacks from corn**

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**Abbreviations:** ABTS, 2,2'-azino-bis(3-ethylbenzothiazoline-6-sulfonic acid); AC, antioxidant capacity; AC-ABTS, antioxidant capacity by means of the ABTS assay; AC-FRAP, antioxidant capacity by means of the FRAP assay; C, conventional hybrid; C-HA, conventional:high amylose hybrid blend (50:50); C-W, conventional:waxy hybrid blend (50:50); CWBPAs, cell wall-bound phenolic acids; FRAP, Ferric reducing antioxidant power; HA, high-amylose hybrid; SPAs, soluble phenolic acids; W, waxy hybrid.

**Abstract:**

This study focused on the suitability of corn milling fractions (break meal, particle size: 250-500  $\mu\text{m}$ ; flour, particle size < 150  $\mu\text{m}$ ) from hybrids different in amylose content (conventional: 18% amylose; high-amylose: 42% amylose; waxy: 2% amylose) and their blends, to produce co-extruded snacks. Antioxidant capacity, phenolic acid content, pasting properties and snack size, hardness, porosity, and density were considered. As regards the bioactive compounds, corn flour reported a marked antioxidant capacity compared to break meal. High amylose hybrid maintained the highest antioxidant capacity and phenolic acid content even after extrusion. Waxy and conventional hybrids led to more expanded and softer snacks, than the high amylose hybrid that, thus, has to be preferred for co-extruded snacks production. Blends led to snacks whose features did not follow a linear trend with the amylose content, suggesting the need for further studies to better understand starch interactions among the various hybrids.

**Keywords:** corn; high amylose; waxy; dry-extrusion; snacks; gluten-free

## 1        **1. Introduction**

2        The snack food market is expanding rapidly and is predicted to continue growth in the future  
3        (Brennan, Derbyshire, Tiwari & Brennan, 2013), particularly within the gluten-free sector. Indeed,  
4        this product category completely meets the demand for minimally processed, ready-to-eat foods.  
5        Among the different technologies used for the production of snacks, the extrusion-cooking  
6        process represents one of the most innovative and interesting production processing (Delgado-  
7        Nieblas, Aguilar-Palazuelos, Gallegos-Infante, Rocha-Guzmán, Zazueta-Morales & Caro-  
8        Corrales, 2012). Extrusion-cooking combines high temperature and high shear stress conditions.  
9        High temperature allows to gelatinize the starch keeping the water in the liquid phase. The dough  
10       is then processed in the cylinder and subsequently extruded through the die at atmospheric  
11       pressure. The sudden breakdown of pressure causes an immediate expansion of the product due  
12       to the rapid evaporation of the water. Using this technology, it is possible to produce food that can  
13       be designed for shape, taste, texture, and sensory characteristics, helping the food industry to  
14       respond to the growing needs of the “modern” consumer.

15       Nowadays, the majority of the studies have focused on the direct-expanded extrudates and how  
16       either formulation (i.e., enrichment in proteins or fibers) or processing conditions (i.e., hydration  
17       level, pressure, temperature, shear) play a role in defining the quality of the final product, as  
18       recently reviewed by Brennan et al. (2013). Conversely, to the best of our knowledge, little is  
19       known about the effect of raw materials and extrusion conditions on the characteristics of co-  
20       extruded snacks. The most common snack produced by co-extrusion is a cereal-based outer tube  
21       with a sweet or savory filling inside. Direct-expanded and co-extruded snacks are different in  
22       texture which is, actually, dependent on the extent of expansion, that is measured by the increase  
23       in diameter after extrusion. High expansion rate is related to increased porosity of the product and  
24       either a large number of gas cells, or a number of large gas cells (Brennan et al., 2013).

25       Few studies highlighted the relation between expansion rate and starch properties (i.e. amylose  
26       content), by adding commercial high-amylose starch in the formulation of puffed snacks (Zhu,

27 Shukri, de Mesa-Stonestreet, Alavi, Dogan & Shi, 2010; Tacer-Caba, Nilufer-Erdil, Boyacioglu &  
28 Ng, 2014). However, none of the available studies make a clear comparison between  
29 conventional, waxy and high amylose corn for the production of co-extruded snacks.  
30 Extruded snacks can be manufactured using a wide variety of starch and/or grains, including corn,  
31 that play a key role in providing all the features desired for highly acceptable snack products, such  
32 as structure, texture, and mouth feel. For most corn-based extruded snacks, corn meal is used  
33 (Riaz, 2006). Corn pearl meal (particle size from 600 to 1000  $\mu\text{m}$ ), break meal (mainly from 250  
34 to 500), and flour (85% of particles under 150  $\mu\text{m}$ ) are the main products obtained from the dry-  
35 milling of corn. They differ in both particle size, in the endosperm area they come from, and thus  
36 in their end-uses. Specifically, meal is obtained from the vitreous part of the endosperm, while the  
37 softer parts are mainly broken down to flour (Blandino, Alfieri, Giordano, Vanara & Redaelli, 2017;  
38 Vanara, Scarpino & Blandino, 2018). As regards food applications, corn meal, that is  
39 characterized by a higher particle size than flour, is mainly used for polenta (pearl meal) or snacks  
40 (break meal), whereas corn flour is used as an ingredient in many gluten-free formulations,  
41 including snacks, bread, and pasta (Marti & Pagani, 2013). In the context of gluten-free products,  
42 using flours instead of the isolated starch as a major ingredient will help deliver gluten-free foods  
43 with enhanced nutritional quality (Pellegrini & Agostoni, 2015). In the case of corn, this is  
44 particularly true for the contribution of phytochemicals, including bioactive compounds such as  
45 phenolic acids and carotenoids mainly responsible for flour antioxidant capacity (Blandino et al.,  
46 2017). Despite that, the potential use of both corn break meal and flour for the production of co-  
47 extruded snacks has not been addressed so far.

48 Taking into consideration these findings, the objective of the present study was to assess the role  
49 corn milling fractions and amylose:amylopectin ratios on the physico-chemical changes during  
50 extrusion-cooking and their impact on the features of co-extruded snacks. In particular, three  
51 hybrids different in amylose content (i.e., conventional, waxy, and high amylose) and two corn  
52 milling fractions (break meal and flour) were considered.

## 53        **2. Materials & Methods**

### 54        **2.1 Materials**

55        All raw materials were kindly provided by Molino Peila S.p.A. (Valperga, Italy). Three corn  
56        varieties different in amylose content were used: i) a conventional hybrid (Pioneer P1547,  
57        amylose = 18%; C), ii) high-amylose hybrid (Planta Amylor, amylose = 42%; HA) and iii) waxy  
58        hybrid (Pioneer P1547E, amylose = 2%; W). All hybrids have been cultivated in the 2018 growing  
59        season in the same growing area in North West Italy. Pioneer P1547 is actually one of the hybrids  
60        more cultivated in Italy within the dry-milling supply chain. For each corn hybrid, two types of  
61        products were obtained: a flour from the softer part of the endosperm (85% of particles under 150  
62         $\mu\text{m}$ ), and a break meal from the vitreous endosperm (77% of particles between 250-500  $\mu\text{m}$ ). HA  
63        and W were used alone and in combination (50:50) with C (C–HA and C – W).

