1	Silicate dissolution boosts the CO ₂ concentrations in subduction fluids
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22	
23	Summary
24	Current estimates of dissolved CO ₂ in subduction-zone fluids based on thermodynamic models rely
25	on a very sparse experimental data base. Here we show that experimental graphite-saturated COH
26	fluids interacting with silicates at 1–3 GPa and 800°C display unpredictably high CO ₂ contents.
27	
28	Abstract
29	Estimates of dissolved CO ₂ in subduction-zone fluids are based on thermodynamic models, relying
30	on a very sparse experimental data base. Here we present experimental data at 1-3 GPa, 800°C and
31	$\Delta FMQ \approx$ -0.5 for the volatiles and solute contents of graphite-saturated fluids in the systems COH,
32	SiO ₂ -COH (+ quartz/coesite) and MgO-SiO ₂ -COH (+ forsterite and enstatite). The CO ₂ content of

- 33 fluids interacting with silicates exceeds the amounts measured in the pure COH system by up to 30
- 34 mol%, as a consequence of a decrease in water activity probably associated with the formation of

organic complexes containing Si–O–C and Si–O–Mg bonds. The interaction of deep aqueous fluids with silicates is a novel mechanism for controlling the composition of subduction COH fluids, promoting the deep CO₂ transfer from the slab–mantle interface to the overlying mantle wedge, in particular where fluids are stable over melts.

39

40 Introduction

41 Subduction of the oceanic lithosphere and its sedimentary cover is accompanied by devolatilization processes¹. CO₂ removal through dissolution of carbonates occurring in altered 42 oceanic lithosphere and its sedimentary cover, along with diapirism of slab rocks^{2,3} and/or melts⁴, 43 provides an efficient way to recycle carbon back to the mantle wedge and, ultimately, to the Earth's 44 surface^{5,6}. However, other forms of carbon, often closely associated with silicates, have been 45 reported in slab rocks and in particular in subduction mélanges. For instance, graphite has been 46 described in blueschist-facies mafic rocks, metasediments and hybridized peridotites at Santa 47 Catalina⁷, and in ophiolitic serpentinites from the Western Alps⁸, where also diamond has been 48 found in UHP metasediments⁹. In Alpine Corsica¹⁰ and in the Western Italian Alps¹¹, reduction of 49 50 carbonates during subduction results in graphite-rich metasediments and serpentinites, suggesting 51 that graphite may become a major phase in hybridized silicate-rich subduction mélanges. Graphite 52 has been considered to represent a refractory sink of carbon in the subducting slab, owing to its lower solubility in aqueous fluids¹² and melts¹³ compared to carbonates. On the other hand, graphite 53 dissolution mechanisms and solute transport in complex COH fluids at high pressures have 54 55 remained experimentally unconstrained. Moreover, recent thermodynamic models highlight the role of graphite in subduction-zone fluids¹⁴ and suggest that the presence of graphite is capable of 56 modifying fluid properties and promoting the formation of C-bearing anions, possibly enhancing 57 58 the complexation of major and trace elements at elevated P and T conditions¹².

59 Here we provide comprehensive experimental constraints on the composition of high-60 pressure graphite-saturated COH fluids in terms of dissolved CO₂, SiO₂ and MgO in increasingly complex petrological systems at controlled redox conditions, buffered by using the double-capsule 61 62 technique and both the nickel-nickel oxide (NNO) and the fayalite-magnetite-quartz (FMQ) buffers, 63 in order to develop a model for the interaction between deep aqueous fluids and silicates in subduction mélanges. A carbonate-free compositional range has been explored at P = 1 GPa, T =64 800°C and P = 3 GPa, T = 800°C in order to focus on the role of graphite and silicates in the 65 66 investigated processes. We synthesized COH fluids in equilibrium with graphite and other minerals representative of subduction mélanges, i.e. Mg-silicates (forsterite and enstatite), representative of 67 68 the mantle component, and quartz, representative of the sedimentary component. Experimental

69 products were analyzed for their volatile COH composition by quadrupole mass spectrometry 70 (QMS) and for their Mg and Si solute load by cryogenic laser ablation inductively coupled plasma mass spectrometry (ICP-MS). Measured data were compared to thermodynamic modeling results. 71 72 Further details are provided in Methods and as Supplementary Information. Our results suggest that 73 the interaction of deep aqueous fluids with silicates in the presence of graphite in a subduction 74 mélange promotes the dissolution of graphite and enhances the CO₂ contents of the fluids; this 75 provides a new mechanism for controlling the volatile composition of COH fluids already at depths 76 of ~30 km.

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78 **Results and discussion**

79 CO₂ contents of fluids in equilibrium with silicates

80 The volatile compositions of COH fluids were measured by piercing the capsules after quench in a gas-tight vessel and then conveying the emanating gases to a quadrupole mass 81 spectrometer (QMS)¹⁵. Measured data were subsequently compared with the compositions 82 83 predicted by traditional thermodynamic modeling using different equations of state and mixing 84 properties of H₂O and non-polar species (details in Methods). Carbon-saturated fluids were 85 synthesized first in the pure COH system, where fluids interacted only with graphite (supplementary fig. 1 a). As predicted by thermodynamic modeling, all analyzed fluids are located 86 87 on the graphite-saturation surfaces (black lines in Fig. 1). The measured $XCO_2 = CO_2 / (H_2O + CO_2)$ $(CO_2)_{molar}$ (supplementary table 1) and modeled compositions (supplementary table 2) of the COH 88 89 fluids coexisting only with graphite overlap in both experiments buffered with NNO and FMQ (Fig. 90 1 and supplementary fig. 2). However, experiments where COH fluids coexist with either 91 quartz/coesite (SiO₂-COH system; supplementary fig. 1 c) or forsterite + enstatite in addition to 92 graphite (MgO–SiO₂–COH system; supplementary fig. 1 b) clearly display a significant increase of 93 XCO₂ (Fig. 1; supplementary table 1). The increase in XCO₂ is + 33 % (MgO–SiO₂–COH) and + 28 % (SiO₂-COH) in experiments buffered by FMQ at 1 GPa, 800°C, + 9 % (SiO₂-COH) in 94 95 experiments buffered by FMQ at 3 GPa, 800°C, and + 14 % (SiO₂-COH) and + 15 % (MgO-SiO₂-96 COH) in experiments buffered by NNO at 1 GPa, 800°C.

