

1 **Sweet-and-salty biocatalysis: fructooligosaccharides production using**
2 ***Cladosporium cladosporioides* in seawater**

3
4 Paolo Zambelli • Immacolata Serra • Lucia Fernandez-Arrojo • Francisco J. Plou • Lucia
5 Tamborini • Paola Conti • Martina L. Contente • Francesco Molinari • Diego Romano*

6
7 diego.romano@unimi.it; phone +39 0250319148; fax 02 50319191.

8
9

P. Zambelli, I. Serra, M. L. Contente, F. Molinari, D. Romano

10 Department of Food, Environmental and Nutritional Sciences (DeFENS),
11 University of Milan
12 Via Mangiagalli 25, 20133 Milan, Italy

13
14 L. Fernandez-Arrojo, F. J. Plou,
15 Instituto de Catálisis y Petroleoquímica CSIC
16 28049 Madrid, Spain

17
18 L. Tamborini, P. Conti
19 Department of Pharmaceutical Sciences (DISFARM)
20 University of Milan,
21 Via Mangiagalli 25, 20133 Milano, Italy

22

23
24 **Abstract** Production of fructooligosaccharides (FOS) from sucrose was obtained using a
25 bioprocess entirely performed in seawater. The halophilic fungus *Cladosporium cladosporioides*
26 MUT 5506 was grown in a seawater-based medium and mycelium displayed an optimal activity
27 in seawater at 50-60 °C, being stable up to 60 °C. Under optimized conditions in seawater (50 °C,
28 sucrose 600 g/L, lyophilized mycelium 40 g/L), *C. cladosporioides* gave a maximum FOS yield
29 of 344 g/L after 72 h with a preponderance of ¹F-FOS derivatives (1-kestose 184 g/L, 1-nystose
30 98 g/L and 1-fructofuranosylnystose 22 g/L), and the noteworthy presence of the non-
31 conventional disaccharide blastose (30 g/L after 144 h). Lyophilized mycelium exhibited good
32 stability in seawater (76% of the initial activity was retained after 15 cycles of reutilization). This
33 proof-of-concept application reports for the first time the production of FOS in a non-
34 conventional medium such as seawater.

35 **Keywords** Fructooligosaccharides • fructofuranosidase • *Cladosporium cladosporioides* •
36 seawater • biocatalysis

37
38
39
40
41
42
43
44
45
46
47
48
49

50 **Introduction**

51 Industrial bioprocesses are characterized by large consumption of fresh water. The development
52 of new (bio) processes should focus not only on efficiency, but also on their sustainability. On
53 Earth, there is a vast quantity of seawater (96.5%) compared to the small amount of fresh water
54 (2.5%) and brackish water (1%) [1]. Therefore, the possible use of non-potable water (i.e.,
55 wastewater or seawater) as a medium for large-scale bioprocesses seems to be a remarkable field
56 of research [2,3]. Halotolerant microorganisms producing enzyme of potential industrial interest
57 are of great interest for developing biotransformations in seawater [4,5].

58 The facultative halophilic fungus *Cladosporium cladosporioides* was recently discovered as an
59 efficient producer of fructooligosaccharides (FOS) from sucrose [6]; lyophilized mycelium of
60 *Cladosporium cladosporioides* gave mainly 1-kestose, 1-nystose, ¹F-fructosylnystose, 6-kestose,
61 neokestose, but also blastose, an unconventional disaccharide ([Fru-β(2→6)-Glc]). FOS are
62 prebiotics used as food ingredients due to their beneficial properties [7,8], such as low caloric
63 intake (2 kcal/g), low glycemic impact, prebiotic action, improved gut absorption of Ca²⁺ and
64 Mg²⁺, lowering blood lipid levels, prevention of urogenital infections, reduced risk of colon
65 cancer and reduction total cholesterol and triglycerides [9,10]. Short-chain ¹F-FOS (mostly 1-
66 kestose, 1-nystose, ¹F-fructosylnystose,) are produced from concentrated sucrose solutions using
67 fungal transfructosylating enzymes, such as *Aspergillus aculatus* [11], *Aspergillus japonicas*
68 [12], *Aspergillus oryzae* [13], *Aspergillus niger* [14], *Aureobasidium pullulans* [15] and
69 *Penicillium citrinum* [16].