64        Co-extruded snacks were produced at industrial level by Fudex Group S.p.A. (Settimo Torinese,  
65        Italy). Dry-extrusion was performed using a co-rotating twin-screw extruder (model 2FB90; screw  
66        speed: 100 rpm; temperature: 117 °C; pressure: 70 bar). For starch susceptibility to  $\alpha$ -amylase  
67        and pasting properties and phenolic acid content and antioxidant capacity, snacks were milled  
68        into flour (particle size less than 250 microns) using a laboratory mill (IKA Universalmühle M20;  
69        IKA Labortechnik, Staufen, Germany), with a water-cooling system to avoid the overheating.

### 70        **2.2. Methods**

#### 71        **2.2.1 Chemical composition**

72        The moisture content, determined in order to express all the results on a dry weight (dw) basis,  
73        was obtained by oven-drying at 105 °C for 24 h. Total starch content was measured according to  
74        the standard method AACC 76-13.01 (Cereals & Grains, 2011). The total protein content  
75        (conversion factor: 5.70) was obtained according to the Kjeldahl method by means of a Kjeltac  
76        system I (Foss Tecator AB, Höganäs, Sweden) (Sovrani et al., 2012). The total dietary fiber  
77        content was determined by means of the Megazyme total dietary fiber analysis kit. The fat

78 (Soxhlet method) and ash (muffle furnace) contents were determined according to the AOAC  
79 (2005) procedures.

## 80 **2.2.2 Extraction and quantification of the soluble (SPAs) and cell wall-bound phenolic** 81 **acids (CWBPAs)**

82 The extraction of free and conjugated SPAs and CWBPAs was performed according to the  
83 procedure proposed by Li, Shewry & Ward (2008) and Nicoletti, Martini, De Rossi, Taddei,  
84 D'Egidio & Corradini (2013) with some modifications. 3,5-Dichloro-4-hydroxybenzoic was used as  
85 an internal standard to ensure that losses due to the extraction method were accounted for.

### 86 Extraction of soluble phenolic acids

87 An aliquot (125 mg) of each sample was extracted with 1 mL of 80:20 (v/v) ethanol:water solution.  
88 The mixtures were vortexed for 30 s, and then sonicated (35 kHz, Sonorex Super RK 156 BH,  
89 Bandelin Electronic, Berlin, Germany) for 10 min, maintaining the temperature at 4°C to avoid  
90 starch gelatinization. Samples were centrifuged at 10,600 x g for 10 min, and a second extraction  
91 was carried out with 80:20 (v/v) ethanol:water solution. The pellet was discarded, while the  
92 supernatants were collected and then evaporated to dryness under a nitrogen stream. Samples  
93 were hydrolyzed with 2 M NaOH for 2 h under continuous stirring at 4°C. After acidification to pH  
94 2 with HCl, soluble phenolic acids were extracted with 500 µL of ethyl acetate. After centrifugation  
95 at 10,600 x g for 2 min the upper layer was transferred in a clean microcentrifuge tube. The  
96 extraction was repeated twice, and the combined supernatants were evaporated to dryness under  
97 a nitrogen stream and then reconstituted in 100 µL of 80:20 (v/v) methanol:water solution.

### 98 Extraction of cell wall-bound phenolic acids

99 Samples (125 mg) were extracted two times with 80:20 (v/v) ethanol:water in order to remove  
100 soluble phenolic acids. Mixtures were vortexed before being sonicated for 10 min. Samples were  
101 then centrifuged at 10,600 x g for 10 min, and the supernatant was removed and discarded. The

102 remaining pellet was hydrolyzed 4 h under continuous stirring at 4°C, by adding 2 M NaOH. After  
103 acidification to pH 2 with HCl, the bound phenolic acids were extracted with 800 µL of ethyl acetate  
104 and then centrifuged at 10,600 x g for 2 min. The extraction was repeated another time. The  
105 combined supernatants were evaporated to dryness under a nitrogen stream, and then  
106 reconstituted in 200 µL of 80:20 (v/v) methanol:water solution.

#### 107 Quantification of soluble and cell wall-bound phenolic acids by means of RP-HPLC/DAD

108 The phenolic extracts were filtered through a 0.2 µm PVDF filter and then analyzed by means of  
109 a high performance liquid chromatograph Agilent 1200 Series (Agilent Technologies, Santa Clara,  
110 CA, US) coupled to an Agilent 1200 Series diode array detector. Separations were carried out  
111 using a 150 x 4.6 mm, 5 µm, Gemini RP-18 column (Phenomenex, Torrance, CA, US); the column  
112 temperature was set at 35 °C. The mobile phase consisted of 0.1% acetic acid in water (solvent  
113 A) and 0.1% acetic acid in methanol (solvent B). The following operating linear gradient was used:  
114 0-22 min, 9-42% B; 22-27 min, 42-90% B; 27-32 min, 90% B. Finally, the mobile phase was  
115 brought to 9% B in 3 min, and this was followed by 16 min of equilibration. The flow rate of the  
116 mobile phase was 1 mL/min. Phenolic acids were identified using the retention times and the  
117 UV/Vis spectra of their respective standards. Solutions of individual phenolic acid standards were  
118 also prepared and diluted to different concentrations to obtain calibration curves for quantification  
119 purposes. The quantifications were performed at the maximum absorption wavelength of each  
120 phenolic acid.

#### 121 **2.2.3 Determination of antioxidant capacity by means of the FRAP assay**

122 The FRAP (Ferric Reducing Antioxidant Power) assay adapted into the QUENCHER method was  
123 performed as described by Serpen, Gökmen & Fogliano (2012). Briefly, FRAP reagent was  
124 prepared by mixing the aqueous solution of 10 mM TPTZ and 20 mM ferric chloride in 300 mM  
125 sodium acetate buffer (pH 3.6) at a ratio of 1:1:10 (v:v:v). Samples (2 mg) were analyzed by  
126 adding FRAP working solution (2 mL). The reaction was carried out under stirring at 1,000 rpm

127 (PCMT Thermoshaker, Grant Instruments, Cambridge, UK). After exactly 120 min from the first  
128 introduction of FRAP solution onto solid samples, centrifugation was performed for 1 min at  
129 20,800 x g, and the absorbance was measured at 593 nm. The final results were expressed as  
130 mmol Trolox equivalents/kg of sample (dw) through a calibration curve.