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98 Si and Mg contents of fluids in equilibrium with silicates

99 The interpretation of the observed differences in volatile content of COH fluids that do and 100 do not interact with silicates is not straightforward. Because we did not find any evidence of 101 hydration and/or carbonation reactions in the run products, our preferred interpretation is that 102 dissolution reactions of silicates are influencing the XCO_2 of the fluid, provided that graphite is

103 present in excess. We therefore measured additionally the dissolved Si and Mg in the synthetic 104 COH fluids at 1 GPa and 800°C by using a modified version of the cryogenic LA-ICP-MS technique¹⁶. This technique was originally developed for the analysis of solutes in pure water, 105 106 which is frozen in the experimental capsules and analyzed via laser-ablation ICP-MS. In the case of 107 COH fluids, an immiscible mixture of water and non-polar gases is expected at the investigated P, T 108 conditions¹⁷ (inset in supplementary fig. 2 e). The cryogenic technique, operating at $\sim -35^{\circ}$ C, only keeps water in a solid state. Therefore, the other volatiles (including CO₂) are lost when the capsule 109 110 is opened for analysis. Consequently, the solute contents retrieved by ICP-MS pertain to the aqueous part of the bulk COH fluid only (supplementary table 3; other details in Methods). In figure 111 112 2 we report the solubility data of quartz (SiO₂-COH system) and forsterite + enstatite (MgO-SiO₂-COH system) at 1 GPa and 800°C, where SiO₂ molalities have been obtained by correcting the 113 114 concentration of the internal standard (Cs) on the basis of the measured fluid XCO_2 (supplementary fig. 3; supplementary table 3). The measured dissolved Si in COH fluids in equilibrium with quartz 115 and graphite at 1 GPa, 800°C and fH_2^{NNO} conditions (XCO₂ = 0.83; supplementary table 1; 116 supplementary fig. 1 d) is 0.30 ± 0.04 mol kgH₂O⁻¹, which is much lower than the quartz solubility 117 in pure water (1.23 mol kgH₂ $O^{-1 \text{ Ref. 18}}$), but much higher than previously reported quartz solubilities 118 in H₂O–CO₂ fluids characterized by similar XCO₂ but without graphite (0.04 mol kgH₂O^{-1 Ref.19} for 119 $XCO_2 = 0.75$; 0.01 mol kgH₂O⁻¹ for $XCO_2 = 0.94$ ^{Ref.20}). The dissolved silica in COH fluids in 120 equilibrium with forsterite, enstatite and graphite ($XCO_2 = 0.84$; supplementary table 1; 121 supplementary fig. 1 e) is much higher compared to the SiO₂-COH system (1.24 mol kgH₂O⁻¹), 122 123 resembling the solubility of quartz in pure water. The solubility of forsterite and enstatite has not previously been measured in mixed H₂O–CO₂ fluids, but it has been investigated in pure water^{21–24}, 124 amounting to 0.21-0.30 mol SiO₂ kgH₂O^{-1 Ref.24}. We additionally performed a dissolution 125 experiment of forsterite and enstatite in pure water (MgO-SiO₂-H₂O system; black dot in Fig. 2), 126 obtaining very similar results ($0.22 \pm 0.06 \text{ mol SiO}_2 \text{ kgH}_2\text{O}^{-1}$), clearly testifying that the solubility 127 128 of forsterite and enstatite in pure water is much lower than in COH-bearing fluids.

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130 Constraints on the increased solubility of silicates

Our solubility results indicate that in both the graphite-saturated SiO_2 -COH and MgO-SiO_2-COH systems, the carbon dissolved in fluids does not behave merely as an inert diluent, but promotes the dissolution of silicates at the conditions of our experiments. The simplest explanation of these results is that new unexpected organic complexes containing Si-O-C and Si-O-Mg bonds are formed in addition to the solutes known experimentally, such as the Mg²⁺ ion and the silica monomer and dimer^{24,25}. This hypothesis is supported by the measured dissolved Mg concentrations in the MgO–SiO₂–H₂O and MgO–SiO₂–COH systems. Although published experimental data are not available to date for the *P*–*T* conditions investigated, the extrapolated solubility of Mg derived from the dissolution of forsterite and enstatite in pure water should be less than 0.17 mol kgH₂O⁻¹ at P = 1-2 GPa and $T = 900-1200^{\circ}C^{23}$. In our experiments in pure water at 1 GPa and 800°C, dissolved Mg is slightly higher (0.28 ± 0.04 mol kgH₂O⁻¹; supplementary table 3). However, in COH fluids at identical *P*, *T* conditions the Mg content almost quadruples (1.08 mol kgH₂O⁻¹; supplementary table 3).

144 In order to gain some insight into the possible aqueous species relevant to the different types 145 of experimental systems reported in the present study, we used a thermodynamic model that also 146 takes Mg- and Si-bearing dissolved species into account, in addition to neutral COH species, and therefore is suitable for the systems SiO₂-COH and MgO-SiO₂-COH. We first performed 147 preliminary calculations using the aqueous speciation-solubility code EQ3²⁶ adapted to include 148 equilibrium constants calculated with the Deep Earth Water model^{27,28} at 1 GPa and 800°C (other 149 150 details in Methods). For the system MgO-SiO₂-H₂O, the predicted silica concentrations agreed with the experimentally measured values. However, the predicted Mg concentrations in the MgO-151 152 SiO₂-H₂O system were too low, even when a predicted equilibrium constant for the species Mg(OH)⁺ was included. Consequently, an Mg(OH)_{2(aq)} complex was fit to the experimental 153 154 solubility data for the MgO–SiO₂–H₂O system (supplementary table 4).

155 In the system MgO–SiO₂–COH, the new Mg(OH)_{2(aq)} complex and the predicted complexes $MgHCO_3^+$, $MgCO_{3(aq)}$, $MgHSiO_3^+$, and $MgSiO_3(aq)$ were used together with the silica monomer and 156 157 dimer in trial calculations to predict Mg and Si solubilities. However, numerous calculations 158 resulted in solubilities that were too low, indicating the likely need for an additional complex 159 involving the components MgO, CO₂, and SiO₂ in the MgO–SiO₂–COH system compared to the 160 carbon-free MgO-SiO₂-H₂O system. An analysis of the available solubility data at 800°C and 1.0 161 GPa for the MgO-SiO₂-H₂O and the MgO-SiO₂-COH systems indicates that a variety of MgO-162 SiO₂–CO₂ complexes might be feasible. For example, complexes involving oxidized C-species such as bicarbonate or carbonate complexes, or complexes involving reduced C-species could account 163 164 for the observed solubilities. In supplementary table 4, we present the results for a complex of Mg 165 with the silicate anion and the organic anion propionate (MgSiC complex) which can be written as Mg[OSi(OH₃)][CH₃CH₂COO]. This complex provides an explanation for the distinctive enhanced 166 167 solubilities of Mg and Si measured in the present study. In particular, the MgSiC complex is 168 predicted to be important in the relatively reduced systems investigated, i.e. bearing H_2O-CO_2 fluids in equilibrium with graphite close to the C–CO₂ (CCO) buffer²⁹. This complex, however, 169 would be insignificant in the COH fluids in all previous studies of silicate solubilities that focused 170

171 on unbuffered H₂O–CO₂ fluids without graphite (i.e., above the CCO buffer), which are potentially 172 stable up to extremely oxidizing conditions. Analogous calculations for the SiO₂-COH system suggest the possibility of other organic complexes involving SiO₂ and reduced C-species. It is worth 173 174 noting here that the stability of organic COH species in subduction-zone fluids has been recently suggested¹⁴. A more complete analysis of the potential importance of MgO–SiO₂–CO₂ complexes 175 176 over a wide range of temperatures and pressures is hampered by the lack of other experimental Mg-177 and Si-solubility data in the MgO-SiO₂-COH and SiO₂-COH systems. Consequently, a full equation of state characterization of the standard partial molal properties of MgO-SiO₂-CO₂ 178 179 complexes must await the development of estimation schemes for refining the properties of such 180 complexes.