70 In this work, we evaluated the possibility to perform FOS production in seawater using
71 lyophilized mycelium of *Cladosporium cladosporioides* grown in seawater; lyophilized mycelia
72 of fungi are easy-to-handle biocatalysts suitable for exploiting mycelium-bound enzymatic
73 activities, often showing remarkable long-term stability [17,18].

74

75

76 **Materials and methods**

77 **Materials**

78 Sucrose, glucose, fructose, 3,5-dinitrosalicylic acid (DNS) were purchased from Sigma Aldrich.
79 1-Kestose and 1-nystose were purchased from Fluka. 1-Fructofuranosylnystose was purchased
80 from Megazyme. Yeast extract was purchased from Difco and barley malt flour from Diagermal.
81 Malt extract was from Merck. All reagents and solvents were of the highest available purity and
82 used as purchased. Seawater (pH 7.5) was collected from the Camogli beach (Genova, Italy) and
83 maintained at 4 °C after microfiltration; water salinity of 35 PSU (Practical Salinity Units) was
84 reported by ARPA (Agenzia Regionale Prevenzione e Ambiente) website for this area.

85 **Cultures production**

86 *C. cladosporium* was previously isolated ^[1] and deposited at Mycotheca Universitatis
87 Taurinensis (MUT) as strain MUT 5506. *C. cladosporium* was routinely maintained on MYA
88 slants (Barley malt flour 100 g L⁻¹ yeast extract 5 g L⁻¹, agar 15 g L⁻¹, pH 5.6) at 4 °C. *C.*
89 *cladosporium* was cultivated in 1 L-Erlenmeyer flasks containing 100 mL of liquid medium
90 (Barley malt flour 100 g L⁻¹, yeast extract 5 g L⁻¹, seawater) for 96 h at 28 °C on a reciprocal
91 shaker (150 spm). Mycelium was harvested by filtration at 4 °C and suspended in deionized
92 water, frozen at -20 °C, and finally lyophilized (Alfa Criosec, Milan, Italy) at plate temperature
93 of 25 °C.

94

95 **Biotransformations**

96 The biotransformation under optimized conditions was performed using lyophilized mycelium
97 (400 mg) suspended in a solution of seawater (10 mL) containing in 6 of sucrose and incubated
98 at 50 °C in an orbital shaker at 90 rpm. The biotransformation was followed by HPLC; at
99 different times, aliquots (100 µL) were withdrawn, diluted with 400 µL of water, incubated for
100 10 min at 90°C to inactivate the enzymes, and analysed by HPLC.

101 Lyophilized mycelium was reused in successive cycles. At the end of 24 h, the biotransformation
102 mixture was centrifuged, the mycelium washed twice with seawater and re-suspended in
103 seawater containing sucrose (600 g/L).

104

105 Fructofuranosidase activity assays

106 The enzymatic activity of the lyophilized mycelium was assayed using the dinitrosalicylic acid
107 (DNS) method adapted to a 96-well microplate scale.^[2] A calibration curve was performed with
108 a 3 g/L fructose solution. Lyophilized mycelia (10 g/L) were incubated with 1 mL of a sucrose
109 solution (100 g/L) in acetate buffer (20 mM pH 6.0) for 20 min at 50 °C and 90 rpm. 50 µL of
110 the solution, conveniently diluted to fit into the calibration curve, were added to each well. Then,
111 50 µL of 10 g/L DNS were added. The plate was incubated for 20 min at 80 °C to develop colour
112 with a seal plate tape (GeneMate). After cooling, 150 µL of water was added to each well, and
113 the absorbance measured at 540 nm using a microplate reader (model Versamax, Molecular
114 Devices). One unit (U) of activity was defined as that catalysing the formation of 1 µmol
115 reducing sugar per minute. Lyophilized mycelia were incubated in the range of pH 3-9 and
116 temperature 25-80 °C to evaluate the maximum of activity. Residual activity of lyophilized
117 mycelia was calculated after different periods of time (2 and 24 h) before substrate addition at
118 pH and temperatures in the range of 3-9 and 40-80 °C respectively. The residual activity was
119 measured at pH 6.0 acetate buffer 20 mM, 50 °C with the DNS method described above.