#### 131 **2.2.4 Determination of antioxidant capacity by means of the ABTS assay**

132 The ABTS (2,2'-azino-bis(3-ethylbenzothiazoline-6-sulfonic acid) assay adapted into  
133 QUENCHER method was performed as described by Serpen et al. (2012). Briefly ABTS<sup>+</sup> working  
134 solution was obtained by diluting the aqueous stock solution (7 mM ABTS, 2.45 mM potassium  
135 persulfate) with water until the absorbance at 734 nm was 1.5. Samples (1.4 mg) were analyzed  
136 by adding 700 µl of ethanol and 700 µl of the ABTS<sup>+</sup> working solution (final solvent ratio -  
137 water:ethanol 50:50). The reaction was carried out in the dark under stirring at 20°C and 1000  
138 rpm for 30 min. The samples were promptly centrifuged for 1 minute at 20,800 x g, and the  
139 absorbance of the supernatant was measured at 734 nm. A control solution, without the ground  
140 sample, was tested under the same conditions, in order to calculate the ABTS<sup>+</sup> inhibition  
141 percentage of the samples. The final results were expressed as mmol Trolox equivalents/kg of  
142 sample (dw) through a calibration curve.

#### 143 **2.2.5 Starch properties**

144 Starch susceptibility to  $\alpha$ -amylase was carried according to the standard method AACC 76-31.01  
145 (Cereals & Grains, 2011).

146 Pasting properties were evaluated using a Micro Visco-Amylo-Graph (Brabender GmbH.,  
147 Duisburg, Germany) according to the procedure of Marengo et al. (2017). Twelve grams of flour  
148 were dispersed in 100 ml of distilled water, scaling both sample and water weight on a 14% flour  
149 moisture basis. The suspensions were subjected to the following temperature profile: heating from  
150 30 up to 95°C, holding at 95°C for 20 minutes and cooling from 95 to 30°C with a heat/cooling  
151 rate of 3°C/min. The following parameters were considered: beginning of gelatinization



152 (temperature at which an initial increase in viscosity occurs), maximum viscosity (maximum  
153 viscosity reached during the analysis), peak temperature (temperature at the maximum viscosity),  
154 breakdown (difference between the maximum viscosity and the viscosity reached at the end of  
155 the holding period) and setback (difference between the final viscosity at 30°C and the viscosity  
156 reached at the end of the holding period).

157 All the measurements were carried out on raw materials and snacks.

## 158 **2.2.6 Snack characterization**

### 159 Area

160 Cylindrical shape snacks were cut using a blade and images of cross sections were acquired at  
161 300 dots per inch with a digital scanner (Epson Perfection 550 Photo, Seiko Epson Corp., Suwa,  
162 Japan). Image analyses were performed using Image ProPlus software (v6; Media Cybernetics,  
163 Inc., Rockville, US). Images were processed into gray level (8 bits). Section area, cell wall area,  
164 and inner area were considered.

### 165 Porosity and bulk density

166 Total porosity and bulk density were assessed with a Pascal Mercury Porosimeter (P240; Thermo  
167 Fisher Scientific, Waltham, US). Samples were subjected to an increasing pressure of up to 200  
168 MPa that makes it possible to measure pores with a radius from  $3.7 \times 10^{-3}$  to 7.5  $\mu\text{m}$ .

### 169 Texture analysis

170 Mechanical properties of the snacks were determined by a three-point bend method using a TA  
171 – XT plus texture analyzer (Stable Micro Systems Ltd., Godalming, UK) equipped with a 10 kg  
172 (100 N) load cell. Samples were compressed with the HDP/3PB probe at a crosshead speed 1  
173 mm/s to 5 mm of original diameter of the extrudate. The compression generated a curve with the  
174 force over distance. The highest value of force was taken as a measurement for hardness.

## 175 **2.2.7 Statistics**

176 Three individual extractions were carried out for each sample for both SAPs and CWBPAs. The  
177 SPAs and CWBPAs content, AC-FRAP, AC-ABTS, and starch susceptibility were measured in  
178 triplicate, whereas pasting properties, porosity and bulk density in duplicate. Image and texture  
179 analysis were carried out on ten and thirty pieces, respectively. One-way analysis of variance was  
180 performed by SPSS for Windows statistical package Version 24 (SPSS Inc., Chicago, Illinois,  
181 US). Significant differences ( $p < 0.05$ ) among the samples were determined using the REGW-F  
182 test.

## 183 **3. Results & Discussion**

### 184 **3.1 Raw materials chemical composition**

185 Corn fractions resulted in different composition according to the particle size: corn flour resulted  
186 in a higher content of starch (76%), fat (2%), and ash (1%) compared to break meal (starch 72%,  
187 fat 1.5%, ash 0.6%). On the other hand, the percentage of protein (7.0% vs 4.6%) and fiber (4.4%  
188 vs 2.6%) was higher in break meal than corn flour.

### 189 **3.2 Phenolic acids and antioxidant capacity of raw materials and snacks**

190 SPAs, CWBPAs, and AC detected in the corn fractions and snacks are reported in Table 1. As  
191 regards the raw materials, both the milling particle size and the type of hybrid affected the  
192 concentration of phenolic acids. The corn flour showed on average a higher concentration of both  
193 SPAs and CWBPAs in comparison with the break meal (+34% and +4%, respectively). Comparing  
194 the hybrids, the highest concentration of CWBPAs was observed in HA (686 and 629 mg/kg dw,  
195 for break meal and flour, respectively), while no significant difference was observed between the  
196 C and W hybrids. Less differences were observed comparing hybrids for their SPA content.  
197 The antioxidant capacity, measured by means of FRAP and ABTS assays, was higher in the HA  
198 hybrid than the other hybrids (+32% and +20%, respectively). Results are in accordance with the  
199 ones of Li, Wei, White & Beta (2007), who stated that among corn genotypes, the high-amylose

200 one had the best antioxidant capacity and the highest concentration of ferulic acid. Similarly, the  
201 HA hybrid analyzed in the present study showed the highest concentration of CWB ferulic acid  
202 (+49%) if compared with the C and W hybrids (data not shown).

203 Several changes occur during extrusion as far as both phenolic acids and AC are concerned  
204 (Figure 1). Specifically, AC increased significantly during processing, resulting - as far as the HA  
205 hybrid is concerned - about 2 times higher in snacks than the related raw material. The increase  
206 in the AC seems not to be related to the changes in SPAs and CWBPAs occurred during  
207 extrusion. Indeed, even if phenolic acids are the main antioxidant compounds in cereals, and  
208 several studies showed a correlation between their concentration and the AC (Beta, Nam, Dexter  
209 & Sapirstein, 2005; Li et al., 2007), both SPAs and CWBPAs decreased during extrusion. The  
210 only exception is the cell wall-bound sinapic acid, whose concentration increased after extrusion.  
211 Interestingly, as far as the HA hybrid is concerned, the concentration of soluble sinapic acid during  
212 processing decreased of 32 mg/kg, whereas in the bound form the concentration increased of 25  
213 mg/kg.