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182 Constraints on the increase of CO₂

183 Analytical results indicate that in both the SiO₂-COH and MgO-SiO₂-COH systems 184 externally buffered by FMQ and NNO, dissolution reactions of either quartz/coesite and forsterite + enstatite are able to boost the CO₂ content of graphite-saturated COH fluids at elevated pressures 185 186 and temperatures. No significant differences have been observed concerning the XCO₂ increase 187 between quartz-bearing and forsterite + enstatite-bearing experiments, suggesting that dissolved Si, rather than Mg, is the major player in this boosting process. This could be attributed to the 188 polymerized nature of silica at high pressures and temperatures²⁰, which may be different from 189 other species, for example aluminum species³⁰. Our model predicts that neutral silica monomers 190 191 $[SiO_2(aq)]$ and dimers $[Si_2O_4)(aq)]$ are important species at the investigated conditions (supplementary table 4), which is supported also by experimental data from forsterite and enstatite 192 incongruent dissolution in pure H₂O at 1 GPa and 700°C²⁴. However, none of the models we 193 developed was able to account for the large increase in the CO₂ solubility in the fluid that was 194 195 experimentally determined in SiO₂-COH or MgO-SiO₂-COH systems. Several possible 196 explanations for this novel effect can be suggested. For instance, very large amounts of HCO₃⁻ or CO_3^{2-} species that would occur in the SiO₂-bearing fluids could be converted to CO₂ through 197 198 reactions of the type:

199
$$\operatorname{CO_3^{2-}} + 2\operatorname{H}^+ \rightleftharpoons \operatorname{CO_2} + \operatorname{H_2O}$$

(Eq. 1)

However, theoretical model results indicate that at 1.0 GPa and 800°C insignificant amounts of HCO₃⁻ or CO₃²⁻ are present in the fluids. Actually, the association forsterite + enstatite at 0.5 GPa and 600°C buffers the pH of the coexisting aqueous fluid to between 2.5 and 4 $^{\text{Ref.14}}$. Our model predicts that at 1 GPa and 800°C the pH of the fluid is 5.57 in the MgO–SiO₂–H₂O system and 3.73 in the MgO–SiO₂–COH system (supplementary table 4). These pH values would favor the stability of the species $CO_{2(aq)}$ against HCO_3^- and $CO_3^{2^-}$. Moreover, reaction (Eq. 1) is independent on the presence of silica, thus it cannot explain the influence exerted by silicate dissolution in enhancing the *X*CO₂ of the fluid.

208 Alternatively, a change in fCO_2 at fixed fH_2 imposed by the buffers could result from a change in fH₂O or fO₂ associated with dissolved silica. In our double-capsule experiments, silicate dissolution 209 210 reactions in both the MgO-SiO₂-COH and SiO₂-COH systems proceed together with the 211 dissolution of graphite. In the pure COH system, the dissolution of graphite at the investigated 212 relatively oxidizing conditions is controlled by the reaction $C + 2H_2 + 2O_2 \rightleftharpoons CO_2 + 2H_2O$ (see Eq. 12 in Methods; supplementary fig. 4) until the fugacity of H₂ in the inner capsule, containing a 213 214 COH fluid, equals that in the outer capsule, containing C-free water in equilibrium with the NNO or 215 the FMQ buffers. The equilibrium constant of the reaction above is:

216
$$K = \frac{f \text{CO}_2 \times (f \text{H}_2 \text{O})^2}{(f \text{H}_2)^2 \times (f \text{O}_2)^2}$$
 (Eq. 2)

Our experimental data (runs COH70 and COH69 in supplementary table 1) and the thermodynamic model of Zhang & Duan (ZD09mod in supplementary table 2; details in Methods) allow retrieving *K* in the pure COH system at 1 GPa and 800°C resulting both in the NNO- and the FMQ-buffered experiments a value of log K = 37.5, assuming log $fH_2^{NNO} = 1.775$ and log $fH_2^{FMQ} = 1.889$, and log $fO_2 = -14.28$ (inner capsule buffered by NNO) and log $fO_2 = -14.31$ (inner capsule buffered by FMQ), respectively.

The observed increase in fluid XCO_2 in SiO₂–COH and MgO–SiO₂–COH systems will result in an increase of fCO_2 . Therefore, it is convenient to express Eq. 2 as a function of fCO_2 :

225
$$f \text{CO}_2 = \frac{K \times (f \text{H}_2)^2 \times (f \text{O}_2)^2}{(f \text{H}_2 \text{O})^2}$$
 (Eq. 3)

- 226 and
- 227 $\log f \operatorname{CO}_2 = \log K + 2 \log f \operatorname{H}_2 + 2 \log f \operatorname{O}_2 2 \log f \operatorname{H}_2 O$ (Eq. 4)

228 By fixing log fH_2 and log K, fCO_2 is expressed as a function of the two variables fO_2 and fH_2O_2 , which can be represented as two tri-dimensional surfaces, one calculated for $\log f H_2^{NNO}$ (Fig. 3 a) 229 and one calculated for $\log fH_2^{FMQ}$ (Fig. 3 b). In order to move from the fCO_2 of the pure COH 230 231 system (green dots in Fig. 3) to the fCO_2 retrieved from measurement in the SiO₂–COH (pink dots) 232 and MgO–SiO₂–COH (ochre dots), either $\log fH_2O$ (i.e. H_2O activity) should decrease at constant 233 log fO₂ (arrays A in Fig. 3) or log fO₂ should increase at constant log fH₂O (arrays B in Fig. 3). This model predicts that very small variations in either log fH_2O or fO_2 (~ 0.03 log units at fH_2^{NNO} ; ~ 234 0.06 log units at fH_2^{FMQ}) can account for the measured increase in fCO_2 in both SiO₂-COH and 235 236 MgO-SiO₂-COH systems (supplementary table 5). However, in view of the absence of redox sensitive components in the minerals under investigation, even small variations of fO_2 are highly 237