120

121 HPLC analysis

122 Analysis of FOS composition was carried out by high-performance anion-exchange
123 chromatography coupled with pulsed amperometric detection (HPAEC-PAD) on a Dionex
124 ICS3000 system consisting of an SP gradient pump, an electrochemical detector with a gold
125 working electrode and Ag/AgCl as reference electrode, and an autosampler (model AS-HV). All
126 eluents were degassed by flushing with helium. A pellicular anion-exchange 4 × 250 mm Carbo-

127 Pack PA-1 column (Dionex) connected to a 4 × 50 mm CarboPac PA-1 guard column was used
128 at 30°C. Eluent preparation was performed with Milli-Q water and NaOH. The initial mobile
129 phase (at 0.5 mL/min) was 100 mM NaOH. A gradient from 0 to 200 mM sodium acetate was
130 performed in 50 min at 0.5 mL/min, and 200 mM sodium acetate was maintained for 25 min.
131 The chromatograms were analyzed using Chromeleon software. The identification of the
132 different carbohydrates was done on the basis of standards commercially available or purified in
133 our laboratory [6].

134

135 Transferase/hydrolase ratio

136 The amount of free fructose (measured by HPLC) is a direct measurement of hydrolytic activity
137 whereas the amount of glucose (measured by HPLC) minus the amount of free fructose
138 corresponds to the transferase activity [11]. Accordingly, a transferase/hydrolase index (T/H
139 index) was calculated using the following equation: $T/H = ([\text{glucose}] - [\text{fructose}])/[\text{fructose}]$.

140

141 **Results**

142 The use of lyophilized mycelium of *Cladosporium cladosporioides* MUT 5506 in freshwater
143 allowed the production of FOSs with a maximum yield of 57% starting from a 600 g/L of
144 sucrose solution. Interestingly, *C. cladosporioides* synthesized a mixture of ¹F-FOS, ⁶F-FOS and
145 ⁶G-FOS, including the presence of a non-conventional disaccharide (blastose). *C.*
146 *cladosporioides* was grown in a seawater-based medium and the biotransformation with
147 mycelium-bound β-fructofuranosidase was evaluated using different amounts of lyophilized
148 mycelium in seawater, using sucrose (600 g/L) as substrate at 30 °C (Table 1).

149 **TABLE 1**

150 Maximum FOS production was always registered after 96 h. The highest yields were obtained
151 using 40 g/L of dry mycelium, and this biocatalyst concentration was used in the following

152 experiments aimed at evaluating the effects of temperature. The reaction rates increased up to
153 60 °C and then decreased rapidly due to thermal inactivation (Figure 1). Thermal stability in
154 seawater was determined by measuring the residual activity after 24 h of incubation over a
155 temperature range from 25 to 80 °C (Figure 1). Mycelium-bound activity was fully maintained
156 up to 50 °C, above which a gradual decrease of stability was observed, with significant
157 inactivation (40% of lost activity) at temperatures above 80 °C. Thus, the best compromise
158 between activity and stability was found at 50 °C.

159 **FIGURE 1**

160 The time-course of FOS production carried out under optimized conditions (40 g/L of
161 lyophilized mycelium, 50 °C, 600 g/L of sucrose) in seawater is reported in Figure 2, while total
162 FOS production and transferase/hydrolase ratio (expressed as T/H index) are reported in Table 2.