214 As observed in previous studies (Yilmaz & Toledo, 2005; Yu, Nanguet & Beta, 2013), the increase  
215 in the AC during extrusion could be due to the products of the Maillard reaction formed during the  
216 processing at high temperatures. As far as phenolic acids are concerned, several studies showed  
217 that the extrusion process greatly affect the composition of both free and bound phenolic acids in  
218 cereals, and that changes could differ depending on the cereal processed because of great  
219 difference of cereal matrix (Zeng, Liu, Luo, Chen & Gong, 2016; Ruiz-Armenta, Zazueta-Morales,  
220 Delgado-Nieblas, Carrillo-López, Aguilar-Palazuelos & Camacho-Hernández, 2019). In the  
221 present study, SPAs suffered the greatest decrease after extrusion. Snacks obtained from the HA  
222 hybrid showed a decrease by 51-59% of SPAs compared to the raw material. Similarly, Altan,  
223 McCarthy & Maskan (2009) observed that extrusion cooking of barley significantly reduced total  
224 phenolics by 46-60%. Extrusion cooking could lead to a decrease of free phenolic acids because  
225 of decomposition caused by high temperatures. Moreover, the extractability of free phenolic acids

226 after extrusion could decrease because of the increased polymerization which could occur during  
227 extrusion. At the same time, CWBPAs could be released from the cell wall during extrusion, and  
228 their extractability could increase because of changes in the organizational structure of extruded  
229 cereals. Nevertheless, even if the concentration of CWBPAs slightly decreased during extrusion,  
230 differences observed in the present study were not significant.

### 231 **3.3 Starch properties**

#### 232 **3.3.1 Starch susceptibility to $\alpha$ -amylase hydrolysis**

233 Starch susceptibility to  $\alpha$ -amylase hydrolysis of corn and the related snacks is shown in Table 2.  
234 In the raw materials, this index is related to the amount of damaged starch, i.e. the starch granules  
235 which are physically broken during the milling or grinding process to make flour. Indeed, damaged  
236 granules are more susceptible to enzymatic hydrolysis having a high contact surface. Taking into  
237 consideration that, as expected, corn break meal samples presented less amount of damaged  
238 starch (Table 2) and higher particle size (data not shown), coming from the vitreous endosperm  
239 of the kernel. On the other hand, the flour samples are obtained from the softer part of the  
240 endosperm (Blandino et al., 2017).

241 As regards the hybrids different in amylose content, the highest damaged starch in snacks from  
242 W flour has been associated with the low hydrogen bonding due to the low amylose content that  
243 may decrease the resistance to crushing and thus increase the starch damage (Bettge, Giroux &  
244 Morris, 2000). On the other hand, the more compact structure in HA might account for the low  
245 values in damaged starch found in both corn flour and break meal from HA.

246 In the case of processed foods, the starch susceptibility index provides information about the  
247 effects of processing on starch structure (Marti, Seetharaman & Pagani, 2010). As expected, the  
248 combination of both thermal and mechanical stresses applied during the dry-extrusion process  
249 resulted in a significant increase in starch susceptibility to  $\alpha$ -amylase hydrolysis, suggesting starch  
250 destructuring. Specifically, snacks from HA exhibited the lowest starch susceptibility when either

251 flour or break meal were used for their production, suggesting that the more compact structure  
252 due to the high amylose content mitigated the effect of processing.

### 253 **3.3.2 Pasting properties**

254 Raw material pasting profiles are reported in Figure 2 and the related indices are summarized in  
255 Table 3. Corn break meal samples showed low viscosity values, compared to corn flours, likely  
256 due to differences in particle size. In addition, in break meal samples, starch reached a plateau  
257 rather than a peak of viscosity, suggesting low hydration and gelatinization capacity. Similar  
258 differences were observed between flour and semolina samples (Mariotti, Zardi, Lucisano &  
259 Pagani, 2005).

260 As regards the amylose content, both W flour and break meal showed a lower pasting  
261 temperature, peak viscosity, and retrogradation tendency (i.e., low final viscosity and setback  
262 values) compared to C, in agreement with literature (Caramanico et al., 2018; Liu, Yuan, Wang,  
263 Reimer, Isaak & Ai, 2019). On the other hand, both HA flour and break meal did not show viscosity  
264 even at 95 °C, which could be ascribed to their high gelatinization temperatures (Liu et al., 2019).  
265 Therefore, HA did not show re-association to provide a high final viscosity. Previous studies  
266 showed that heating HA starch at temperatures above 120 °C completely gelatinized starch (Liu  
267 et al., 2019). As expected, blending either W or HA with C resulted in an intermediate behaviour.  
268 Regardless of the type of milling fractions and corn hybrid, snacks did not show a pasting profile  
269 (data not shown), as a result of starch degradation occurring during the extrusion process and  
270 confirming the starch susceptibility data in Table 2. Dry-extrusion leads to a high gelatinization  
271 degree of the starch causing the loss of its gelatinisation and retrogradation properties. This  
272 behavior was common in extruded products obtained from various raw materials (Gomez &  
273 Aguilera, 1983; Ozcan & Jackson, 2005; Tacer-Caba et al., 2014).

### 274 **3.4 Snack features**

275 The features of snacks in terms of total and section area, bulk density, porosity, and hardness are  
276 summarized in Table 4. The overall quality of snacks greatly depends on the type of product, i.e.  
277 direct-expanded vs co-extruded snack. The former is characterized by low bulk density and high  
278 expansion rate; the latter by a compact structure, in which voids are undesired. In this study we  
279 focused on co-extruded snacks that typically have an extrusion-cooked outer shell that will be  
280 filled with a savory or sweet filling. Since the filling needs to be contained inside the snack, a  
281 compact structure is desirable. In this kind of products, structure compactness might be assessed  
282 by low volume and consequently high bulk density and porosity. Last but not least, various  
283 sensory attributes, including crispy texture, contribute to the definition of product quality.  
284 Specifically, usually, the higher the expansion rate, the lower the bulk density and the hardness  
285 (Tacer-Caba et al., 2014). Moreover, hardness is related to some other parameters, such as  
286 porosity, cell size and cell wall thickness and the final product density (Robin, Schuchmann &  
287 Palzer, 2012).

288 The section area could be considered an index of the degree of expansion of the product. Indeed,  
289 the higher the area, the higher is the expansion rate, considering that the die of the extruder did  
290 not change during the extrusion trials.

291 The section area of snacks made from corn flours is generally higher than the area of corn meal  
292 snacks (Table 4), suggesting high expansion degree and confirming previous findings about the  
293 relation between increased particle size and decreased expansion of extrudates (Garber, Hsieh  
294 & Huff, 1997; Shevkani, Kaur, Singh, Singh & Singh, 2014). The lower expansion of snacks from  
295 powders of larger particles could be due to incomplete starch gelatinization, as shown by the  
296 pasting profiles in Figure 2. The differences in section area among the snacks made from either  
297 corn flour or break meal were similar when HA was used, suggesting that the type of hybrid  
298 prevails on particle size.

299 Regardless of the particle size, snacks from C and HA showed the highest and lowest section  
300 and cell wall area (which is the difference between section and inner area), respectively. Previous  
301 studies emphasized the role of HA on the expansion rate of corn starch snacks (Mercier & Feillet,  
302 1975; Zhu et al., 2010). Specifically, HA starch required higher extrusion temperature to reach an  
303 expansion degree comparable to starches with less amylose content (Mercier & Feillet, 1975).

304 The amount of amylose in the products and both section and cell wall area did not follow a linear  
305 trend (data not shown), suggesting that it is not only the amylose content, but likely also the starch  
306 structure to determine the characteristics of the final product.