238 unlikely in our experimental system and therefore we suggest that a decrease in fH_2O is the culprit 239 of the observed increase in fCO₂ in the MgO-SiO₂-COH and SiO₂-COH systems. By using the H₂O fugacity coefficient from Zhang & Duan³¹ (1.579 at 1 GPa and 800°C), we are able to 240 calculate the decrease in water activity (aH_2O), assuming that $aH_2O = fH_2O/fH_2O^0$, where fH_2O^0 is 241 the fugacity of pure water at 1 GPa and 800°C (i.e., 15785.5). The required decrease in *a*H₂O with 242 243 respect to the pure COH system is -4.17 log units in the experiments buffered with NNO and -4.14 244 log units in the experiments buffered with FMQ. Because only small differences in measured XCO₂ 245 have been observed between the SiO₂-COH and MgO-SiO₂-COH systems, we argue that dissolved silica monomers [Si(OH)₄] and dimers [Si₂O(OH)₆] are much more effective than MgO–SiO₂–CO₂ 246 247 complexes in decreasing water activity. The activity of total silica can be calculated on the basis of the measured SiO_2 molality in the experiments buffered with NNO and the measured XCO_2 of the 248 corresponding COH fluid²⁰, log (aSiO₂) being equal to -2.59 in MgO–SiO₂–COH and -2.90 in the 249 SiO₂-COH systems. The activity of dissolved silica in the SiO₂-COH and MgO-SiO₂-COH 250 251 systems is therefore much higher (about 20 times in SiO₂-COH system; 40 times in MgO-SiO₂-252 COH system) compared to the difference in aH₂O estimated in the SiO₂-COH and MgO-SiO₂-253 COH systems versus the pure COH system. In order to match the observed increase in fCO_2 we 254 estimated that only 0.31 mol% (SiO₂-COH system; i.e., 0.006 mSiO₂/kgH₂O) and 1.89 mol% 255 (MgO-SiO₂-COH system; i.e., 0.004 mSiO₂/kgH₂O) of the measured dissolved silica are required, 256 assuming that the decrease in water activity is solely related to the formation of hydrated silica 257 monomers $[Si(OH)_4]$ and dimers $[Si_2O(OH)_6]$. These low solubility data (cf. also supplementary 258 table 4) are almost identical to quartz solubility in graphite-free systems bearing very high-XCO₂ H₂O-CO₂ fluids²⁰, strongly supporting the hypothesis that additional new SiO₂-CO₂ and MgO-259 SiO₂-CO₂ complexes are required to account for the surprisingly high total dissolved silica 260 261 measured in our experiments.

262

263 Dissolution of graphite and silicates in subduction mélanges

264 Our results suggest that the silica component derived from the dissolution of either 265 magnesium silicates or quartz/coesite alone, even in absence of carbonates, controls the 266 composition of deep COH fluids in equilibrium with graphite, in particular enhancing their CO₂ 267 content when compared to SiO₂-free systems. This mechanism could be effective especially in cold subduction zones, where subsolidus conditions prevail, and particularly in subduction mélanges, 268 where silicate minerals and graphite¹⁰ are thought to be abundant and flushed by aqueous fluids 269 originating from the dehydration of the subducted lithosphere ^{32,33}(Fig. 4). Independently from the 270 271 occurrence of carbonates, the dissolution of silicates can boost the dissolution of graphite in the

272 subduction mélange in the form of volatile CO_2 dissolved in COH fluids by up to + 30 % compared 273 to silicate-free systems. These CO₂-rich fluids will interact with the overlying mantle rocks, 274 influencing metasomatic processes, carbonation/decarbonation reactions, and the melting temperatures of rocks in the mantle wedge³. From this perspective, the fact that fluid inclusions in 275 shallow-mantle xenoliths are often dominated by CO₂ over water³⁴ could be an effect of the 276 277 inherited CO₂-rich composition of slab-derived fluids, and does not necessarily require extensive 278 diffusional hydrogen loss from the inclusion to the host mineral. Moreover, as this CO₂ boosting effect cannot be predicted by available thermodynamic models that have been used to estimate the 279 amount of CO₂ recycled from subducted carbon-bearing sediments⁵, the estimated carbon transfer 280 linked to the oxidation of sedimentary organic carbon and graphite (~ 6 Mt C/y^5) probably needs to 281 282 be adjusted up by 10–30% (0.6–1.8 Mt C/y). Additional experiments investigating more complex, carbonate-bearing systems as well as an improved quantification of the content of graphite and 283 284 organic matter in subducted sediments are required to better quantify the impact of this novel 285 mechanism on the global carbon flux.

286

287 Methods

288 Investigating the fluid composition in COH-bearing systems

Several experimental studies investigated separately the effect of the volatiles H_2O^{36-39} and CO_2 ⁴⁰⁻ 289 ⁴³ on subsolidus and melting relations in peridotitic systems at upper-mantle conditions. Only few 290 studies considered the effect of the simultaneous occurrence of H₂O and CO₂ or more generally, the 291 influence of COH fluids on the peridotitic systems^{3,44,45}. The H₂O/CO₂ ratio in COH fluids is 292 293 crucial because it affects the location of carbonation/decarbonation reactions and the position of the 294 solidus. However, the H₂O/CO₂ ratio of the fluid in equilibrium with mantle minerals has mainly been estimated through thermodynamic modeling³, using equations of state of simple H₂O-non-295 polar gas systems^{46,47} (e.g., H₂O–CO₂–CH₄), equations that do not consider the complexity related 296 297 to dissolution processes⁴⁸.

Another fundamental property of H₂O-bearing fluids at high-pressure conditions is the capacity to transport dissolved species¹⁸. The amount of solutes from rock-forming minerals in aqueous fluids increase with increasing pressure^{23,49–51} until the fluid becomes no longer distinguishable from a silicate melt and a supercritical liquid is formed^{52,53} The solubility of forsterite and enstatite has been measured in pure water up to 1.5 GPa and at $T = 700-1300^{\circ}C^{24}$. Experimental data on mineral dissolution in mixed H₂O–CO₂ fluid are available only for quartz^{19,20,54}, albite⁵⁵ and diopside⁵⁶ and suggests that solubility decreases with increasing content of CO₂ in the fluid.

The aim of the paper is to provide for the first time experimental constraints on the composition of 305 306 high-pressure COH fluids in equilibrium with graphite in terms of both volatile content and 307 dissolved solutes in increasingly complex petrological systems at controlled fO_2 conditions. Fluids 308 have been investigated in equilibrium with graphite only in the system COH, with graphite + 309 quartz/coesite in the system SiO₂-COH and with graphite + forsterite + enstatite in the system 310 MgO-SiO₂-COH. Two different experimental setups and analytical techniques were employed to 311 determine the volatile composition and the solubility of minerals in COH fluids at P = 1.0 and 3.0 312 GPa, and $T = 800^{\circ}$ C. These conditions were selected for sake of simplicity to avoid the presence of carbonates (magnesite) in the system MgO-SiO₂-COH and the consequent complexities related to 313 314 carbonate dissolution. In particular, the link between H₂O/CO₂ ratio (derived analytically by means of a quadrupole mass spectrometer [QMS]¹⁵) and silicate dissolution (investigated by cryogenic 315 laser-ablation inductively coupled plasma mass spectrometry [LA-ICP-MS]³⁵) is highlighted here 316 317 and compared with thermodynamic calculations.