163 **TABLE 2**

164 The highest amount of FOS (344 g/L) was reached after 72, with a preponderance of ¹F-FOS
165 derivatives (1-kestose 184 g/L, 1-nystose 98 g/L and 1-fructofuranosylnystose 22 g/L at 72 h)
166 and significantly lower concentrations of 6-kestose (12 g/L), neo-kestose (11 g/L), and neo-
167 nystose (6 g/L). The highest amount of the non-conventional disaccharide blastose was observed
168 at 144 h (30 g/L). The ratio between transfructosylating and hydrolytic activity (T/H index) was
169 very high until 72 h and decreased at prolonged times, as expected for fructofuranosidase-
170 catalyzed biotransformations [19].

171 The reuse of lyophilized mycelium was studied in a batch reactor measuring the activity in a
172 sequence of reaction cycles in seawater. Figure 3 illustrates the operational stability of the
173 lyophilized mycelium in 15 successive reaction cycles of 24 h each. Lyophilized mycelium of *C.*
174 *cladosporioides* retained 76% of the initial activity after 15 cycles of reutilization.

175 **FIGURE 3**

176 **Discussion**

177 Fructofuranosidases can catalyze the synthesis (from sucrose) or hydrolysis of
178 fructooligosaccharides (FOS) [19]. During the synthesis of FOS, one molecule of sucrose acts as
179 fructose donor (releasing one molecule of glucose) and another is the fructose acceptor for GF2
180 synthesis; the extension of the FOS chain involves GF2 as fructose acceptor and another
181 molecule of sucrose as fructose donor, thus generating GF3 [20]. Alternatively,
182 fructofuranosidases may also catalyse the hydrolysis of FOS, thus releasing fructose. Therefore,
183 the maximal fructooligosaccharides production depends on the ratio between transfructosylation
184 and hydrolysis, deductible from the relative amounts of glucose and fructose formed during the
185 biotransformation [19].

186 The more efficient bioprocesses for producing FOS described in literature furnish yields in the
187 range of 54-61% of total FOS starting from 400-700 g/L of sucrose in freshwater [21]. In all
188 these bioprocesses, the transfructosylation/hydrolysis ratio is a key-factor for determining high
189 yields of FOSs. In a recent work, we reported that a strain of the filamentous fungus
190 *Cladosporium cladosporioides* (now deposited at Mycotheca Universitatis Taurinensis as strain
191 MUT 5506) showed high mycelium-bound transfructosylating activity, furnishing a maximum
192 FOS yield of 56%, when used in a conventional aqueous buffer [6]. The FOS mixture contained
193 ¹F-FOS, ⁶F-FOS and ⁶G-FOS, including the presence of a non-conventional disaccharide,
194 characterised and identified as blastose. The FOS yields observed using *C. cladosporioides* MUT
195 5506 are comparable with the ones described for the industrial biotransformation carried out
196 with enzymes from *Aspergillus niger* or *Aureobasidium pullulans*, but, in the case of *C.*
197 *cladosporioides*, a wider array of FOS with different glycosidic bonds is produced.

198 High yields of FOS depends on enzyme properties, but also on biotransformation conditions
199 suitable for favouring transfructosylation over hydrolysis (i.e., temperature, high sucrose
200 concentration and high salt concentration with consequent low water activity). During the
201 physiological characterization of *C. cladosporioides* MUT 5506, we noticed that this strain is a
202 facultative halophilic microorganism, being able to grow at different concentration of NaCl and

203 also in microfiltered seawater added with the necessary nutrients. This observation led us to
204 investigate the transfructosylating activity of the lyophilized mycelium of *C. cladosporioides*
205 MUT 5506 grown in seawater. The prospect to perform bioprocesses avoiding the consumption
206 of drinkable water seems a remarkable way for optimizing the use of natural resources in
207 sustainable bioprocesses [2].