307 Snacks from HA showed the highest values of the inner area (Table 4), suggesting the potential  
308 application of this raw material to produce co-extruded snacks to be filled. While using corn flour,  
309 the snack with the highest inner area was obtained when HA was blended with C (Table 4).

310 The highest values of both bulk density and porosity were obtained when corn break meal was  
311 used, in agreement with the lowest area (Table 4). Other authors found a similar relation between  
312 bulk density and expansion rate (Zhu et al., 2010; Tacer-Caba et al., 2014). As regards the hybrid  
313 type, using HA resulting in a snack with high bulk density and porosity. The higher particle size of  
314 break meal - together with its gelatinization difficulty - masks the effect of HA on these indices.

315 As regards hardness, snacks from corn break meal were generally firmer than those made from  
316 flour, because of their reduced section area (or diametric expansion) and increased bulk density  
317 (Table 4).

318 The effect of the type of hybrid and amylose content is evident just in the case of corn flour.  
319 Specifically, using HA flour determined the production of a firmer snack, suggesting that amylose  
320 played a significant role in determining the mechanical strength of the products, as already shown  
321 in soy protein - high amylose starch extrudates (Zhu et al., 2010). Several factors might account  
322 for the mechanical properties of snacks, including volume, average cell size and cell size  
323 distribution, thus porosity (Zhu et al., 2010). This result could be justified by the high bulk density

324 of this sample compared to the others. Confirming the above, this sample showed the smallest  
325 section area, which indicated a more compact structure which better resisted compression load.  
326 A different behaviour was observed about the samples obtained from corn break meal; in this  
327 case, the hardest samples were the one obtained from C-W blend. However, it is important to  
328 note that C, W and HA were not significantly different in hardness. This could be due to the coarse  
329 particle size that limits starch gelatinisation even in C and W, that are usually able to gelatinize,  
330 in agreement with both pasting profiles (Figure 2).  
331 As for samples from blends, in both corn flour and break meal, hardness values are different from  
332 what we might expect analysing the raw materials. These behaviours are probably due to a  
333 particular rearrangement of starch during the dry-extrusion process, that is worthy of further  
334 investigation.

#### 335 **4. Conclusions**

336 This study provided an insight into the interactions between amylose content and type of milling  
337 fraction in defining the characteristics of corn snacks.

338 As regards bioactive compounds, HA confirmed the highest antioxidant capacity and phenolic  
339 acid content, maintaining superior content of these phytochemicals in the related snacks.  
340 Moreover, for each hybrid the corn flour fraction reported a marked antioxidant capacity compared  
341 to break meal. Furthermore, in order to obtain healthier foods, the opportunity to use these finer  
342 milling fractions, need to be carefully considered, in particular for genotypes more subject to  
343 environmental stress such as high amylose corn, taking in consideration their higher risk for  
344 fumonisin and other mycotoxin contamination (Vanara et al., 2018).

345 W and C corn (with 2 and 18% amylose content, respectively) led to more expanded and softer  
346 snacks. In the case of co-extruded snack, the best results in terms of texture, porosity, bulk  
347 density, and section area expansion were obtained using flour from HA (40% amylose). The high  
348 compact structure of this kind of snack is related to the peculiar starch properties of HA, which



349 results in the lowest gelatinization degree. Starch gelatinization properties were also restricted  
350 when corn break meal (with higher particle size) was used instead of corn flour. In this case, the  
351 milling fraction seems to mask the effect of amylose content. Blending both HA and W hybrids to  
352 the C one led to snacks whose features did not follow a linear trend with the amylose content,  
353 suggesting that beside the latter, also the starch structure/properties are strategic in defining the  
354 quality of the final product. Taking into consideration these findings, the particular rearrangement  
355 of starch when different hybrids are blended during the dry extrusion process is worthy of further  
356 studies.

357 **Declaration of Competing Interest.** The authors declare that they have no known competing  
358 financial interests or personal relationships that could have appeared to influence the work  
359 reported in this paper.

360 **Acknowledgements:** This work was supported by Regione Piemonte (POR FESR 2014-2020),  
361 as a part of the EXFREE Project. The authors thank Mr. Davide Carrara (DeFENS, Università  
362 degli Studi di Milano), Dr. Alessandro Peila (Molino Peila S.p.A.), Dr. Umberto Lenzi (Fudex Group  
363 S.p.A.) for technical support.

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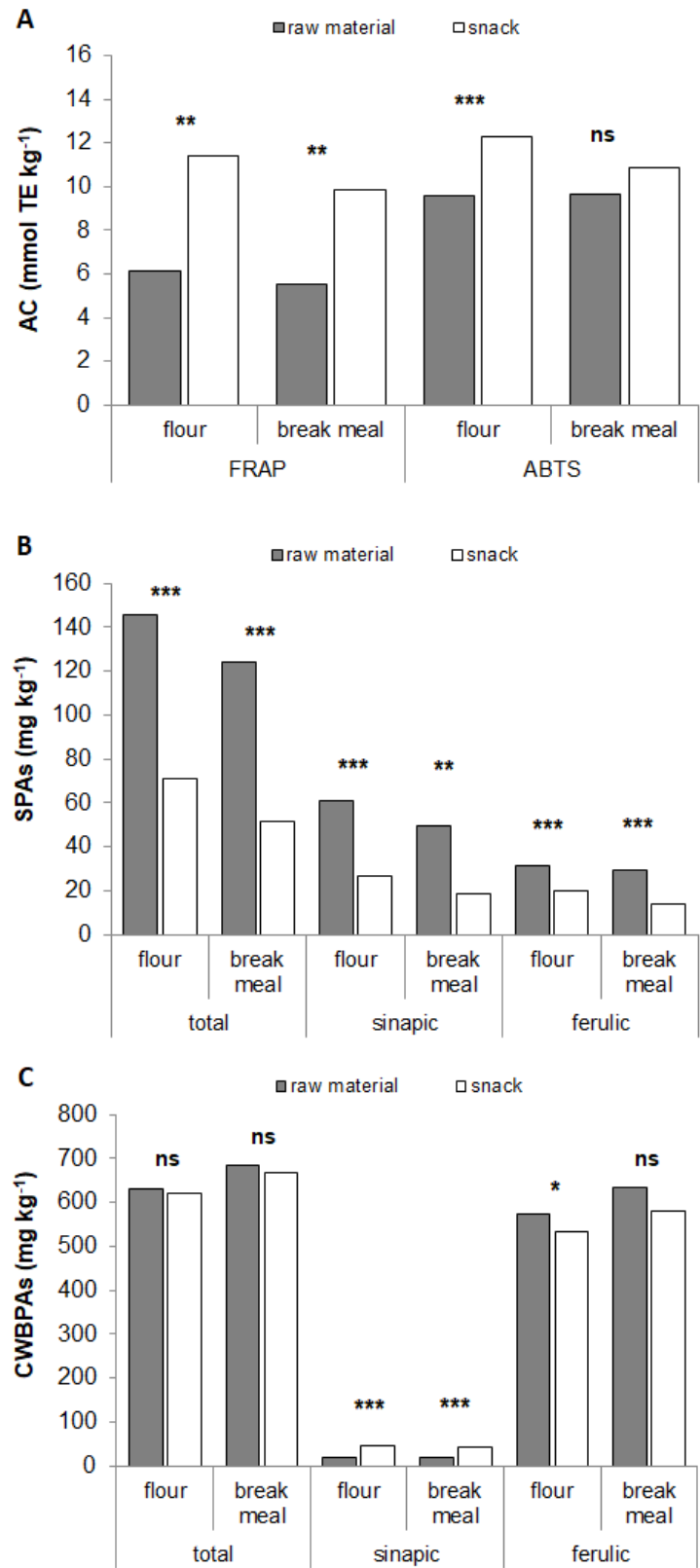
457 **Figure captions**