318

319 Bulk compositions and starting materials

320 COH fluids were generated starting either from oxalic acid dihydrate (OAD; $H_2C_2O_4 \cdot 2H_2O$) or an 321 equivalent mixture of 1:1 oxalic acid anhydrous (OAA; $H_2C_2O_4$) + water (supplementary fig. 1). 322 OAD was employed in the experimental runs aimed at investigating the COH volatile composition 323 by means of the capsule-piercing QMS technique¹⁵ (QMS experiments; supplementary figs 1 a–c). 324 The dissociation of oxalic acid at high temperature is given by the reaction:

(Eq. 5)

325
$$H_2C_2O_4 \cdot 2H_2O \rightleftharpoons 2H_2O + 2CO_2 + H_2$$

326 generating a starting fluid characterized by XH_2O (= H_2O/CO_2+H_2O) = 0.5 and an excess of H_2 .

Instead of OAD, OAA + Cs-doped (590 μ g g⁻¹) water was employed as fluid source in experiments on mineral solubility in COH fluids (LA-ICP-MS experiments; supplementary figs. 1 d–e), to ensure the presence of an internal standard (Cs) for LA-ICP-MS data quantification³⁵ The thermal dissociation of OAA at high temperature conditions generates a CO₂–H₂ fluid according to the reaction:

332
$$H_2C_2O_4 \rightleftharpoons 2 CO_2 + H_2$$
 (Eq. 6)

- The addition of a proper amount of Cs-doped water in the capsule allowed to obtain a starting fluid composition with $XH_2O = 0.5$ for the LA-ICP-MS experiments too.
- Graphite (ceramic-grade powder, checked for purity and crystallinity by X-ray powder diffraction and scanning electron microscopy) was added in all experiments to ensure carbon saturation of the COH fluid. In SiO₂–COH and MgO–SiO₂–COH experiments, natural quartz powder (supplementary fig. 1 c) and a mixture of synthetic forsterite and enstatite (supplementary fig. 1 b)

339 were added respectively, with fluid/solid ratios of about 0.2 by weight. Forsterite and enstatite were 340 synthesized from dried nano-crystalline Mg(OH)₂ (Sigma-Aldrich, 99.9% purity) and silicon 341 dioxide (Balzers, 99.9% purity), mixed in stoichiometric proportions, pelletized and loaded in a 342 vertical furnace at 1500°C for 24 h. Synthesis products were ground in ethanol for 1 hour, dried and 343 characterized by X-ray powder diffraction analysis (Bruker, AXS D8 Advance, ETH Zurich; 344 Philips X'pert MPD, University of Milan). The resulting composition of the mixture, derived by 345 Rietveld analysis, is forsterite 83.2 wt%, enstatite 16.7 wt% and cristobalite 0.1 wt%. Run products 346 were characterized using scanning electron microscopy and electron microprobe WDS analyses 347 (Jeol JXA 8200). Silica polymorphs (quartz/coesite) were identified by X-ray diffraction analysis.

- In LA-ICP-MS experiments, a layer of diamond powder (grain size 20 μm) serves as a trap for
 collecting the COH fluids in equilibrium with solids (supplementary fig. 1 d).
- 350

351 Experimental conditions and apparatus

352 Capsules were welded shut in a frozen steel holder to avoid overheating. Capsules were reweighed 353 to ensure no fluid loss during welding occurred. Sintered MgO rods were employed to embed the 354 capsule, surrounded by a graphite heater, Pyrex glass and NaCl. A rocking piston-cylinder 355 apparatus was used to reach high-pressure and high-temperature conditions. The rocking piston-356 cylinder is a regular end-loaded piston-cylinder, which allows forward and backward rotation of 357 180° during the experimental run, thus inverting its position in the gravity field. Chemical inhomogeneity within the capsule is in fact common in fluid saturated experiments. The rocking 358 piston-cylinder overcomes this problem⁵⁷ as the rotation of the sample induces Rayleigh-Taylor 359 instabilities, forcing the fluid to migrate and causing chemical re-homogenization. Pressure 360 calibration of the rocking apparatus is based on the quartz to coesite transitions⁵⁸ at P = 3.07 GPa 361 and $T = 1000^{\circ}$ C, and P = 2.93 at $T = 800^{\circ}$ C (accuracy ± 0.01 GPa and $\pm 5^{\circ}$ C). Temperature was 362 363 measured with a K-type thermocouple located within 0.6 mm from the top of the capsule and is 364 considered accurate to $\pm 5^{\circ}$ C.

365

366 Buffering strategy and thermodynamic modeling

Because the volatile composition of graphite-saturated COH fluids is dependent on the redox state
of the system, all experiments were performed using a conventional double-capsule design to
constrain the chemical potentials (supplementary fig. 1).

- 370 The outer Au capsule (OD = 5 mm in QMS experiments; OD = 3 mm in LA-ICP-MS experiments
- 371 contains a buffering mixture of either Ni + NiO + H₂O (NNO) or fayalite + magnetite + quartz +

372 H₂O (FMQ; ferrosilite + magnetite + coesite at 3 GPa, 800°C). As long as all phases are present in 373 the buffering mixtures, they fix the fugacity of H₂ (fH_2^{NNO} , fH_2^{FMQ}) through the reactions:

(Eq. 8)

- 374 $Ni + H_2O \Rightarrow NiO + H_2$ (Eq. 7)
- 375 3 $Fe_2SiO_4 + 2 H_2O \rightleftharpoons 2 Fe_3O_4 + 3 SiO_2 + 2 H_2$