208 Lyophilized mycelium of *C. cladosporioides* MUT 5506 grown in a seawater-based medium
209 produced 344 g/L (57% w/w) of total FOSs from 600 g/L of sucrose in seawater under optimized
210 conditions after 72 h. It should be pointed out that in all the experiments, seawater was only
211 microfiltered, with no further optimization/modification of the medium (e.g. pH, salt
212 composition). Interestingly, the overall performances were very similar (or even slightly better)
213 compared with what observed in a conventional buffer [6]. Hence, the use of seawater (both as
214 growth and biotransformation medium) resulted suitable for the overall process of FOS
215 production. The transfructosylating/hydrolysis ratio (expressed in this work as T/H index, see
216 Materials and methods) decreased during the reaction, indicating that fructooligosaccharides
217 were progressively hydrolysed; this phenomenon is commonly observed with
218 fructofuranosidase-catalyzed reactions [22,23]. Preliminary tests about the stability of the
219 mycelium-bound enzyme(s) in seawater indicated that 76% of the original activity was
220 maintained after 15 cycles of biotransformation, opening the possibility of studies for setting up
221 continuous processes.

222 In conclusion, the production of fructooligosaccharides using lyophilized mycelium of the
223 halophilic fungus *Cladosporium cladosporioides* MUT 5506 was entirely accomplished in
224 seawater. This proof-of-concept application reports for the first time the production of alternative
225 sweeteners by using a bioprocess where the biocatalyst was produced and used in a non-
226 conventional medium, such as seawater. [Purification of FOS from salts and other impurities
227 \(including the main by-product glucose\) can be efficiently performed by nanofiltration \[24\] or
228 simulated moving bed \(SMB\) chromatography \[25\]; more recently, a simple and effective](#)

229 [process using activated charcoal for directly purifying FOS from a fermentative broth was](#)
230 [proposed \[26\].](#)

231

232 **Acknowledgements**

233 This work was supported by the European Community FP7-KBBE.2012.3.2-02 project
234 MACUMBA, grant agreement N. 311975.

235

236

237

238

239

240

241

242

243

244

245

246

247

248

249

250

251

252

253

254

255

256

257
258
259
260
261
262
263
264
265
266
267
268
269
270
271
272
273
274
275
276
277
278
279
280
281

References

- [1] Gleick HP. In *Water in Crisis-A Guide to the World's Fresh-Water Resources*. Eds.: P. H. Gleick; Oxford University Press; New York. 1993.
- [2] Domínguez de María P. On the use of seawater as reaction media for large-scale applications in biorefineries. *ChemCatChem* 2013; 5:1643–1648.
- [3] Grande PM, Domínguez de María P. Enzymatic hydrolysis of microcrystalline cellulose in concentrated seawater. *Bioresour Technol* 2011; 104:799–802.
- [4] Dionisi HM, Lozada M, Olivera NL. Bioprospection of marine microorganisms: biotechnological applications and methods. *Rev Argent Microbiol* 2012; 44:49–60.
- [5] Trincone A. Marine biocatalysts: enzymatic features and applications. *Mar Drugs* 2011; 9:478–499.
- [6] Zambelli P, Fernandez-Arrojo L, Romano D, Santos-Moriano P, Gimeno-Perez M, Poveda A, Gandolfi R, Fernández-Lobato M, Molinari F, Plou FJ. Production of fructooligosaccharides by mycelium-bound transfructosylation activity present in *Cladosporium cladosporioides* and *Penicillium sizovae*. *Process Biochem* 2014; 49:2174–2180.
- [7] Ganaie MA, Lateef A, Gupta US. Enzymatic trends of fructooligosaccharides production by microorganisms. *Appl Biochem Biotechnol* 2014; 172:2143–2159.
- [8] Kovács Z, Benjamins E, Grau K, Rehman A, Ebrahimi M, Czermak P. *Adv Biochem Eng Biotechnol* 2014; 143:257–295.