458 **Figure 1.** Figure 1. Antioxidant capacity (FRAP and ABTS assay, panel A), total, sinapic and  
459 ferulic soluble phenolic acids (SPAs; panel B) and total, sinapic and ferulic cell wall-bound  
460 phenolic acids (CWBPAs; panel C) detected in the high-amylose hybrid raw materials (grey bars)  
461 and snacks (white bars).

462 Data are expressed on a dw basis. Level of significance of ANOVA: ns=p-value >0.05; \*=p-value  
463 <0.05; \*\*=p-value <0.01; \*\*\*=p-value<0.001. Reported values are based on 3 replications.

464 **Figure 2.** Pasting profiles of break meal (panel A) and flours (panel B) from conventional hybrid  
465 (grey), waxy hybrid (yellow), high-amylose hybrid (orange), conventional-high amylose blend  
466 (green) and conventional-way blend (blue).

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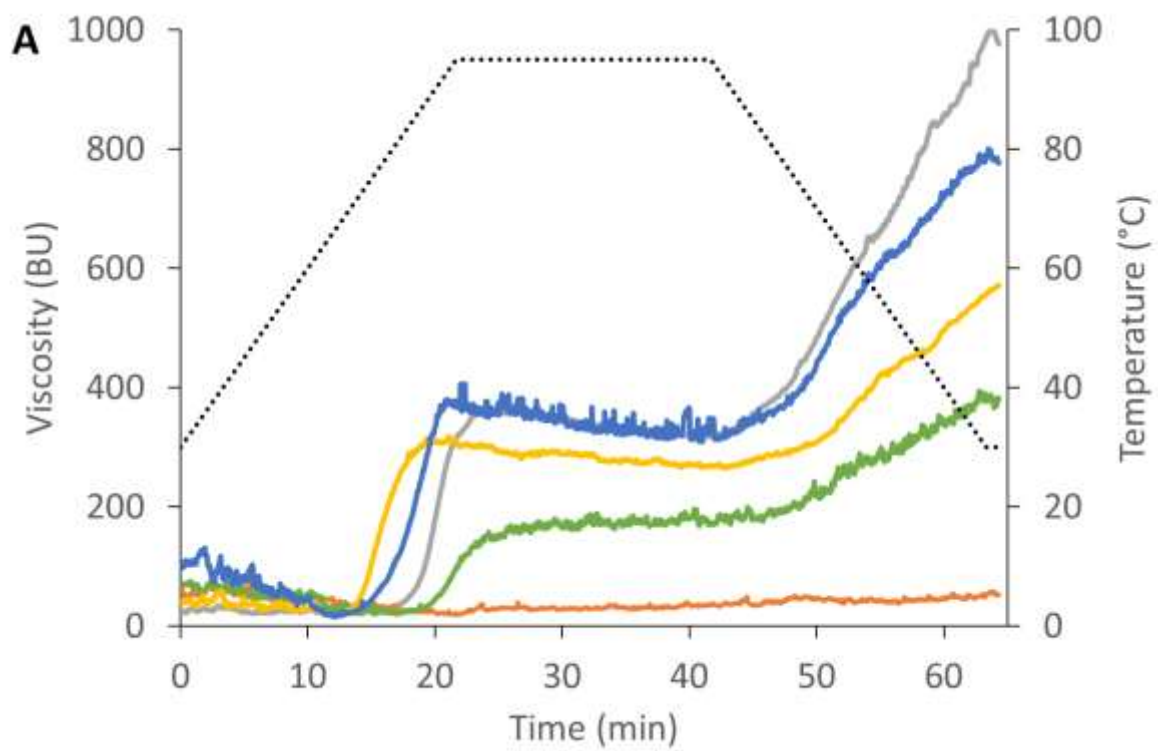
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Figure 1. Antioxidant capacity (FRAP and ABTS assay, panel A), total, sinapic and ferulic soluble phenolic acids (SPAs; panel B) and total, sinapic and ferulic cell wall-bound phenolic acids

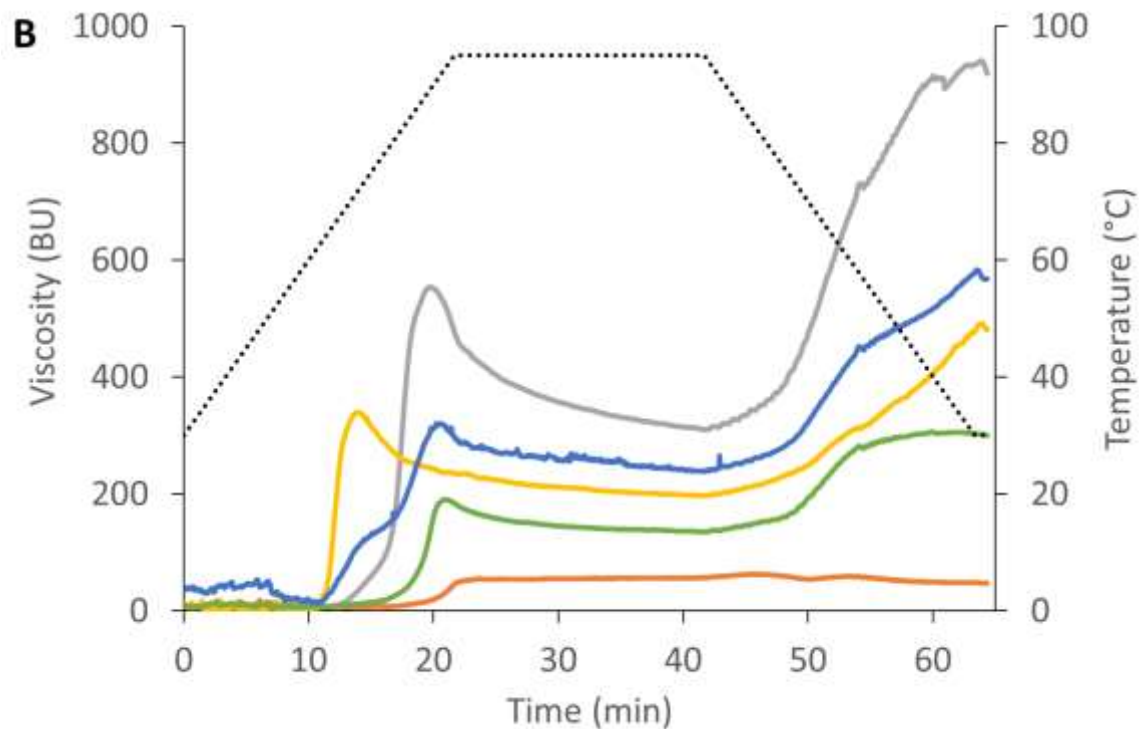
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 484 (green) and conventional-way blend (blue).  
 485

Table 1. Soluble (free and conjugated forms) phenolic acids (SPAs), cell wall -bound phenolic acids (CWBPA), and antioxidant capacity (AC) detected in the corn raw material and derived snacks.