376 The inner $Au_{60}Pd_{40}$ capsule (OD = 2.3 mm), which contains the COH fluids in equilibrium with 377 graphite \pm quartz/coesite \pm forsterite+enstatite, is permeable to hydrogen. Therefore, the fugacity 378 (and, thus, the chemical potential) of H₂ is expected to be homogeneous and identical in the inner 379 and in the outer capsules. Indirectly, also all the other species composing the COH fluid will be 380 externally buffered, including oxygen. However, since the inner capsule contains a mixed COH 381 fluid instead of pure water, the oxygen fugacity in the inner capsule will be lower compared to that fixed in the outer capsule. The fugacities of oxygen and hydrogen fixed in the outer capsule by both 382 NNO and FMQ were calculated employing Perple X⁵⁹ (http://www.perplex.ethz.ch) using the 383 thermodynamic dataset of Holland and Powell⁶⁰ revised by the authors in 2004 and the Perple X 384 385 EoS n. 16 (H–O HSMRK/MRK hybrid EoS) (supplementary table 2). Subsequently, we calculated 386 the speciation of the graphite-buffered COH fluid in the inner capsule for fH_2 fixed by both NNO and FMQ through thermodynamic modeling using i) the software package Perple X⁵⁹ (based on 387 Gibbs free energy minimization) and the EoS of Connolly and Cesare (1993)⁴⁶ (Perple X EoS n. 388 11) (CC93 in supplementary table 2); ii) the Excel spreadsheet GFluid³¹ (based on gaseous 389 equilibrium constants K_p) with the EoS of Zhang and Duan (2009)⁴⁷ and the static H₂ fugacity 390 coefficient provided in the spreadsheet (ZD09 in supplementary table 2); iii) the Excel spreadsheet 391 GFluid³¹ (based on gaseous equilibrium constants K_p) with the EoS of Zhang and Duan (2009)⁴⁷, 392 with a modified H₂ fugacity coefficient (γ H₂) changing dynamically as a function of X(O), fitted 393 from the EoS of Connolly and Cesare (1993) $(\gamma H_2 = a \bullet X(O)^3 + b \bullet X(O)^2 + c \bullet X(O) + d$, where: at 1 394 GPa and 800°C, a = -43.919, b = 114.55, c = -105.75 and d = 41.215; at 3 GPa and 800°C, a = -43.919, b = 114.55, c = -105.75 and d = 41.215; at 3 GPa and 800°C, a = -43.919, b = 114.55, c = -105.75 and d = 41.215; at 3 GPa and 800°C, a = -43.919, b = 114.55, c = -105.75 and d = 41.215; at 3 GPa and 800°C, a = -43.919, b = 114.55, c = -105.75 and d = 41.215; at 3 GPa and 800°C, a = -43.919, b = 114.55, c = -105.75 and d = 41.215; at 3 GPa and 800°C, a = -43.919, b = -105.75, c = -105.75, 395 11208, b = 26723, c = -21949 and d = 6979.2) (ZD09mod in supplementary table 2). By assuming 396 that fH_2 of the COH fluid in the inner capsule is equal to fH_2^{NNO} and fH_2^{FMQ} , we were able to 397 calculate the molar fractions of volatiles (H₂O, CO₂, CO, CH₄, H₂, O₂), the X(O), the fO_2 and the 398 ΔFMQ (= log fO_2 - log fO_2^{FMQ}) of the COH fluid in the inner capsule at the investigated P and T 399 400 conditions (see supplementary table 2 for modeling at 1-3 GPa and 800°C). Depending on the 401 thermodynamic models used, predicted fluids are characterized by the following Δ FMQ values:

- 402 -0.67 (CC93), -0.64 (ZD09) and -0.58 (ZD09mod) at 1 GPa, 800°C, *f*H₂^{NNO};
- 403 -0.73 (CC93), -0.70 (ZD09) and -0.61 (ZD09mod) at 1 GPa, 800°C, *f*H₂^{FMQ};
- --0.42 (CC93), -1.17 (ZD09) and -0.47 (ZD09mod) at 3 GPa, 800°C, *f*H₂^{FMQ}.

- 405 Predicted fluids are mainly composed of H_2O and CO_2 , with XCO_2 [= $CO_2/(CO_2 + H_2O)$] generally
- 406 higher compared to the starting equimolar H_2O-CO_2 composition (supplementary table 2). In fact,
- 407 the equilibration of the COH fluid in the inner capsule is accomplished by these coupled reactions:

408
$$H_2O \rightleftharpoons H_2 + \frac{1}{2}O_2$$
 (Eq. 9)

$$409 \qquad C + O_2 \rightleftharpoons CO_2 \tag{Eq. 10}$$

410 which can be condensed to the following graphite-consuming reactions:

411
$$C + 2H_2O \rightleftharpoons CO_2 + 2H_2$$
 (Eq. 11)

412
$$C + 2H_2 + 2O_2 \rightleftharpoons CO_2 + 2H_2O$$
 (Eq. 12)

- In conclusion, the equilibration of the COH fluid at run conditions implies that CO_2 is produced in the inner capsule by oxidation of graphite. As a consequence, the XCO_2 of the COH fluid in the inner capsule increases until equilibrium in fH_2 is reached between the inner and outer capsules (supplementary fig. 4).
- We experimentally verified the fluid composition predicted by thermodynamic modeling, by 417 retrieving analytically the XCO₂ ratio by means of QMS technique¹⁵, summarized in the next 418 section. At both P = 1 GPa, $T = 800^{\circ}$ C and P = 3 GPa, $T = 800^{\circ}$ C measured and calculated ratios 419 420 are concordant within errors with ZD09mod for both NNO- and FMQ-buffered experiments 421 performed in the COH system (supplementary tables 1 and 2; supplementary fig. 2). Therefore, we 422 conclude that this model can reproduces experimental data in the pure COH system. In the SiO₂-423 COH and MgO-SiO₂-COH systems, literature data and the new experimental data discussed in this 424 paper demonstrate that dissolved Mg-and Si-bearing species resulting from dissolution reactions 425 taking place between solid phases and COH fluids occur in addition (Fig. 2; supplementary table 3). By retrieving the XCO_2 in these systems analytically using the capsule-piercing QMS technique¹⁵, 426 427 we have demonstrated that the thermodynamic calculations outlined above, which do not take into 428 account these dissolved species, cannot be applied to predict the fluid composition in complex 429 systems, in particular those bearing silicates.
- 430 The aqueous speciation and solubility calculations in the investigated silicate-bearing systems were carried out using mass balance, charge, balance, and mass action expressions in the code EQ3²⁶. 431 432 The equilibrium constants involving aqueous ions, water, and minerals were calculated using the DEW model²⁷. Aqueous ionic activity coefficients were calculated using the extended Debye-433 434 Hückel equation including the conversion from the mole fraction scale to the molality scale. The activity coefficients of neutral aqueous CO₂ and CH₄ were approximated in the MgO-SiO₂-COH 435 system by a conversion of the standard states in the model for COH fluids of Zhang and Duan³¹ to 436 the hypothetical 1.0 molal standard state. The activity of H₂O was approximated in the MgO-SiO₂-437 COH system by its mole fraction. Additional new equilibria for the species Mg(OH)_{2,aq} and 438

Mg[OSi(OH₃)][CH₃CH₂COO]⁰ (supplementary table 4) were fitted to the experimental solubilities 439 440 in the systems MgO-SiO₂-H₂O and MgO-SiO₂-COH, respectively at 800°C and 1.0 GPa. The calculated molalities of the most abundant Mg- and Si-species are given in supplementary table 4. It 441 can be seen from the model results that both the Mg(OH)_{2,aq} and Mg[OSi(OH₃)][CH₃CH₂COO]⁰ 442 443 species are predicted to contribute significantly to the total solubilities of both Mg and Si in the 444 MgO–SiO₂–COH system. However, because of the low activity of water in the system the amounts 445 of Mg(OH)_{2.aq}, Si(OH)_{4.aq}, and (OH)₃SiOSi(OH)_{3.aq} are much lower than in the carbon-free system. Under more oxidizing conditions, the Mg[OSi(OH₃)][CH₃CH₂COO]⁰ species would become 446 unimportant, and the solubilities of Mg and Si in the MgO-SiO2-COH system could become 447 448 extremely low.