- 282 [9] Sabater-Molina M, Larqué E, Torrella F, Zamora S. Dietary fructooligosaccharides and
283 potential benefits on health. *J Physiol Biochem* 2009; 65:315–328.
- 284 [10] Sangeetha PT, Ramesh MN, Prapulla SG. Recent trends in the microbial production,
285 analysis and application of fructooligosaccharides. *Trend Food Sci Technol* 2005; 16:442–
286 457.
- 287
- 288 [11] Ghazi I, Fernandez-Arrojo L, Garcia-Arellano H, Plou FJ, Ballesteros A. Purification and
289 kinetic characterization of a fructosyltransferase from *Aspergillus aculeatus*. *J Biotechnol*
290 2007; 128:204–211.
- 291 [12] Chien CS, Lee WC, Lin TJ. Immobilization of *Aspergillus japonicus* by entrapping cells in
292 gluten for production of fructooligosaccharides. *Enzyme Microb Technol* 2001; 29:252–257.
- 293 [13] Sangeetha PT, Ramesh MN, Prapulla SG. Production of fructo-oligosaccharides by
294 fructosyl transferase from *Aspergillus oryzae* CFR 202 and *Aureobasidium pullulans* CFR
295 77. *Process Biochem* 2004;39:753–758.
- 296 [14] L'Hocine L, Wang Z, Jiang B, Xu S. Purification and partial characterization of
297 fructosyltransferase and invertase from *Aspergillus niger* AS0023. *J Biotechnol* 2000;
298 81:73–84.
- 299 [15] Hayashi S, Yoshiyama T, Fuji N, Shinohara S. Production of a novel syrup containing
300 neofructooligosaccharides by the cells of *Penicillium citrinum*. *Biotechnol Lett* 2000;
301 22:1465–1469.
- 302 [16] Lim JS, Park MC, Lee JH, Park SW, Kim SW. Optimization of culture medium and
303 conditions for Neo-fructooligosaccharides production by *Penicillium citrinum*. *Eur Food*
304 *Res Technol* 2005; 221:639–644.

- 305 [17] Converti A, Del Borghi A, Gandolfi R, Lodi A, Molinari F, Palazzi E. Reactivity and
306 stability of mycelium-bound carboxylesterase from *Aspergillus oryzae*. Biotechnol Bioeng
307 2002; 77:232–237.
- 308 [18] Gandolfi R, Converti A, Pirozzi D, Molinari F. Efficient and selective microbial
309 esterification with dry mycelium of *Rhizopus oryzae*. J Biotechnol 2001; 92:21–26.
- 310 [19] Plou FJ, De Segura AG, Ballestreros A. Application of glycosidases and transglycosidases
311 in the synthesis of oligosaccharides. In: Polaina J and MacCabe AP (Eds.) Industrial
312 Enzymes. Springer, Dordrecht 2007; pp 141-157.
- 313 [20] Maugeri F, Hernalsteens S. Screening of yeast strains for transfructosylating activity. J Mol
314 Catal B Enzym 2007; 49:43–49.
- 315 [21] Mutanda T, Mokoena MP, Olaniran AO, Wilhelmi BS, Whiteley CG. Microbial enzymatic
316 production and applications of short-chain fructooligosaccharides and
317 inulooligosaccharides: recent advances and current perspectives. J Ind Microbiol Biotechnol
318 2014; 41:893–906.
- 319 [22] Álvaro-Benito M, de Abreu M, Fernández-Arrojo L, Plou FJ, Jiménez-Barbero J,
320 Ballesteros A, Polaina J, Fernández-Lobato M. Characterization of a β -fructofuranosidase
321 from *Schwanniomyces occidentalis* with transfructosylating activity yielding the prebiotic 6-
322 kestose. J Biotechnol 2007; 132:75–81.
- 323
- 324 [23] Linde D, Macias I, Fernandez-Arrojo L, Plou FJ, Jimenez A, Fernandez-Lobato M.
325 Molecular and biochemical characterization of a fructofuranosidase from
326 *Xanthophyllomyces dendrorhous*. Appl Environ Microbiol 2009; 75:1065–1073.
- 327
- 328 [\[24\] Goulas AK, Kapasakalidis PG, Sinclair HR, Rastall RA, Grandison AS. Purification of](#)
329 [oligosaccharides by nanofiltration. J Membr Sci 2002; 209:321–335.](#)