Product	Milling fraction	Corn hybrids	SPAs <sup>1</sup> mg/kg	CWBPA <sup>1</sup> mg/kg	AC-FRAP mmol TE/kg	AC-ABTS mmol TE/kg
Raw materials	break meal (250-500 µm)	C	87.3±5.1 <sup>d</sup>	385.2±4.6 <sup>c</sup>	3.6±0.0 <sup>f</sup>	7.0±0.1 <sup>e</sup>
		C-HA	104.7±10.6 <sup>cd</sup>	561.1±26.4 <sup>b</sup>	4.4±0.2 <sup>e</sup>	8.2±0.2 <sup>cd</sup>
		HA	124.4±8.2 <sup>b</sup>	685.7±78.2 <sup>a</sup>	5.5±0.5 <sup>def</sup>	9.6±0.5 <sup>a</sup>
		C-W	94.2±2.2 <sup>cd</sup>	347.9±23.3 <sup>c</sup>	3.6±0.1 <sup>f</sup>	7.8±0.1 <sup>de</sup>
		W	106.3±6.7 <sup>c</sup>	398.6±41.8 <sup>c</sup>	3.9±0.3 <sup>ef</sup>	7.4±0.5 <sup>de</sup>
	flour (< 150 µm)	C	131.3±3.8 <sup>ab</sup>	448.3±34.4 <sup>c</sup>	5.2±0.1 <sup>abcd</sup>	8.6±0.5 <sup>bcd</sup>
		C-HA	140.7±0.7 <sup>ab</sup>	538.6±53.2 <sup>b</sup>	5.3±0.6 <sup>abc</sup>	8.9±0.4 <sup>abc</sup>
		HA	145.7±10.1 <sup>a</sup>	629.3±17.8 <sup>ab</sup>	6.2±0.7 <sup>a</sup>	9.6±0.4 <sup>ab</sup>
		C-W	130.2±4.4 <sup>ab</sup>	442.4±26.0 <sup>c</sup>	4.5±0.1 <sup>cde</sup>	7.9±0.2 <sup>de</sup>
		W	143.7±9.0 <sup>a</sup>	426.7±19.6 <sup>c</sup>	4.8±0.1 <sup>bcd</sup>	8.0±0.5 <sup>cde</sup>
Snacks	break meal (250-500 µm)	C	32.8±3.0 <sup>c</sup>	380.6±21.9 <sup>e</sup>	7.0±0.2 <sup>cde</sup>	8.5±0.2 <sup>d</sup>
		C-HA	32.8±0.6 <sup>c</sup>	508.7±62.5 <sup>cd</sup>	5.9±0.8 <sup>e</sup>	10.1±0.3 <sup>bc</sup>
		HA	51.4±9.9 <sup>b</sup>	666.6±41.2 <sup>a</sup>	9.9±1.0 <sup>b</sup>	10.9±0.6 <sup>b</sup>
		C-W	30.8±5.7 <sup>c</sup>	422.5±41.4 <sup>de</sup>	6.2±0.2 <sup>de</sup>	8.7±0.3 <sup>d</sup>
		W	34.7±0.7 <sup>c</sup>	453.2±0.7 <sup>cde</sup>	6.2±0.2 <sup>e</sup>	8.4±0.1 <sup>d</sup>
	flour (< 150 µm)	C	48.3±2.3 <sup>b</sup>	466.3±40.2 <sup>cde</sup>	8.6±0.2 <sup>cd</sup>	10.1±0.3 <sup>bc</sup>
		C-HA	35.0±0.7 <sup>c</sup>	553.2±45.2 <sup>bc</sup>	7.6±0.9 <sup>cde</sup>	9.8±0.4 <sup>c</sup>
		HA	71.4±0.7 <sup>a</sup>	619.6±41.2 <sup>ab</sup>	11.4±1.0 <sup>a</sup>	12.3±0.5 <sup>a</sup>
		C-W	26.5±0.9 <sup>c</sup>	489.5±18.4 <sup>cd</sup>	6.8±0.4 <sup>de</sup>	8.1±0.3 <sup>d</sup>
		W	35.3±0.5 <sup>c</sup>	493.2±36.8 <sup>cd</sup>	7.8±0.5 <sup>cd</sup>	8.6±0.3 <sup>d</sup>

Data are expressed on a dw basis. Within each product (raw materials or snacks), means ± standard deviation followed by different letters in the same column are significantly different, according to the REGW-Q test (p<0.001). Reported values are based on 3 replications. <sup>1</sup> sum of the SPAs and CWBPAs determined by means of the RP-HPLC/DAD

C, conventional hybrid; C-HA, conventional:high amylose hybrid blend (50:50); C-W, conventional:waxy hybrid blend (50:50); HA, high-amylose hybrid; W, waxy hybrid; AC-ABTS, antioxidant capacity by means of the ABTS assay; AC-FRAP, antioxidant capacity by means of the FRAP assay.

Table 2. Starch susceptibility to  $\alpha$ -amylase hydrolysis (g/100g dw).

	Raw materials		Snacks	
	Break meal (250-500 $\mu$ m)	Flour (<150 $\mu$ m)	Break meal (250-500 $\mu$ m)	Flour (<150 $\mu$ m)
C	3.6 $\pm$ 0.1 <sup>d</sup>	4.7 $\pm$ 0.2 <sup>c</sup>	61.3 $\pm$ 1.7 <sup>AB</sup>	59.5 $\pm$ 1.7 <sup>B</sup>
C-HA	3.0 $\pm$ 0.2 <sup>e</sup>	5.7 $\pm$ 0.2 <sup>b</sup>	51.9 $\pm$ 2.7 <sup>CD</sup>	52.5 $\pm$ 3.3 <sup>C</sup>
HA	2.5 $\pm$ 0.2 <sup>f</sup>	5.6 $\pm$ 0.1 <sup>b</sup>	48.1 $\pm$ 1.0 <sup>D</sup>	48.4 $\pm$ 2.1 <sup>D</sup>
C-W	3.4 $\pm$ 0.2 <sup>de</sup>	5.8 $\pm$ 0.1 <sup>b</sup>	56.3 $\pm$ 3.6 <sup>E</sup>	58.2 $\pm$ 1.8 <sup>B</sup>
W	3.4 $\pm$ 0.2 <sup>de</sup>	6.8 $\pm$ 0.3 <sup>a</sup>	59.6 $\pm$ 2.2 <sup>B</sup>	66.5 $\pm$ 3.0 <sup>A</sup>

Within each product (raw materials or snacks), means  $\pm$  standard deviation followed by different letters are significantly different, according to the REGW-Q test ( $p < 0.001$ ). Reported values are based on two replications. Lowercase letters refer to raw materials; uppercase letters refer to snacks.