449

450 Analysis of volatiles

451 Here we provide a brief summary of the technique used to measure the volatile composition of the 452 COH fluids in the inner capsule. The full description and the validation of the technique is provided in Tiraboschi et al. (2016)¹⁵. Quenched COH fluids are extracted from the inner capsule and 453 454 conveyed to a quadrupole mass spectrometer (QMS). The capsule-piercing device consists of an 455 extraction vessel (reactor) that is heated by an electric furnace to $T = 80^{\circ}$ C to transform liquid water into water vapor. The reactor, made of Teflon, is composed of a basal part, where the capsule is 456 457 placed, and a top part, where a steel pointer is mounted. The piercing is executed by screwing the 458 basal part on to the top part until the pointer penetrates the capsule. The capsule, partially embedded 459 in epoxy, is mounted on a steel support, designed to oppose the rotation exerted by the steel pointer 460 during the piercing operation. The furnace design includes a pilot hole in the base part that permits 461 screwing the reactor with a hex key while placed in the furnace. Openings on the top of the reactor 462 allow the carrier gas (ultrapure Ar) to flow inside it and to generate vent or vacuum conditions. The 463 presence of O-rings ensures a tight seal. The reactor is connected to a QMS by a heated line (80°C) 464 to avoid condensation of water on the metal tubes. The pressure conditions in the line and in the 465 reactor are monitored through high-resolution sensor gauges (± 1 mbar precision). The temperatures of the line, reactor and furnace are monitored with K-type thermocouples. Line and reactor 466 pressures and temperatures are recorded by a Eurotherm NanodacTM data recorder with PID control. 467 The internal volume of the reactor was calibrated against the distance h between the basal and the 468 469 top part. P-T-V conditions in the reactor at the time of piercing are used to retrieve the total moles, 470 *n*, of gases released from the capsule, following the ideal gas law n = RT/PV.

471 For the calibration of the QMS, standard gas mixtures of known compositions were utilized: (i) 80
472 vol% Ar, 10 vol% CO₂, 10 vol% O₂; (ii) 80 vol% Ar, 10 vol% CH₄, 10 vol% CO; and (iii) 90 vol%

Ar, 10 vol% H₂. Water calibration is performed by loading a known amount of water (typically 1 473 474 μ L) with a micro-syringe inserted through a silicon septum present at the top into the reactor. The calibration allows performing quantitative analyses of H₂O, CO₂, CH₄, CO, H₂ and O₂. 475 476 Uncertainties for major species were typically ~1% for H₂O and CO₂, and ~10% for CO. After 477 piercing has occurred, gases are conveyed to the QMS by opening a valve. For every m/z channel, 478 the QMS counts are measured every 5 seconds for 310 steps, for a total of 1550 seconds of 479 measurement time. The moles of gases were obtained by comparing the areas of the m/z peaks with 480 those of the standards, using a least-squares regression method. Monte Carlo simulations provided 481 the propagation of uncertainties for each species, which corresponds to measurement uncertainty of 482 the sample and can be represented as a probability distribution plot in ternary COH diagrams.

483

484 Analysis of solutes

485 The solute content in the fluid was measured employing the cryogenic LA-ICP-MS technique also known as the "freezing technique"³⁵, which is applied for the first time on double capsules bearing 486 487 COH fluids. The recovered experimental capsule is mounted on a freezing stage, which consists of 488 a stack of two Peltier elements, surrounded by plastic to thermally insulate the elements from the atmosphere⁶¹. The sample holder is placed on a copper block, in direct contact with the Peltier 489 elements and cooled to $T \sim -35^{\circ}$ C. The conventional freezing-technique has been updated using a 490 491 cutter blade mounted on a steel support. This device allows cutting longitudinally double capsules 492 by fastening a screw that pushes the cutter blade via a steel block through the capsule. During this 493 operation, the capsule is enclosed in a copper holder. Once the capsule is cut open, the cutting 494 device is removed from the freezing stage together with the upper part of the capsule holder 495 including the top part of the capsule. The upper half of the capsule is investigated using a binocular 496 microscope, while the lower part remains frozen on the stage during the entire laser-ablation 497 analytical session that follows immediately.

498 Analyses were performed using a 193 nm ArF GeoLas Pro excimer laser system coupled to an 499 ELAN DRCD-e quadrupole mass spectrometer at University of Bern. We analyzed the diamond trap for ${}^{24}Mg$, ${}^{25}Mg$, ${}^{26}Mg$, ${}^{29}Si$, ${}^{62}Ni$, ${}^{133}Cs$, ${}^{195}Pt$, and ${}^{197}Au$, using a 60 μ m beam diameter, ~13 500 501 J/cm laser fluency, and 5 Hz repetition rate. Data were acquired in blocks of up to ~10 individual 502 sample analyses bracketed by three analyses of the standard NIST SRM610, placed in the ablation chamber with the sample. Background was taken for ~50 seconds and the sample signal, on the 503 504 diamond trap or on the solid residue, was collected for ~20 seconds. LA-ICP-MS data reduction employed the SILLS software⁶² and in-house spreadsheets to calculate solute concentrations, 505

506 employing rigorous limit of detection filtering⁶³ for each element and each measurement 507 individually.

508 The cryogenic technique has been originally developed for analyzing the solute content of aqueous 509 fluids. Cesium, introduced in the starting materials, is employed as an internal standard for data 510 quantification, because it is a highly incompatible element that fractionates completely into the 511 aqueous fluid phase at the given residual mineralogy. In our experiments, we introduced a known amount of water solution doped with 590 μ g g⁻¹ Cs [as Cs(OH)₂]. As the initial Cs/H₂O ratio is 512 fixed, once the Cs concentration in the fluid phase coexisting with minerals at run P and T is 513 known, solute concentrations of the fluid can be calculated³⁵. However, compared to experiments 514 bearing aqueous fluids, our double-capsule, COH-bearing experiments are more complex, because 515 516 the initial Cs/H₂O is not fixed, as the water content in the inner capsule is variable, depending on P, T and fH_2-fO_2 conditions (see Eqs. 11 and 12). In fact, in double capsule arrangements H_2 is a 517 mobile component that can be added or removed from the system through diffusion in and out of 518 519 the inner capsule. This implies that the initial Cs concentration cannot be used as an internal 520 standard. This value needs to be corrected taking into account the change in total water mass 521 present in the inner capsule relative to initial amount of loaded water, as a consequence of fluid 522 XCO_2 re-equilibration at the fH_2 - fO_2 conditions imposed by the buffers. If H_2O is consumed during 523 fluid re-equilibration at run conditions, Cs concentration in the residual water increases; if H₂O is 524 produced, Cs concentration decreases (supplementary fig. 3). We estimated the corrected Cs 525 concentration at run P and T using a model, which assumes that fluid equilibration at the hydrogen 526 fugacity conditions imposed by the buffers NNO and FMQ is governed only by H₂ mobility and no 527 hydration or carbonation reactions occur in the capsule charge. As long as these two assumptions 528 are valid, it is possible to estimate the amount of Cs in the inner capsule in the following way 529 considering a classic dilution equation:

530
$$C_i \text{Cs} * V_i \text{H}_2 0 = C_f \text{Cs} * V_f \text{H}_2 0$$
 (Eq. 13)

where C_i Cs is the initial concentration of Cs in the aqueous solution loaded into the capsule (590 µg g⁻¹) and C_j Cs is the final concentration of Cs after fluid equilibration at fH₂ conditions. V_i H₂O and

- 533 V_f H₂O are the initial and final volumes of water.
- 534 The volume of water is proportional to the moles according to:

535
$$VH_2O = nH_2O * V_{mol}H_2O$$
 (Eq. 14)

536 (VH₂O, volume of water; *n*, number of H₂O moles; V_{mol} H₂O, molar volume of water).