330

331 [\[25\]Vaňková K, Onderková Z, Antořová M, Polakovič M. Design and economics of industrial](#)
332 [production of fructooligosaccharides. Chem Pap 2008; 62:375–381.](#)

333

334 [\[26\]Nobre C, Teixeira JA, Rodrigues LR. Fructo-oligosaccharides purification from a](#)
335 [fermentative broth using an activated charcoal column. New Biotechnol 2012; 29:395-401.](#)

336

337

338

339 **Figure legends**

340

341 **Fig. 1.** Effect of temperature on activity and stability of lyophilized mycelium of *C.*
342 *cladosporioides* in seawater (pH 7.5). Stability is defined as residual activity determined at 50 °C
343 after pre-incubation of the lyophilised mycelia for 24 h in seawater at different temperatures.
344 Standard deviations were lower than 5%.

345 **Fig. 2.** Time-course of FOS production with lyophilized mycelium of *C. cladosporioides*.
346 Reaction conditions: 600 g/L sucrose, 40 g/L lyophilized mycelium, seawater (pH 7.5), 50 °C.
347 Results are the average of three triplicates, with standard deviations lower than 5%. Standard
348 deviations were lower than 5%.

349

350 **Fig. 3** Reuse assay of lyophilized mycelium of *C. cladosporioides* in repeated-batch reactions.
351 After each reaction cycle (24 h), the lyophilized mycelium was separated from the reaction
352 medium and washed.

353

354

355

356

357
358
359
360

361
362
363

364
365
366
367
368
369
370
371
372
373
374
375
376
377
378
379
380
381
382
383
384
385
386
387
388
389

Table 1 Maximum FOS production and fructofuranosidase activity. FOS production after 96 h of biotransformation with different amounts of *Cladosporium cladosporioides* lyophilized mycelium in seawater (pH 7.5), with an initial sucrose concentration of 600 g/L.

Amount of mycelium (g/L)	Activity (U/g)	Maximum FOS production (g/L)
10	6.9	108
20	7.9	164
30	8.9	188
40	8.8	208
50	7.4	194

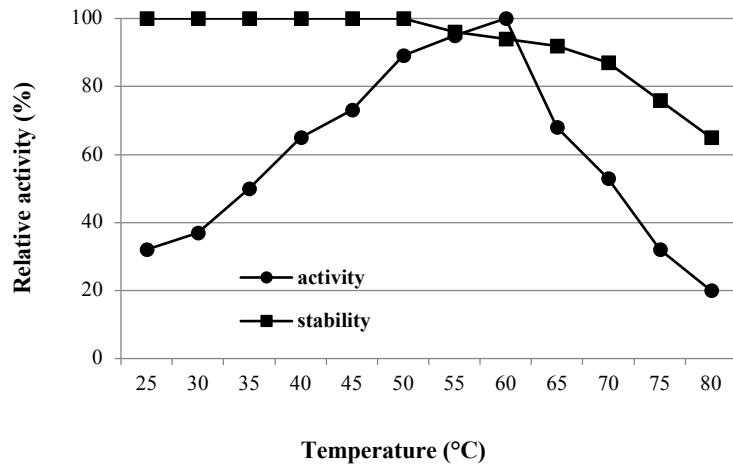
390
391
392
393
394

395 **Table 2** Time-course of total FOS production and T/H index. $T/H = ([\text{glucose}] -$
396 $[\text{fructose}])/[\text{fructose}]$

Time (h)	Total FOS production (g/L)	T/H index
24	176	5.0
48	291	4.8
72	344	4.7
96	340	4.1
120	309	3.4
144	292	2.7