C, conventional hybrid; C-HA, conventional:high amylose hybrid blend (50:50); C-W, conventional:waxy hybrid blend (50:50); HA, high-amylose hybrid; W, waxy hybrid.

Table 3. Pasting properties of break meal and flour fractions.

Parameters	Milling fraction	C	C-HA	HA	C-W	W
Pasting temperature (°C)	Break meal (250-500 µm)	77.1±1.8 <sup>c</sup>	89.5±0.7 <sup>a</sup>	-	72.2±1.3 <sup>d</sup>	70.1±0.2 <sup>de</sup>
	Flour (<150 µm)	68.2 ± 1.2 <sup>e</sup>	76.9±1.5 <sup>c</sup>	86.2±1.2 <sup>b</sup>	66.8±0.1 <sup>ef</sup>	64.1±1.4 <sup>f</sup>
Maximum viscosity (°C)	Break meal (250-500 µm)	94.9±0.01 <sup>a</sup>	95.1±0.1 <sup>a</sup>	-	92.0±0.01 <sup>ab</sup>	89.2±3.4 <sup>b</sup>
	Flour (<150 µm)	88.9±0.1 <sup>b</sup>	93.9±1.9 <sup>a</sup>	95.1±0.1 <sup>a</sup>	90.5±0.1 <sup>b</sup>	73.1±2.1 <sup>c</sup>
Maximum viscosity (UB)	Break meal (250-500 µm)	347.5±16.2 <sup>b</sup>	178.5±0.7 <sup>c</sup>	-	380.5±0.7 <sup>b</sup>	300.0±24.0 <sup>b</sup>
	Flour (<150 µm)	556.0±2.8 <sup>a</sup>	201.5±16.3 <sup>c</sup>	58.1±1.4 <sup>d</sup>	358.3±53.7 <sup>b</sup>	347.2±11.3 <sup>b</sup>
Breakdown (UB)	Break meal (250-500 µm)	37.0±5.6 <sup>de</sup>	13.5±6.3 <sup>ef</sup>	-	55.0±2.83 <sup>d</sup>	44.0±5.6 <sup>de</sup>
	Flour (<150 µm)	247.5±4.9 <sup>a</sup>	44.5±11.9 <sup>de</sup>	-	96.5±21.9 <sup>c</sup>	154.5±18.1 <sup>b</sup>
Final viscosity (UB)	Break meal (250-500 µm)	952.5±33.2 <sup>a</sup>	376.5±4.9 <sup>de</sup>	-	781.0±5.6 <sup>b</sup>	559.5±19.0 <sup>c</sup>
	Flour (<150 µm)	922.0±2.8 <sup>a</sup>	327.5±39.3 <sup>e</sup>	47.5±0.7 <sup>f</sup>	617.0±69.3 <sup>c</sup>	461.5±27.6 <sup>d</sup>
Setback (UB)	Break meal (250-500 µm)	637.0±48.0 <sup>a</sup>	220.0±11.3 <sup>de</sup>	-	479.0±15.5 <sup>b</sup>	294.5±9.1 <sup>d</sup>
	Flour (<150 µm)	625.5±4.9 <sup>a</sup>	174.5±12.2 <sup>e</sup>	-	370.0±42.4 <sup>c</sup>	265.5±21.9 <sup>d</sup>

Means ± standard deviation followed by different letters are significantly different, according to the REGW-Q test ( $p < 0.001$ ). Reported values are based on two replications.

Pasting temperature, temperature at which an initial increase in viscosity occurs; maximum viscosity, maximum viscosity reached during the analysis; peak temperature, temperature at the maximum viscosity; breakdown, difference between the maximum viscosity and the viscosity reached at the end of the holding period; setback, difference between the final viscosity at 30°C and the viscosity reached at the end of the holding period.

C, conventional hybrid; C-HA, conventional:high amylose hybrid blend (50:50); C-W, conventional:waxy hybrid blend (50:50); HA, high-amylose hybrid; W, waxy hybrid

Table 4. Features of snacks made from either break meal and flour fractions.

Parameters	Milling fraction	C	C-HA	HA	C-W	W
Section area (mm <sup>2</sup> )	Break meal (250-500 μm)	356.3 ± 19.7 <sup>a</sup>	294.0 ± 24.8 <sup>c</sup>	235.2 ± 17.7 <sup>d</sup>	300 ± 18.2 <sup>bc</sup>	282.5 ± 34.3 <sup>c</sup>
	Flour (<150 μm)	376.2 ± 21.7 <sup>a</sup>	294.5 ± 21.4 <sup>c</sup>	232.7 ± 15.6 <sup>d</sup>	353.1 ± 14.7 <sup>a</sup>	322.1 ± 16.2 <sup>b</sup>
Inner area (mm <sup>2</sup> )	Break meal (250-500 μm)	21.0 ± 7.4 <sup>bcd</sup>	43.5 ± 5.7 <sup>a</sup>	42.5 ± 6.0 <sup>a</sup>	27.3 ± 4.2 <sup>bc</sup>	23.5 ± 3.8 <sup>bcd</sup>
	Flour (<150 μm)	23.5 ± 5.9 <sup>bcd</sup>	39.6 ± 5.6 <sup>a</sup>	27.4 ± 2.9 <sup>b</sup>	17.6 ± 7.4 <sup>d</sup>	19.5 ± 4.3 <sup>de</sup>
Bulk density (gcm <sup>-3</sup> )	Break meal (250-500 μm)	1.60	1.65	2.20	1.67	1.60
	Flour (<150 μm)	1.16	1.30	1.38	1.51	1.40
Porosity (%)	Break meal (250-500 μm)	51.8	45.4	67.1	64.0	60.9
	Flour (<150 μm)	30.7	56.8	67.3	50.4	39.5
Hardness (N)	Break meal (250-500 μm)	29.4 ± 1.2 <sup>a</sup>	21.3 ± 1.1 <sup>bc</sup>	28.2 ± 1.2 <sup>a</sup>	12.9 ± 1.4 <sup>d</sup>	33.1 ± 2.5 <sup>a</sup>
	Flour (<150 μm)	19.2 ± 0.5 <sup>c</sup>	20.5 ± 0.5 <sup>c</sup>	27.9 ± 0.5 <sup>a</sup>	11.8 ± 0.5 <sup>d</sup>	23.3 ± 0.5 <sup>b</sup>

Means ± standard deviation followed by different letters are significantly different, according to the REGW-Q test (p<0.001). Reported values are based on thirty replications for harness and on ten replications for section area and inner area.

C, conventional hybrid; C-HA, conventional:high amylose hybrid blend (50:50); C-W, conventional:waxy hybrid blend (50:50); HA, high-amylose hybrid; W, waxy hybrid.