537 Considering that at fixed pressure and temperature conditions the molar volume of water is 538 constant, we obtain the following dilution equation:

539
$$C_i \text{Cs} * n_i \text{H}_2 0 = C_f \text{Cs} * n_f \text{H}_2 0$$
 (Eq. 15)

540 The final Cs concentration in the aquesous fluid fraction will be given by:

541
$$C_f C_s = \frac{C_i C_s * n_i H_2 O}{n_f H_2 O}$$
 (Eq. 16)

542 As n_iH_2O is known (the initial amount of water charged into the capsule), this equation can be 543 solved as long as n_fH_2O is constrained, through equation:

544
$$n_f H_2 0 = n_i H_2 0 * \frac{X H_2 O_f}{X H_2 O_i}$$
 (Eq. 17)

where XH_2O_f is the final $H_2O/(CO_2+H_2O)$ ratio measured by QMS analysis, and XH_2O_i is the initial $H_2O/(CO_2+H_2O)$ ratio retrieved on the basis of the amounts of water and OAA charged into the capsule. Solute concentrations in the aqueous fraction of the COH fluid at run *P* and *T* can thus be calculated (Fig. 2; supplementary table 3).

549

550 Data availability

- 551 The authors declare that the data supporting the findings of this study are available within the 552 article.
- 553

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719 End notes

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727 Author contribution

The capsule-piercing apparatus was conceived by S.T. and built by S.R. QMS analyses were performed by S.T, S.R., C.T and F.M. LA-ICP-MS analyses were carried out by T.P., P.U., C.T. and S.T. Thermodynamic modeling was performed by S.T. and D.S. All authors participated in

- extensive discussions and the preparation of the manuscript.
- 732

733 **Conflict of interest**

The authors declare no competing financial interests.

736 Legends

Fig. 1: Measured volatile composition of graphite-saturated fluids interacting with silicates.

C-O-H diagram showing the volatile composition of fluids, measured by quadrupole mass 738 spectrometry, synthesized at P = 1 GPa, $T = 800^{\circ}$ C and fH_2^{NNO} (a) and fH_2^{FMQ} (b) conditions, and P 739 = 3 GPa, $T = 800^{\circ}$ C and fH_2^{FMQ} (c) in equilibrium with graphite only (COH system; green dots), 740 741 graphite + forsterite + enstatite (MgO-SiO₂-COH system; ochre dots) and graphite + quartz (S-742 COH system; pink dots). The graphite-saturation surfaces, i.e. the loci of points representing all possible compositions of graphite-saturated COH fluids (G-COH) at fixed P, T and variable fO_2 743 conditions, calculated by thermodynamic modeling⁴⁶, are shown for comparison (black curves) 744 along with the volatile fluid composition predicted by the EoS of Zhang & Duan (2009)⁴⁷ using the 745 H_2 fugacity coefficient of Connolly & Cesare (1993)⁴⁶ (blue squares; see Supplementary 746 Information for details). Compared to the pure COH system, the XCO_2 [=CO₂/(H₂O+CO₂)] of the 747 748 fluids, shown in the zoom boxes, increases silicate-bearing systems.



Fig. 2: Measured dissolved SiO₂ in graphite-saturated fluids interacting with silicates

Solute contents in experimental fluids at P = 1 GPa, $T = 800^{\circ}$ C and fH_2^{NNO} in equilibrium with

753 graphite + forsterite + enstatite (MgO-SiO₂-COH system; ochre dot), and with graphite + quartz

754 (SiO₂–COH system; pink dot), expressed as moles of SiO₂ per kg of water, measured by cryogenic

755 laser-ablation ICP-MS. Solute content of forsterite + enstatite in pure water (black dot) and selected

756 literature solubility data in the systems SiO₂–H₂O, SiO₂–COH and MgO–SiO₂–H₂O are shown for

757 comparison. The measured dissolved silica is 0.22 mol kgH₂O⁻¹ in the MgO–SiO₂–H₂O system,

758 0.30 mol kgH₂O⁻¹ in the SiO₂–COH system (XCO₂ = 0.83) and 1.24 mol kgH₂O⁻¹ in the MgO–

759 SiO₂-COH system (XCO₂ = 0.84).

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761 762

Fig. 3: Model for increased dissolved CO₂ in graphite-saturated fluids interacting with silicates.

3D plot of the equations $\log fCO_2 = \log K + 2 \log fH_2^{NNO} + 2 \log fO_2 - 2 \log fH_2O$ (a) and $\log fCO_2 = \log K + 2 \log fH_2^{FMQ} + 2 \log fO_2 - 2 \log fH_2O$ (b), assuming $\log K = 37.5$, retrieved from the

reprimental data and thermodynamic modeling at 1 GPa and 800°C, using the EoS of Zhang &

768 Duan $(2009)^{47}$ and the H₂ fugacity coefficient of Connolly & Cesare $(1993)^{46}$. The increase in *X*CO₂

769 observed experimentally in the systems SiO₂–COH (pink dots) and MgO–SiO₂–COH (ochre dots),

compared to the pure COH system (green dots), can be achieved either by decreasing fH_2O (arrays

A; preferred interpretation) or by increasing fO_2 (arrays B; unlikely because of the lack of Fe and

772 other redox sensitive elements in the considered silicates). The decrease in fH_2O is ascribed to

773 dissolved Si-complexes and almost independent on dissolved Mg-complexes, and therefore

attributable to formation of hydrated silica monomers $[Si(OH)_4]$ and dimers $[Si_2O(OH)_6]$.





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Fig. 4: Evolution of dissolved CO_2 in fluids flushing a subduction mélange.

779 a) C-O-H diagram showing the compositional evolution of an aqueous fluid (empty dot) from a 780 slab interacting with graphite alone (magenta dot) and graphite + silicates (blue dot) in the subduction mélange. Compared to fluids interacting with graphite alone, fluids in equilibrium with 781 782 graphite + silicates display markedly higher XCO₂ (up to +30 mol% at 1 GPa, 800°C and fH_2^{FMQ}); 783 b) schematic drawing of a subduction mélange typical of collisional orogens flushed by aqueous 784 fluids released from the underlying dehydrating slab. In the model, these fluids interact with slices of rocks bearing forsterite + enstatite (mantle-derived) and graphite + quartz (sedimentary slab 785 786 cover). Because of the quadratic growth, small changes in water fugacity/activity due to dissolution of silicates and the consequent release of organosilicon complexes, can enhance the CO₂ content in 787 COH fluids, even in the absence of carbonates, as long as graphite is present. Such fluids will flush 788 789 the overlying mantle wedge, influencing metasomatic and/or melting processes.