397
398
399

400



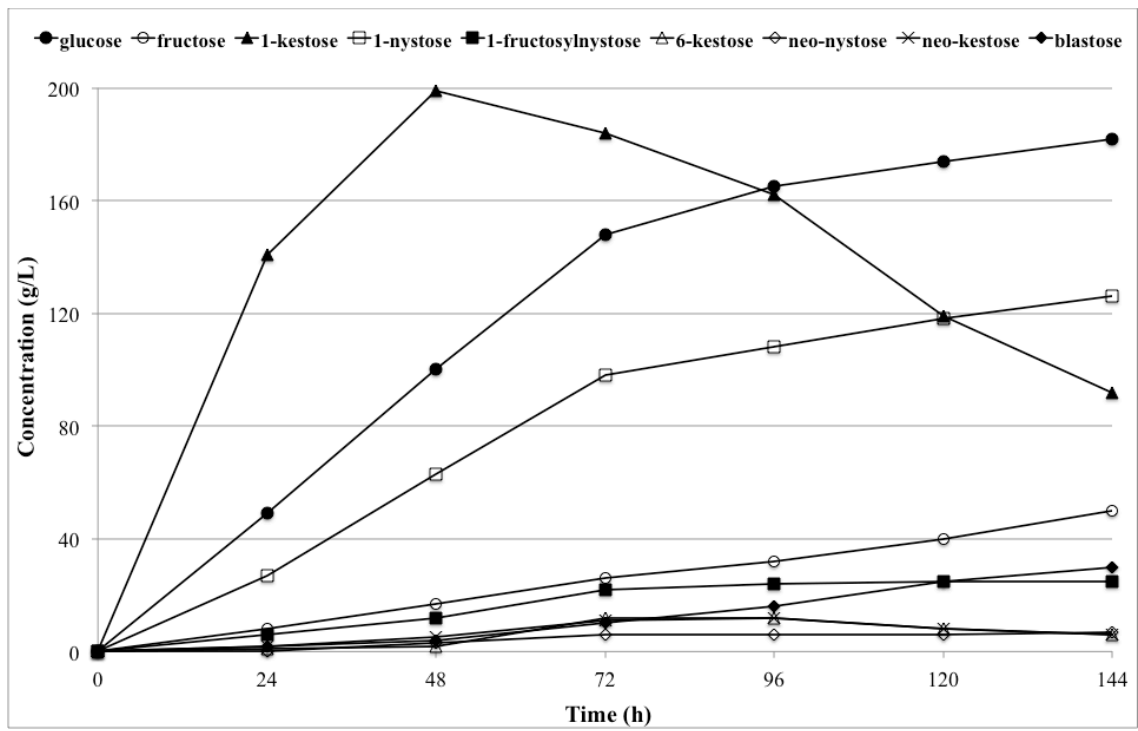
401

402

403 **Figure 1.**

404

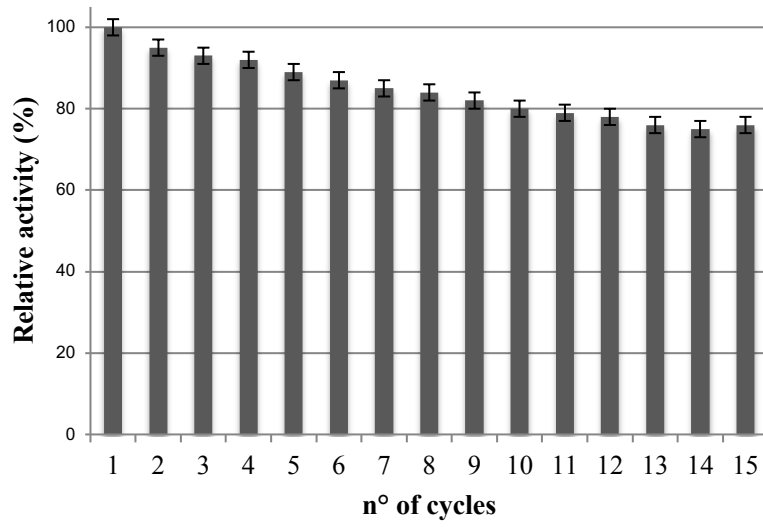
405
406



407
408 **Figure 2.**

409

410



411

412 **Figure 3**